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Desalination for Safe Water Supply

*Guidance for the Health and Environmental Aspects Applicable to
Desalination*

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Note: A,B,C APPENDICES are available as drafts at www.who.int/water_sanitation_health.

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Preface

Access to sufficient quantities of safe water for drinking and domestic uses and also for commercial and industrial applications is critical to health and well being, and the opportunity to achieve human and economic development. People in many areas of the world have historically suffered from inadequate access to safe water. Some must walk long distances just to obtain sufficient water to sustain life. As a result they have had to endure health consequences and have not had the opportunity to develop their resources and capabilities to achieve major improvements in their well being. With growth of world population the availability of the limited quantities of fresh water decreases.

Desalination technologies were introduced about 50 years ago and were able to expand access to water, but at high cost. Developments of new and improved technologies have now significantly broadened the opportunities to access major quantities of safe water in many parts of the world. Costs are still significant but there has been a reducing cost trend, and the option is much more widely available. When the alternative is no water or inadequate water greater cost may be endurable in many circumstances.

More than 12,000 desalination plants are in operation throughout the world producing about 40 million cubic meters of water per day. The number is growing rapidly as the need for fresh water supplies grows more acute and technologies improve and unit costs are reduced

Desalination plants use waters impaired with salts (seawater or brackish water) or other contaminants as their sources. It appears that performance, operating and product quality specifications have evolved virtually on a site-by-site basis relative to source and the specific end product water use.

Most drinking water applications use World Health Organization drinking water guidelines in some way as finished water quality specifications. WHO Guidelines for Drinking-water Quality (GDWQ) cover a broad spectrum of contaminants from inorganic and synthetic organic chemicals, disinfection byproducts, microbial indicators and radionuclides, and are aimed at typical drinking water sources and technologies. Because desalination is applied to non-typical source waters, and often uses non-typical technologies, existing WHO Guidelines may not fully cover the unique factors that can be encountered during intake, production and distribution of desalinated water.

Apart from the quality and safety of the finished drinking water, numerous other health and environmental protection issues are also evident when considering the impacts of desalination processes. Not all of them are unique to desalination, and they may also relate to any large construction project sited in a coastal or other environmentally sensitive area. Protection of the coastal ecosystem and protection of groundwater from contamination by surface disposal of concentrates are examples of issues that must be addressed during the design, construction and operation of a desalination facility.

This document addresses both drinking water quality and environmental protection issues in order to assist both proposed and existing desalination facilities to be optimized to assure that nations and consumers will be able to enjoy the benefits of the expanded access to desalinated water with the assurance of quality, safety and environmental protection.

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Abbreviations and Acronyms

AI	Aggressiveness Index
AM	Anion Transfer Membrane
AOC	Assimilable Organic Carbon
AOP	Advanced Oxidation Process
BOD	Biochemical Oxygen Demand
BOM	Biodegradable Organic Matter
BTEX	Benzene, Toluene, Xylenes, Ethyl Benzene
BWRO	Brackish Water Reverse Osmosis
CCPP	Calcium Carbonate Precipitation Potential
CEB	Chemically enhanced backwash
CFD	Computational Fluid Dynamics
CM	Cation Transfer Membrane
CW	Cooling water
DBP	Disinfection by-product
DOC	Dissolved Organic Carbon
ED	Electrodialysis
EDR	Electrolysis Reversal
EDTA	Ethylenediaminetetraacetic acid
EIA	Environmental Impact Assessment
EIR	Environmental Impact Report
EMRO	WHO Eastern Mediterranean Regional Office, Cairo, Egypt
FRC	Free Residual Chlorine
GDWQ	WHO Guidelines for Drinking-water Quality
GRP	Glass reinforced plastic
GWI	Global Water Intelligence
HDD	Horizontal Directionally Drilled Collector
HDPE	High Density Polyethylene
HPC	Heterotrophic Plate Counts
LR	Larson Ratio
LSI	Langlier Saturation Index
MED	Multieffect Distillation
MED-TC	MED system with a thermo-compressor device
MF	Microfiltration
MGD	Million gallons per day, about 3785 cubic metres per MGD.
MS2	Male specific bacteriophage (F-RNA)
MSF	Multistage Flash Distillation
MU	Makeup water
MVC	Mechanical Vapor Compression
MW	Molecular Weight
NCG	Non-condensable gas
NDEA	Nitrosodiethylamine
NDMA	Nitrosodimethylamine or dimethylnitrosamine
NF	Nanofiltration
NOM	Natural Organic Matter

ORP	Oxidation Reduction Potential
PFU	Plaque forming unit
POE	Point-of-Entry
POU	Point-of-Use
PP	Polypropylene
PTA	Packed Tower Aeration
PVC	Polyvinyl chloride
RO	Reverse Osmosis
RTRP	Reinforced thermosetting resin pipe
SBS	Sodium Bisulfite
SDI	Silt Density Index
SWRO	Seawater Reverse Osmosis
TBT	Top brine temperature
TDS	Total Dissolved Solids
THMs	Trihalomethanes
TOC	Total Organic Carbon
TON	Total Organic Nitrogen
TOR	Terms of Reference
TSS	Total Suspended Solids
TVC	Thermal Vapor Compression
UF	Ultrafiltration
VCD	Vapor Compression Distillation
WET	Whole Effluent Toxicity
WHO	World Health Organization
WSP	Water Safety Plan
ZID	Zone of initial dilution

Desalinated Drinking-water Production: Health and Environment Issues

Desalination of seawater and brackish waters is a highly developed and integrated set of processes that adds several dimensions of complexity beyond what is typically involved in the production of drinking water from fresh water sources. This chapter provides insights into the concept of drinking water production and treatment and the elements that are managed in that process, as well as integrated management approaches for assuring the quality and safety of drinking water at the consumer's tap.

Access to sufficient quantities of safe water for drinking and domestic uses and also for commercial and industrial applications is critical to health and well being, and the opportunity to achieve economic development. People in many areas of the world have historically suffered from inadequate access to safe water. Some must walk long distances just to obtain sufficient water to sustain life. As a result they have had to endure health consequences and have not had the opportunity to develop their resources and capabilities to achieve major improvements in their well being. Desalination technologies were introduced about 50 years ago and were able to expand access to water, but at high cost. Developments of new and improved technologies have now significantly broadened the opportunities to access major quantities of safe water in many parts of the world. Costs are still significant but there has been a reducing cost trend, and the option is much more widely available. When the alternative is no water or inadequate water greater cost may be endurable.

Desalination of seawater and brackish water, along with planned water reuse for indirect potable and non-potable applications (e.g. irrigation) have been growing rapidly worldwide in recent years. This is because the need to produce more water and efficiently use water to satisfy the needs of growing and more demanding populations has become acute. These technologies are an advance in complexity from the more traditional technologies usually applied to relatively good quality freshwaters. As such, the cost of production is greater than from freshwater sources, but they are being applied in areas where the need is also greater. They share some of the same technologies so the science and technology of both processes have developed somewhat in tandem. This document focuses upon desalination and examines the major technologies and the health and environmental considerations that they bring that are in addition to water production from more traditional sources.

As of the beginning of 2006, more than 12,000 desalination plants are in operation throughout the world producing about 40 million cubic meters (roughly 10 billion US gallons) of water per day. About 50% of the capacity exists in the West Asia Gulf region. North America has about 17%, Asia apart from the Gulf about 10% and North Africa and Europe account for about 8 % and 7%, respectively, and Australia a bit over 1%. (GWI, 2006) The desalination market is predicted to grow by 12% per year to 2010. Capacity is expected to reach 94 million m³/day by 2015. (Water, 2006) Desalination plant sizes and designs range from more than 1,000,000 m³/day to 20 to 100 m³/day. Home sized reverse osmosis units may produce only a few litres per day. Over the next 10 years at least 100 billion USD for desalination is projected to be

needed in the Arab states alone just to keep up with economic growth and water demand, according to a 2006 report. (EMS, 2006)

This document was initiated to address health and environment questions associated with applications of desalination for drinking water supply. Many of these issues are not unique to desalination and they are also dealt with in the WHO Guidelines for Drinking-water Quality that this guidance for desalination augments.

- What are appropriate considerations for assuring the healthfulness of drinking water produced by desalination of seawater and brackish waters?
 - Should these reflect climate?
 - Should any other high end uses be considered?
- What should be the quality management guidance for blending waters that are added post desalination for adjustment and stabilization?
- What is the appropriate guidance for aesthetic and stability factors, e.g., TDS, pH, taste/odour, turbidity, corrosion indices, etc.?
- Should guidance reflect potentially nutritionally desirable components of reconstituted finished water, e.g., calcium, magnesium, fluoride?
- How should the quality specifications and safety of chemicals and materials used in production and in contact with the water e.g., coagulants, disinfectants, pipe and surfaces in desalination plants, distribution systems, etc be addressed?
- How should guidance include recommendations for monitoring of plant performance and water during distribution, e.g., key chemicals and microbiological parameters and frequencies?
- How should the guidance include considerations of environmental protection factors relating to siting, marine ecology, ground water protection, energy production, and air quality?

These topics are addressed in detail in the document:

- **Water quality, technology and health issues**

Drinking water systems should strive to produce and deliver to consumers safe drinking water that meets all quality specifications. Several technologies have applications for producing high quality water from non freshwater sources. The WHO Guidelines for Drinking-water Quality (GDWQ) provide comprehensive information in this respect and it applies equally to conventional or desalinated drinking water. Due to its nature, origin and typical locations where practiced, desalinated water provides some additional issues to be considered in respect to both potential chemical and microbial components. This guidance addresses both types of contaminants and it recommends some augmentations to the GDWQ to reflect some issues that are specific to desalinated drinking water.

- **Aesthetics and water stability**

Although not directly health related, aesthetic factors like taste, odour, turbidity, and total dissolved solids (TDS) affect palatability and thus consumer acceptance, and indirectly health. Corrosion control and hardness and pH have economic consequences and they also determine the extraction of metals and other pipe components during distribution. Chemical additives and blending are used to adjust these parameters and the composition and lifespan of the distribution network are intimately related to them.

- **Blending waters**

Blending is used to increase the TDS and improve the stability of finished desalinated water. Components of the blending water can also affect the quality and safety of the finished water because it may not receive any further treatment beyond residual disinfection. Some contaminants may be best controlled by selection of or pretreatment of the blending water. It is possible that some of the microorganisms in the blending water could be resistant to the residual disinfectant, could contribute to biofilms, or could be inadequately represented by surrogate microbial quality measurements such as *E. coli* or heterotrophic plate counts.

- **Nutritionally Desirable Components**

Desalinated water is stabilized by adding lime and other chemicals. Although drinking water cannot be relied on to be a significant source of supplemental minerals in the daily diet, there is a legitimate question as to the optimal mineral balance of drinking water to assure quality and health benefits. There is a consensus that dietary calcium and magnesium are important health factors, as well as certain trace metals, and fluoride is also considered to be beneficial for dental and possibly skeletal health by most authorities. (Cotruvo, 2006, WHO, 2005, WHO, 2006) There is a public health policy and practical economic and political question as to whether and to what extent drinking water should provide nutritional elements, and this question would be addressed differently in different dietary, political and social environments.

- **Chemicals and materials used in water production**

Chemicals used in desalination processes are similar to those used in standard water production; however, they may be used in greater amounts and under different conditions. Polymeric membranes as used in desalination processes are not yet as widely used in conventional water treatment, and metals and other components could be subjected to greater than usual thermal and corrosion stresses in desalination compared to conventional water treatment, and distribution.

The WHO GDWQ addresses Chemicals and Materials used in Drinking Water Treatment. It provides some recommended quality and dose specifications, but also encourages the institution of processes for guidelines for quality and safety of direct and indirect additives by national and international institutions. This Desalination Guidance encourages governments to establish systems for specifying the appropriateness and quality of additives encountered in desalination, or to adopt existing credible recognized standards for those products that would be tailored to desalination conditions.

- **Water quality and distribution system monitoring**

Desalination processes utilize non-traditional water sources and technologies and produce drinking water that is different from usual sources and processes. Desalination may also be practiced in locations that require longer distribution networks. Recommendations for monitoring for process surveillance and distributed water quality are provided to assist water suppliers and regulators. Some chemical and microbial monitoring for desalination system management and to assure safety could be site specific so operators and authorities should consider identification of a small number of key parameters associated with desalination, included or in addition to the WHO GDWQ, that would be useful in particular circumstances as well as articulating basic principals that should be utilized when designing a monitoring scheme.

- **Environmental quality and environmental impact assessments**

As with any major project, large-scale desalination projects can have a significant effects on the environment during construction and operation. Procedures and elements of Environmental Impact Assessments (EIA) are provided in this Guidance to assist project designers and decision makers to anticipate and address environmental concerns that should considered when undertaking a project. Among the factors that are addressed are: siting considerations, coastal zone/marine protection regarding withdrawal and discharge, air pollution from energy production and consumption, groundwater protection from drying beds, leachates, and sludge disposal.

1.1 Drinking-water production and related issues

Drinking water production processes can be divided into three broad categories each of which will impact the quality of the finished water received by the consumer:

- I. Source Water
- II. Treatment Technology
- III. Distribution System

Some of the factors and issues that distinguish desalination from most typical drinking water operations are as follows:

Source Water

- Total Dissolved Solids in the range of about 5,000 to 40,000 mg/litre
- High levels of particular ions including sodium, calcium, magnesium, bromide, iodide, sulfate, chloride
- Total Organic Carbon type
- Petroleum contamination potential
- Microbial contaminants and other organisms

Treatment Technology

- Reverse Osmosis (RO) membranes and distillation
- Leachates from system components

- Pretreatment and anti fouling additives
- Disinfection by-products
- Blending with source waters

Distribution System Management

- Corrosion control additives
- Corrosion products
- Bacterial regrowth, including non pathogenic HPC and pathogens like *legionella*

Related issues that needed to be considered included:

- Are there risks from consumption of water with low total dissolved solids (TDS) either from general reduced mineralization or reduced dietary consumption of specific minerals, or from corrosivity toward components of the plumbing and distribution system.
- Environmental impacts of desalination operations and brine disposal.
- Whether microorganisms unique to saline waters may not be removed by the desalination process or post blending disinfection

Monitoring of source water, process performance, finished water and distributed water to assure consistent quality at the consumer's tap.

1.2 Source water composition

A typical fresh water source for producing potable water could be a river, lake, impoundment or shallow or deep groundwater. The water could be virtually pristine, affected by natural contaminants, or impacted by agricultural and anthropogenic waste discharges. Even a pristine source may not be wholly desirable because it could contain minerals and suspended particulates that adversely affect the taste and aesthetic quality or safety, and natural organic materials (Total Organic Carbon and Total Organic Nitrogen) that could adversely affect the quality of the finished water and place demands upon the treatment processes. The range of mineralization of most fresh waters considered to be desirable could be from less than 100 mg/litre to about 1000 mg/litre.. Microbial contamination can occur in any even pristine source water, but especially in surface waters. Many surface waters are significantly impacted by controlled or uncontrolled discharges of sewage, agricultural or industrial wastes, and surface runoff, so virtually all surface waters require filtration and disinfection prior to becoming acceptable drinking water. Groundwaters often benefit from natural filtration from passage through the ground and underground storage, but they can also be naturally contaminated (e.g. TDS, arsenic or excess fluoride). If they are 'under the influence of surface water' they also can become contaminated by surface waste discharges of sewage, agricultural and industrial waste or spills particularly if the aquifer is shallow, or the overlaying soil is porous and does not retard migration of some contaminants, or disposal in unlined ponds is practiced. However, many groundwaters are sufficiently protected that they may be consumed without further treatment, or possibly only disinfection.

Table 1.1 Major ion composition of seawater (mg/litre) (Al-Mutaz, 2000)

Constituent	Normal Seawater	Eastern Mediterranean	Arabian Gulf At Kuwait	Red Sea At Jeddah
Chloride (Cl ⁻¹)	18,980	21,200	23,000	22,219
Sodium (Na ⁺¹)	10,556	11,800	15,850	14,255
Sulfate (SO ₄ ⁻²)	2,649	2,950	3,200	3,078
Magnesium (Mg ⁺²)	1,262	1,403	1,765	742
Calcium (Ca ⁺²)	400	423	500	225
Potassium (K ⁺¹)	380	463	460	210
Bicarbonate (HCO ₃ ⁻¹)	140	--	142	146
Strontium (Sr ⁺²)	13	--	--	--
Bromide (Br ⁻¹)	65	155	80	72
Boric Acid (H ₃ BO ₃)	26	72	--	--
Fluoride (F ⁻¹)	1	--	--	--
Silicate (SiO ₃ ⁻²)	1	--	1.5	--
Iodide (I ⁻¹)	<1	2	--	--
Other	1	--	--	--
Total Dissolved Solids	34,483	38,600	45,000	41,000

-- = not reported

Table 1.2 Major ion composition of a raw brackish water (mg/litre) (USBR, 1976)

Constituent	Design Value	Design Range
Calcium (Ca ⁺²)	258	230 - 272
Magnesium (Mg ⁺²)	90	86 - 108
Sodium (Na ⁺¹)	739	552 - 739
Potassium (K ⁺¹)	9	NK
Strontium (Sr ⁺²)	3	NK
Iron (Fe ⁺²)	< 1	0 - < 1
Manganese (Mn ⁺²)	1	0 - 1
Bicarbonate (HCO ₃ ⁻¹)	385	353 - 385
Chloride (Cl ⁻¹)	870	605 - 888
Sulfate (SO ₄ ⁻²)	1,011	943 - 1,208
Nitrate (NO ₃ ⁻¹)	1	NK
Phosphate (PO ₄ ⁻³)	< 1	NK
Silica (SiO ₂)	25	NK
Total Dissolved Solids	3,394	2,849 - 3,450
pH	8.0	7.8 - 8.3
Temperature	75 °F	65 °F - 85 °F

NK = not known: the sum of these ions is estimated to be between 30 and 40 mg/litre

Seawaters and brackish waters, however, are defined by the extent of the mineralization that they contain. Thus, their composition includes substantial quantities of minerals that is partly a function of their geographic location, and they also contain organic carbon and microbial contaminants, and they can also be impacted by waste discharges. Tables 1.1 (Al-Mutaz, 2000) and 1.2 (USBR, 1976) above provide information on the typical mineral composition of several seawaters. Obviously, special technologies will be required to convert these waters into drinking water that would be safe and desirable to consume.

1.3 Fresh water treatment technologies

Treatment of fresh, i.e., low salinity, waters centres on particulate removal and microbial inactivation. Thus, filtration and disinfection are the main technologies used, with some exceptions. Coagulation, sedimentation, and rapid sand filtration are commonly used in surface waters, with chlorine or chlorine dioxide and possibly ultraviolet light for primary disinfection, and sometimes chloramines for secondary disinfection. Ozone is used for several purposes. Some reduction of natural organics occurs in the coagulation/filtration process; microfiltration and ultrafiltration are becoming more widely used, powdered carbon and granular activated carbon are used for taste and odour and sometimes to reduce organics; softening is sometimes practiced to reduce hardness caused by calcium and magnesium. Targeted technologies are used in some applications e.g. for arsenic or nitrate removals.

Home treatment technologies are usually applied as a polish on supplied water, however, there are some technologies that can provide complete treatment and purification. Those technologies should be tested under rigorous conditions and certified by a credible independent organization to meet the claims that they make. They can be at the point-of-use (POU, end of tap), or point-of-entry (POE, whole house) treating all of the water entering the home. The most common systems usually involve ion exchange water softening, or activated carbon for chlorine taste and some organics, or iron removal. There are also technologies available for controlling specific classes of contaminants and some can be used to meet standards and guidelines for various chemicals and sanitary microbial contaminants. Disinfection techniques are also available for home or traveller use.

1.4 Desalination technologies

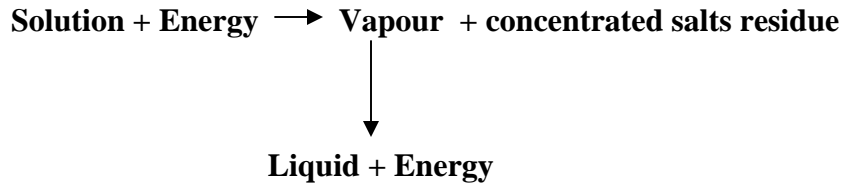
Desalination processes remove dissolved salts and other materials from seawater and brackish water. Related membrane processes are also used for water softening and waste water reclamation. The principal desalination technologies in use are distillation and membrane technologies. Desalination technologies are energy intensive and research is continually evolving approaches that improve efficiency and reduce energy consumption. Cogeneration facilities are now the norm for desalination projects.

1.4.1 Distillation technologies

The principal distillation systems include Multistage Flash (MSF) distillation, Multi-effect Distillation (MED) and Vapour Compression Distillation (VCD). Distillation plants can produce water in the range of 1 to 50 mg/litter TDS. Alkaline cleaners remove organic fouling and acid cleaners remove scale and salts.

A simplified outline of the process is provided in Figure 1.2. In distillation processes source water is heated and vaporized; the condensed vapour has very low total dissolved solids, while concentrated brine is produced as a residual. Inorganic salts and high molecular weight natural organics are non volatile and thus easily separated, however there are circumstances where volatile petroleum chemicals are present due to spills and other contamination. Even though their vapour pressures can range from low to very high some of them of higher molecular weight can also be steam distilled.

Figure 1.1 Distillation process representation



For water, the boiling point (where the vapour pressure of the liquid is the same as the external pressure) is 100°C (212°F) at 1 atmosphere (101.325 kilo Pascals, 1013.25 millibars, 760 mm Hg, or 14.7 pounds per square inch). As the concentration of solute increases the boiling point of the solution increases; as the pressure is decreased, the boiling temperature decreases. The amount of energy required to vaporize a liquid is called the heat of vaporization. For water, this amounts to 2,256 kilojoules per kilogram at 100°C (970 Btu per pound at 212°F). The same amount of heat must be removed from the vapour to condense it back to liquid at the boiling point. In desalination processes, the heat generated from vapour condensation is transferred to feed water to cause its vaporization and thus improve the thermal efficiency of the process and reduce fuel consumption and cost.

Multistage Flash Distillation (MSF)

MSF plants are major contributors to the world desalting capacity. The principle of MSF distillation is that heated water will boil rapidly (flash) when the pressure of the vapour is rapidly reduced below the vapour pressure of the liquid at that temperature. The vapour that is generated is condensed on to surfaces that are in contact with feed water thus heating it prior to its introduction into the flash chamber. This will recover most of the heat of vaporization. Approximately 25 to 50% of the flow is recovered as fresh water in multistage plants. Characteristics of MSF plants include high feed water volume and flow, corrosion and scaling in the plant, and high rates of use of treatment chemicals.

Multiple – Effect distillation (MEF)

Configurations of MEF plants include vertical or horizontal tubes. Steam is condensed on one side of a tube with heat transfer causing evaporation of saline water on the other side. Pressure is reduced sequentially in each effect (stage) as the temperature declines, and additional heat is provided in each stage to improve performance.

Vapour compression distillation (VCD)

VCD systems function by compressing water vapour causing condensation on a heat transfer surface (tube) which allows the heat of condensation to be transported to brine on the other side

of the surface resulting in vaporization. The compressor is the principal energy requirement. The compressor increases the pressure on the vapour side and lowers the pressure on the feed water brine side to lower its boiling temperature.

1.4.2 Membrane technologies

Common membranes are polymeric materials such as cellulose triacetate or more likely polyamides and polysulfones. Membranes are typically layered or thin film composites. The surface contact layer (rejection layer) is adhered to a porous support, which can be produced from the same material as the surface. Membrane thickness is on the order of 0.05 mm. Selection factors for membranes include: pH stability, working life, mechanical strength, pressurization capacity and selectivity and efficiency for removal of solutes. Membranes are located in a module and they can be configured as hollow fibre, spiral, plate and tubular. Each has its own characteristics that affect selection in particular cases. Hollow fibre and spiral configurations generally have more favourable operating characteristics of performance relative to cost and they are most commonly used. Operating pressures are in the range of 250 – 1000 psi (17 to 68 bar, 1724 kPa to 6896 kPa).

There are numerous compositions of membranes within each category. Table 1.2 provides some generalized performance expectations for 4 major categories of membrane systems. The larger pore membranes like MF and UF are often used as pretreatments to remove larger particulate contaminants and to reduce the loadings on the more restrictive membranes like RO, and extend their performance and run times.

Table 1.2 Comparison of Membrane Process Performance Characteristics

Membrane Type	Nominal Pore Size (in µm) (approximate)	Constituents Removed
Microfiltration	0.1 to 1	particulates, bacteria, protozoa
Ultrafiltration	0.001 to 0.1	viruses, large and high MW organics e.g. pyrogens
Nanofiltration	+/- 0.001	multivalent metal ions, some organics
Reverse Osmosis	0.0001 to 0.001	Seawater, brackish water desalination, organics >100-300 daltons

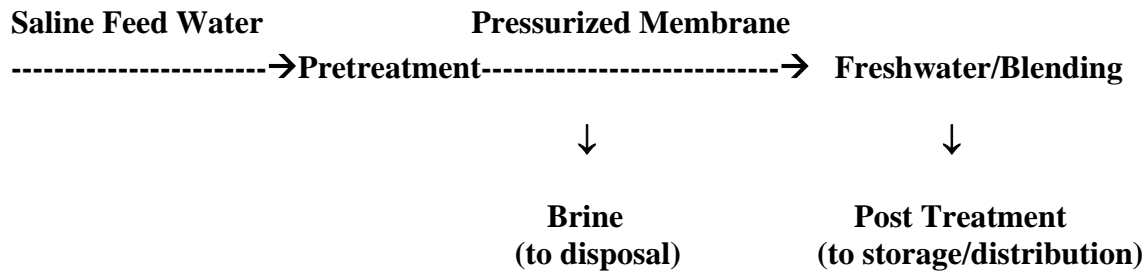
(from www.watertreatmentguide.com)

Reverse Osmosis (RO)

Reverse osmosis systems reverse the natural process of solvent transport across a semi-permeable membrane from a region of lower solute concentration into one of higher solute concentration to equalize the free energies. In RO external pressure is applied to the high solute (concentrated) water to cause solvent (water) to migrate through the membrane leaving the solute

(salts and other non permeates) in a more concentrated brine. Some membranes will reject up to 99% of all ionic solids and commonly have molecular weight cut off in the range of 100 to 300 daltons for organic chemicals. Increased pressure increases the rate of permeation, however fouling would also increase. Figure 1.2 illustrates the basic RO process, which includes Pretreatment, Membrane Transport, and Post Treatment prior to distribution. RO processes can produce water in the range of 10 to 500 mg/litre TDS.

Figure 1.2 RO desalination process outline



Nanofiltration

Nanofiltration is capable of removing many relatively larger organic compounds in the range of about 300 to 1000 Daltons, and rejecting many divalent salts; monovalent ions removal can be in the range of 50 to 90%. It is applied in water softening, food and pharmaceutical applications. Nanofiltration operates at lower pressure than RO systems e.g. ~50 psi to 450 psi (344.74 kilopascals to 3102.6 kilopascal). Systems may include several stages of polymeric membranes.

(from www.appliedmembranes.com and www.dunlopdesign.com/resources/nanofiltration)

Electrodialysis

In electrodialysis-based treatment systems a direct current (DC) is passed through the water, which drives the ions (not the water) through membranes to electrodes of opposite charge. In electrodialysis reversal (EDR) systems, the polarity of the electrodes is reversed periodically during the treatment process. Ion-transfer (perm-selective) anion and cation membranes separate the ions in the source water. Electrodialysis (ED and EDR) processes utilize selective membranes that contain cation and anion exchange groups. Under a direct current electric field, cations and anions migrate to the respective electrodes so that ion-rich and ion-depleted streams form in alternate spaces between membranes. Reversal of electric fields reduces scaling and flushes the membranes. Pretreatment is required to control scale and extend membrane life and to prevent migration of non ionized substances such as bacteria and organics and silica.

Forward osmosis

Forward osmosis (FO) is one of the experimental approaches being studied. In FO, ammonia and carbon dioxide are added to fresh water on the opposite side of the membrane from the saline water to increase the ammonium carbonate concentration so that water from the salt solution naturally migrates through the membrane to the ammonium carbonate ‘draw’ solution without

external pressure. The diluted ‘draw’ solution is then heated to drive off the ammonia and carbon dioxide which are captured and reused (Elimelich, 2006). Potential advantages compared to RO include: no external pressure is required; high recovery efficiency; lower energy costs. Additional research is required to determine its viability.

1.5 Pretreatment

Feedwater is treated to protect the membranes by removing some contaminants and controlling microbial growth on the membrane and to facilitate membrane operation. Suspended solids are removed by filtration, pH adjustments (lowering) are made to protect the membrane and control precipitation of salts; antiscaling inhibitors are added to control calcium carbonates and sulfates. Iron, manganese and some organics cause fouling of membranes. A disinfectant is added to control biofouling of the membrane. Disinfection can involve chlorine species, ozone or UV light and other agents. Marine organisms, algae and bacteria must be eliminated, and if chlorine is used it should be neutralized prior to contact with the membrane.

1.6 Post Treatment

Product water must be treated to stabilize it and make it compatible with the distribution system. Adjustment of pH to approximately 8 is required. Carbonation or use of other chemicals such as lime may be applied, and blending with some source water may be done to increase alkalinity and TDS and stabilize the water. Addition of corrosion inhibitors like polyphosphates may be necessary. Post disinfection is also necessary to control microorganisms during distribution, as well as to eliminate pathogens from the blending process. Degasification may also be necessary. Many systems blend back a portion of the source water with the desalinated water for mineralization. With seawater, this is usually limited to about 1% due to taste contributed by sodium salts. Both blending with source water or treatment with lime or limestone also reconstitute some of the beneficial minerals. Some systems have utilized electrolysis of seawater to generate hypochlorite in situ for disinfection and then blend it back to the desalinated water at about 1%. This practice generates very large amounts of bromate and organohalogen disinfection by-products (halogenated DBPs) and even the 1% blended desalinated water can far exceed the WHO drinking water guideline of 10 ppb bromate.

1.7 Technical and health issues associated with desalination

1.7.1 Potentially beneficial chemicals

Water components can supplement dietary intake of trace micronutrients and macronutrients or contribute undesirable contaminants. The line between health and illness in a population is not a single bright line, but rather a complex matter of optimal intake, versus adequate intake, versus intake that is inadequate to maintain good health, versus a toxic intake that will lead to frank illness in some higher risk segments of the population. Some parts of the population such as young children, pregnant women, the aged and infirm and immune compromised can be more sensitive than the typical healthy adult to both essential and hazardous dietary components.

Some of the chemicals of beneficial interest in drinking water include calcium, magnesium, sodium, chloride, lead, selenium, potassium, boron, bromide, iodide, fluoride, chromium, and manganese. Seawater is rich in ions like calcium, magnesium, sodium, chloride and iodine, but low in other essential ions like zinc, copper, chromium and manganese.

Desalination processes significantly reduce all of the ions in drinking water so that people who traditionally consume desalinated water may be consistently receiving smaller amounts of some nutrients relative to people who consume water from more traditional sources and thus are disadvantaged if their diets are not sufficient. Since desalinated water can be stabilized by addition of lime, for example, or sometimes blending, some of these ions will be automatically replenished in that process. (WHO, 2005; WHO 2006)

Sodium can be present in desalinated water depending upon the efficiency of salts removal and the post treatment blending which could involve non-desalinated seawater. Typical daily dietary intake of sodium can be in the range of 2000 to 10,000 mg and more and is a function of personal taste and cultural factors. Water is usually not a significant contributor to total daily sodium intake except for persons under a physician's care who are required to be on highly restricted diets of less than 400 mg sodium per day.

1.8 Contamination issues

1.8.1 Source contamination

Source selection and source protection are the best ways to avoid contamination of finished water by certain organics, surface runoff, ship discharges, and chemical and sanitary waste outfalls near the intake to the desalination plant. When contamination occurs, pretreatments may be necessary and these can involve enhanced disinfection, an adsorption process using granular activated carbon or more frequently powdered activated carbon for intermittent contamination. Of course, contaminants in blending waters will be transported to the finished water thus appropriate pretreatment of blending water may also be required.

1.8.2 Petroleum and petroleum products

The molecular weight cut off for RO membrane performance is typically in the range of 100-300 daltons for organic chemicals. RO membranes can remove larger molecules, however significant fouling would impede operations; small molecules pass through the membrane. Distillation processes can theoretically separate any substance by fractionation based upon boiling point differences, however distillation for desalination is not designed to be a fractionating system, thus substances with boiling points lower than water's would be carried over in the vapours and should be vented out.

1.8.3 Disinfection and microbial control in drinking water

Similar to fresh waters, sea and brine waters can contain pathogenic microorganisms including bacteria, protozoa and viruses. Disinfection can be applied at several points during the treatment process. The question is what is the adequate level of disinfection to protect public health from exposure to pathogenic microbes and are there any unique risks that may be associated with desalination practices. During pretreatment a disinfectant, often chlorine, will be added to reduce biofouling and protect the membrane from degradation. Membranes also have the capacity to remove microorganisms by preventing their passage to the finished water. So long as the membranes are intact virtually complete removals of microorganisms can occur, however some bacteria can grow through the membrane.

Ultrafiltration membranes which have pores (~0.001 to 0.1 micrometres) have been demonstrated to achieve significant reductions of virus and protozoa (McLaughlin, 1998). Better performance would be expected from RO membranes. Several challenge tests employing giardia lamblia and cryptosporidia cysts and MS2 bacteriophage with an ultra-filtration membrane of nominal pore size of 0.035 micrometre, and 0.1 micrometre absolute have demonstrated very effective removals. Giardia cysts can vary from 4 to 14 micrometres in length and 5 to 10 micrometres in width; cryptosporidia cysts range from about 4 to 6 micrometres. These intact ultrafiltration membranes (0.1 micron nominal) should completely remove the cysts. MS2 bacteriophage size is approximately 0.027 micrometres, which is smaller than the pore size of the UF membrane. However, substantial removal can be achieved probably due to adsorption of the virus on suspended particles, adsorption on the membrane or from the secondary filtration due to fouling of the membrane surface.

In a bench scale study (Adham, 1998) that evaluated rejection of MS2 coliphage (0.025 micrometres, icosahedral) by several commercial RO membranes with a nominal pore size cut off of <0.001 micrometres, permeation was observed in several cases. Although these were bench scale simulations in particle free water, they demonstrate that even similar RO membranes can have very different performance, and quality control procedures are required in their manufacture to assure consistent performance for very small organisms like viruses.

Distillation at high temperatures close to the normal boiling point of water would likely eliminate all pathogens. However, reduced pressures are used in some desalination systems to reduce the boiling point and reduce energy demands. Temperatures as low as 50° to 60°C may be reached. Several pathogenic organisms including many protozoa are denatured or killed in a few seconds to minutes at milk pasteurization temperatures in the 63°C (30 minutes) to 72°C (16 seconds) range, but spores and some viruses require higher temperatures and longer times.

Microbial growth during storage and distribution may be particular concerns when water is stored and distributed in very warm climates. Most regrowth microorganisms are not frank pathogens, but microorganisms such as *Legionella* that grow in plumbing systems at warm temperatures are a particular health concern, and have caused numerous disease outbreaks in hospitals and other buildings.

1.9 Disinfection by-products (DBPs)

Significant amounts of disinfection by-products can be formed in the pretreatment process that are applied in both membrane and distillation processes. The desalination process must then be relied upon to remove them along with the other contaminants that are present. Small solvent molecules like trihalomethanes will challenge the membranes, and since many of the DBPs are volatile they will also require venting during distillation processes. Since desalinated waters are lower in Total Organic Carbon than most natural waters it would be expected that the post desalination disinfectant demand and also disinfectant byproduct formation would be relatively low, and this has been indicated in some studies of trihalomethane production that have been reported (Al-Rabeh, 2005). However, this could be significantly affected by the type of blend water that is used post treatment to stabilize the water. One of the factors to consider would be the amount of brominated organic byproducts that could be formed if bromide is reintroduced to the finished waters. Since the TOC found in seawater could be different than TOC in fresh

waters, and since the pretreatment conditions are also different, it is probable that there would be some differences in the chemistry of the byproduct formation reactions that could lead to some different byproducts or different distributions of byproducts.

1.10 Waste and concentrates management

Wastes from desalination plants include concentrated brines, backwash liquids containing scale and corrosion salts and antifouling chemicals, and pretreatment chemicals in filter waste sludges. Depending upon the location and other circumstances including access to the ocean and sensitive aquifers, concentrations of toxic substances etc., wastes could be discharged directly to the sea, mixed with other waste streams before discharge, discharged to sewers or treated at a sewage treatment plant, placed in lined lagoons and dried and disposed in landfills. Concentrates disposal is one of the most challenging issues with respect to desalination processes. Recovery of important minerals from concentrates is possible and may be economically viable in some cases, because it also reduces waste disposal costs.

1.11 Energy consumption

Desalination plants require significant amounts of electricity and heat depending upon the process, temperature and source water quality. For example, it has been estimated that one plant producing about seven million gallons (about 26,500 m³) per day could require about 50 million kWh/yr., which would be similar to the energy demands of an oil refinery or a small steel mill. For this reason, cogeneration facilities provide significant opportunities for efficiencies. There is an obvious synergy between desalination and energy plants. Energy production plants require large water intakes for cooling purposes, they produce substantial amounts of waste heat that is usable in the desalination facility, and the spent water disposal system may also be shared. The International Atomic Energy Agency has studied the role of nuclear power plants as cogeneration facilities

1.12 Environmental Impacts

Installation and operation of a desalination facility will have the potential for adverse impacts on air quality, water/sea environment, and ground water and possibly other aspects. These must all be considered and their acceptability and mitigation requirements would usually be matters of national and local regulation and policies. Studies to examine these effects would usually be conducted at each candidate site, and post installation monitoring programs should be instituted. A brief partial listing of issues follows:

Construction: Coastal zone and sea floor ecology, birds and mammals habitat; erosion, non point source pollution.

Energy: Fuel source and fuel transportation, cooling water discharges, air emissions from electrical power generation and fuel combustion.

Air Quality: Energy production related.

Marine Environment: Constituents in waste discharges, thermal effects, feed water intake process, effects of biocides in discharge water, and toxic metals, oxygen levels, turbidity, salinity, mixing zones, commercial fishing impacts, recreation, and many others.

Ground Water: Seepage from unlined drying lagoons causing increased salinity and possibly toxic metals deposition.

1.13 Water Safety Plans in the operation and management of water systems

The most effective way to consistently ensure the safety of a drinking-water supply is through the use of a comprehensive planning, risk assessment and risk management approach that encompasses all of the steps in the water supply train from the catchment to the consumer. The WHO has developed the systematized Water Safety Plan (WSP) approach based upon the understanding of water system function derived from the worldwide history of successful practices for managing drinking water quality (WHO, 2004; WHO 2005a). The WSP concept draws upon principles and concepts of sanitary surveys, prevention, multiple barriers, vulnerability assessments, and quality management systems such as Hazard Assessment Critical Control Points (HACCP) as used in the food industry. A WSP has three key components: system assessment; measures to monitor and control identified risks; and management plans describing actions to be taken during normal operations or incident conditions. These are guided by health-based targets (drinking water standards, guidelines and codes), and overseen through surveillance of every significant aspect of the drinking water system.

Note: This section was derived in part from an assessment and its references prepared for the WHO's Eastern Mediterranean Regional Office by J.A. Cotruvo. It was also the basis for New World Health Organization Guidance for Desalination: Desalinated Water Quality Health and Environmental Impact, Environment 2007

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Desalination Technology– Essential Issues and Considerations

2.1 General Description

This section analyses the major aspects of desalination technology engineering and chemistry. The section also identifies potential process-related mechanisms that may bring about departures from a desired drinking water quality goal. Environmental considerations are taken into account in the decisions for selection of the treatment processes and technologies and concentrates management. It also highlights system designs and operational conditions that may bring about possible contamination or degradation of the desalinated product water, and design and operational practices that are normally adopted in order to avoid such departures. It could be considered as guidance for process selection, design and operation of desalination processes. The document has been structured to address both major installations that produce large quantities of product water (i.e., plants with production capacity of over 10 MGD, about 40,000 m³/day) as well as small installations such as package plants, ship-board systems and point-of-use facilities that are typically installed in remote areas in order to supplement existing water systems, and where practical reasons often prevent the designers from adopting solutions and procedures that are widely used in large scale installations.

2.1.1 Desalination processes and water quality issues

Water produced by desalination methods has the potential for contamination from source water and from the use of various chemicals added at the pre-treatment and desalination and post treatment stages. Natural water resources are more likely to be impacted by microbiological contamination when they are receiving waters of wastewater discharges and surface runoff.

Regulatory frameworks developed for water produced by desalination take account of these differences and in addition they consider the type of desalination process employed, either using thermal or membrane technology. Testing processes are discussed in Chapter 5, and they assume that monitoring is designed for operational control as well as to meet regulatory quality requirements. Monitoring is not an end in itself, rather it should be designed to provide useful information to confirm that the process was properly designed, and built and is being properly operated to prevent contamination from reaching consumers.

2.1.2 Water Safety Plans

The safety and performance of a system for providing drinking water depends upon the design, management and operation of the three principal components: source, treatment, and distribution. If contamination has occurred and it is not controlled before it reaches the consumers taps, illness or even death is possible. So, the entire system must be designed to anticipate and cope with all

of the problems that could occur, and proper performance of the entire system must be assured at all times. The most effective way to consistently ensure the safety of a drinking-water supply is through the use of a comprehensive risk assessment and risk management approach that encompasses all of the steps in the water supply train from the source water catchments to the consumer. This concept is fully applicable to desalination systems. The WHO has developed the systematized Water Safety Plan (WSP) approach based upon the understanding of water system function derived from the worldwide history of successful practices for managing drinking water quality (WHO, 2004c), see also Chapter 6. The WSP concept draws upon principles and concepts of prevention, multiple barriers and quality management systems such as Hazard Assessment Critical Control Points (HACCP) as used in the food industry. Desalination treatment processes are usually more comprehensive than standard water technologies so they are particularly suited to WSP applications.

A WSP has three key components guided by health-based targets (drinking water standards and guidelines, and codes), and overseen through surveillance of every significant aspect of the drinking water system. The three components are:

System assessment to determine whether the system as a whole (from source to consumer) can consistently deliver water that meets health based targets. This includes assessment of design criteria for new systems as well as modifications.

Measures to monitor and control identified risks (and deficiencies) and ensure that health-based targets are met. For each control measure, appropriate operational monitoring should be defined and instituted that will rapidly detect deviations.

Management plans describing actions to be taken during normal operations or incident conditions, and documenting the system assessment (including system upgrades and improvements), monitoring, and communication plans and supporting programmes.

The primary objectives of a WSP are the minimization of contamination of source waters, reduction or removal of contamination through appropriate treatment processes, and prevention of contamination during processing, distribution and storage. These objectives are equally applicable to and can be tailored to large piped supplies and small community supplies, large facilities (hotels and hospitals), and even household systems. The objectives are met through the interpretation and detailed implementation of the key phrases: ‘hazard assessment’ and ‘critical control points’, in a systematic and documented planned methodology for the entire life of the system. A progression of the key steps in developing a WSP is as follows:

- Assemble and train the team to prepare the WSP;
- Document and describe the system;
- Undertake a detailed hazard assessment and risk characterization to identify and understand how hazards can enter into the system;
- Assess the existing system (including a description of the system and a flow diagram);
- Identify control measures - the specific means by which specific hazards may be controlled;

- Define monitoring of the control measures – what are the limits that define acceptable performance and how are these monitored;
- Establish procedures to verify that the WSP is functioning effectively and will meet the health-based targets
- Develop supporting programmes e.g. training, hygiene practices, standard operating procedures, upgrades and improvements, research and development etc.;
- Develop management procedures including corrective actions for normal and incident conditions;
- Establish documentation and communication procedures.

These key steps in the WSP operate in a continuous and cyclical mode by returning to the documenting and system description step and repeating the process routinely. Detailed expansions of this WSP concept can be found in the Guidelines for Drinking-water Quality (WHO, 2004) and in other writings including detailed discussions of WSPs for distribution systems.

2.2 Structure of this section

The description of desalination treatment technologies presented herein follows the treatment process sequence of a typical desalination plant (see Figure 2.1). For each treatment process step there is a description of the main treatment technologies that are widely used, followed by a part where issues and considerations are highlighted for the treatment process step.

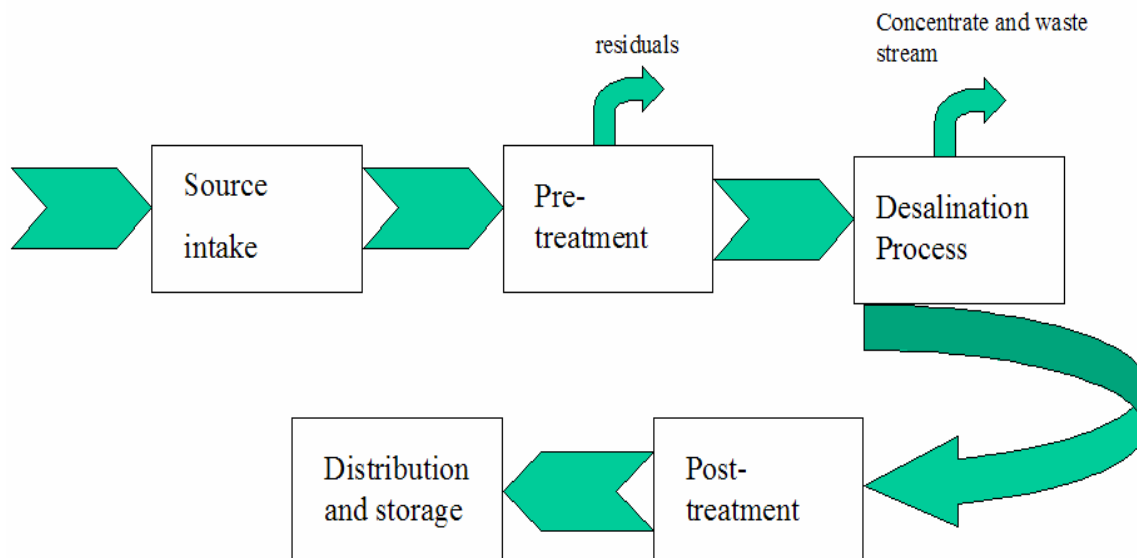


Figure 2.1 Typical sequence of desalination treatment and distribution processes

2.3 Source water intake facilities

2.3.1 General description

Desalination facilities require an intake system capable of providing a reliable quantity of source water (raw feed water) of a reasonably consistent quality and with a minimum ecological impact. As the first step in the pre-treatment process, the type of intake used would affect a range of source water quality parameters and would impact the performance of downstream treatment facilities. Intake designs are highly site specific, possibly more so than any other aspect of the desalination facility. The design, modelling, monitoring, and permitting activities that surround them, may represent as much as 10% to 30 % of the capital cost of the entire facility. A good intake design would not only protect downstream equipment and reduce environmental impact on aquatic life, but it would enhance process performance and reduce pre-treatment system capital and operating costs as well.

Two general types of intake facilities are used to obtain source water for desalination plants: subsurface intakes (wells, infiltration galleries, etc.) and open intakes. Seawater intake wells are either vertical or horizontal source water collectors, which are typically located in close vicinity to the sea. In the case of aquifers of high porosity and transmissivity, which easily facilitate underground seawater transport such as the limestone formations of many Caribbean islands and Malta, seawater of high quality and large quantity may be collected using intake wells located in-land rather than at the shore. This allows reducing the distance for seawater collection, and thus the costs of conveyance by locating the desalination plant closer to the main users rather than at the shore. Brackish water treatment plants usually use wells for source water collection, since the source water is typically located above in-land brackish aquifers.

Intake wells are relatively simple to build and the seawater or brackish water they collect is pre-treated via slow filtration through the subsurface sand/seabed formations in the area of source water extraction. Vertical intake wells are usually less costly than horizontal wells; however their productivity is relatively small and therefore, the use of vertical wells for large plants is less favourable (Figure 2.2).

Horizontal subsurface intakes are more suitable for larger seawater desalination plants and are applied in two configurations: radial Ranney-type collector wells (Figure 2.3) and horizontal directionally drilled (HDD) collectors. Vertical wells and radial collector wells are used to tap into the on-shore coastal aquifer or inland brackish water aquifer, while HDD collectors are typically extended off-shore under the seabed for direct harvesting of seawater. The HDD collector wells consist of relatively shallow blank well casing with one or more horizontal perforated screens bored under an angle (typically inclined at 15 to 20 degrees) and extending from the surface entry point underground past the mean tide line at a minimum depth below the sea floor of 5 to 10 meters.

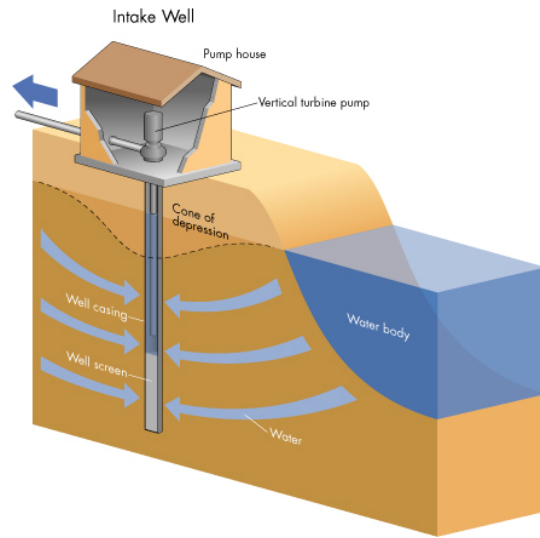


Figure 2.2 Vertical intake well

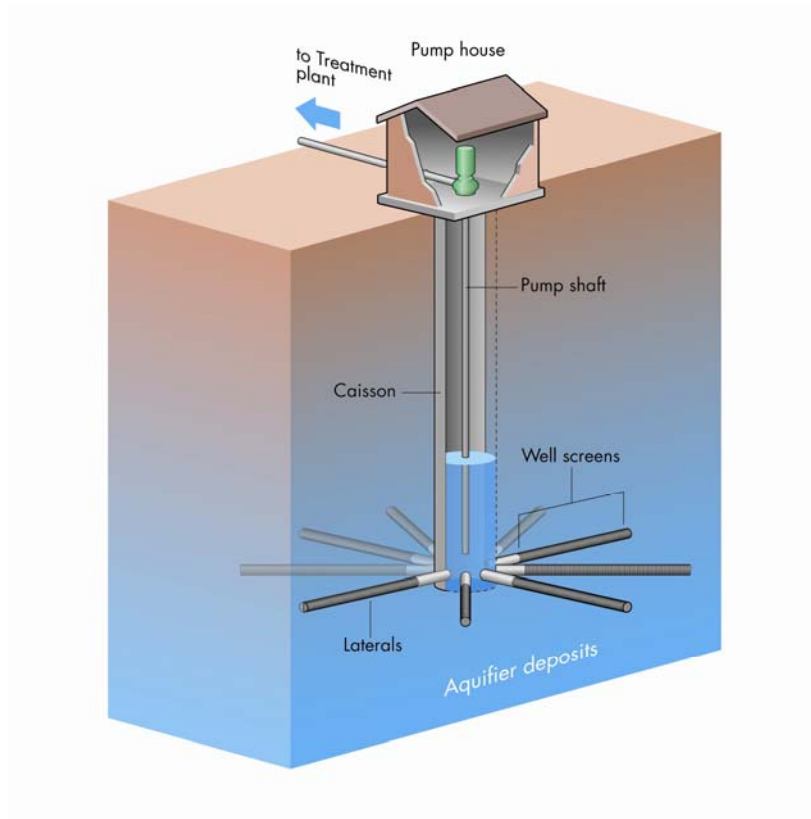


Figure 2.3 Horizontal intake well

Open ocean intakes are suitable for all sizes of seawater desalination plants, but are typically more economical for plants of production capacity higher than 20,000 m³/day. Open intakes for large seawater desalination plants are often complex structures including intake piping which typically extends several hundred to several thousand meters into the ocean. Source water collected through open intakes usually requires pre-treatment prior to reverse osmosis desalination. The cost and time for construction of a new open ocean intake could be significant and could reach 10 to 20 percent of the overall desalination plant construction cost. Open ocean intakes would result in some entrainment of aquatic organisms as compared to beach wells because they take raw seawater directly from the ocean rather than source water pre-filtered through the coastal sand formations. Sub-seabed horizontal intakes have the benefit of providing some filtration pre-treatment while causing minimal entrainment of marine life and having limited aesthetics impact on shoreline (Peters, 2006).

Raw seawater collected using wells is usually of better quality in terms of solids, slit, oil & grease, natural organic contamination and aquatic microorganisms, as compared to open seawater intakes. Well intakes may also yield source water of lower salinity than open intakes. They, however, have the potential for altering the flows of hydraulically connected freshwater aquifers and possibly accelerating seawater intrusion into these aquifers. Use of subsurface intakes for large desalination plants may be limited by a number of site-specific factors that should be taken under consideration when selecting the most suitable type of intake for a particular project (Voutchkov, 2004).

Issues and considerations

Water quality

A thorough raw water characterization at the proposed intake site(s) must include an evaluation of physical, microbial and chemical characteristics, meteorological and oceanographic data, and aquatic biology. An appropriate intake design must also consider the potential effects of fouling, continuous or intermittent pollution, and navigation, and take necessary steps to mitigate these source water contamination, environmental and operational risks. Seasonal variations should also be characterized and understood, preferably before the desalination plant is designed and built. Chapter 5 (Monitoring) provides a detailed description of suggested water quality monitoring needs for desalination plants.

Like most process systems, desalination plants operate most efficiently and predictably when feedwater characteristics remain relatively constant and are not subject to rapid or dramatic water quality fluctuations. Therefore, the water quality review should consider both seasonal and diurnal fluctuations. The review should consider all constituents that may impact plant operation and process performance including: water temperature, total dissolved solids (TDS), total suspended solids (TSS), membrane scaling compounds (calcium, silica, magnesium, barium, etc.) and total organic carbon (TOC). Desalination intake water requirements and quality vary based on the desalination process employed. Feedwater volume requirements generally range from approximately 25% more than the production capacity of some brackish water reverse osmosis (BWRO) plants to two times the plant production capacity for seawater reverse osmosis (SWRO) systems. Because they have both process and cooling water requirements, thermal seawater desalination systems often require more than ten times the distillate production. The

necessary feedwater must be available whenever a plant is operating if the plant is to meet productivity goals.

In addition to the permeability, productivity, and safe yield of the source water aquifer, the key factor that determines the location and feasibility of the intake for brackish water desalination plant is the raw water quality. Plant failure can be caused by large changes of intake water salinity, and variations or elevated concentration of water quality contaminants such as silica, manganese, iron, radionuclides, or scaling compounds that may create fouling or operational problems which increase treatment costs or limit the available options for concentrate disposal. Subsurface geologic conditions determine to great extent the quantity and quality of the raw water. Confined or semi-confined aquifers yield the most suitable source of water for brackish water desalination systems (Missimer, 1999).

Whenever groundwater is pumped from an aquifer, there is always some modification of the natural flow in this aquifer. Some brackish water aquifers are density stratified and when water is pumped from the top portion of the aquifer, higher salinity groundwater propagates upwards increasing source water salinity over time. Many brackish water aquifers are semi-confined and they may have a common boundary with other aquifers of different water quality. When the production aquifer is pumped, a certain portion of the recharge volume to this source water aquifer may be supplied from the adjacent bounding aquifers, thus causing a change of source water quality from that of the original aquifer to the water quality of the bounding aquifers over time. These changes in source water quality over time may not only affect the intake water salinity but also the overall ion make up of the source water for the brackish water desalination plant which may affect the systems allowable recovery and may also affect concentrate disposal permitting. Therefore, it is essential to conduct pre-design hydrogeological investigation that includes predictive modelling of the potential long-term changes in source water quality that could occur over the useful life of the subsurface intake system. Protection of freshwater aquifers is an essential consideration.

Impacts on aquatic life

Environmental impacts associated with concentrate discharge have historically been considered the greatest single ecological impediment in selecting the site for a desalination facility. However, aquatic life impingement and entrainment by the desalination plant intake are more difficult to identify and quantify, and may also result in measurable environmental impacts.

Impingement occurs when aquatic organisms are trapped against intake screens by the velocity and force of flowing water. Entrainment occurs when smaller organisms pass through the intake screens and into the process equipment. The results of impingement and entrainment vary considerably with the volume and velocity of feedwater and the use of mitigation measures developed to minimize their impact. Impingement and entrainment of aquatic organisms are not environmental impacts unique for open intakes of seawater desalination plants. Conventional freshwater open intakes from surface water sources (i.e., rivers, lakes, estuaries) may also cause measurable impingement and entrainment. There are a number of surface and subsurface intake options that may be employed to mitigate these and other environmental considerations, and all options should be thoroughly examined.

Water discoloration, and taste and odour issues associated with anaerobic wells

Some seawater and brackish water wells draw their water supply from anaerobic aquifers which may contain hydrogen sulfide (H₂S). In these instances, the feedwater intake and conveyance systems should remain pressurized to prevent the formation of elemental sulphur. After desalination, product water must be degasified to prevent taste and odour problems. Some brackish waters from anaerobic wells may contain large amounts of iron and manganese in reduced form. Exposure to oxygen may oxidize the iron and manganese salts and discolour the source and product water. In this case, the source water should be treated with greensand filters to oxidize and remove iron and/or manganese salts under controlled conditions.

Biofouling

All natural water systems contain a wide range of microorganisms that can cause operational problems, if not controlled. These organisms grow predominantly in slime-enclosed biofilms attached to surfaces. Biofilms may form very rapidly, restricting the flow of water through a membrane. The formation of a biofilm of microorganisms on the surface of the desalination membranes of SWRO and BWRO plants and on the contact surfaces of thermal desalination plants such as to cause a measurable reduction of the production capacity of the desalination system is typically referred to as biofouling. Although most aquatic organisms typically causing biofouling are not pathogens, their excessive growth could have a negative effect on desalination plant's overall performance and efficiency. Once a biofilm establishes itself and fouls a membrane, it may be extremely difficult, or even impossible to remove. Desalination plants with open intakes typically incorporate facilities for biofouling control which include the use of chlorine or other oxidants or biocides to control excessive bio-growth. Thermal desalination plants usually practice continuous chlorination, while most membrane system practice intermittent or shock chlorination.

Aquatic organisms, including mussels, barnacles, clams and mollusks may grow in intake channels, pipes and equipment, causing operational problems. Open intake systems are usually equipped with provisions for hindering of bio-growth and periodic removal of aquatic organisms from the plant intake facilities in order to maintain reliable and consistent plant performance.

Co-location of desalination plants and power generation facilities

Because power generation plants require large volumes of cooling water to condense power-cycle steam, desalination facilities often consider co-location with a power plant with which they can share a common intake. The avoided cost of constructing and permitting a new intake may reduce the capital cost of a large desalination facility by several million dollars. A more detailed description of the co-location configuration is provided in the *Concentrate Management* section of this Chapter. However, entrainment considerations with once-through power plant cooling systems may affect the permitting of co-located desalination facilities. Power plants and desalination facilities proposing to share seawater intakes must identify how the operation of both the power plant and desalination plant will be coordinated to minimize impingement and entrainment.

A number of recent studies indicate that the incremental entrainment effect of desalination plant intakes co-located with once-through power plants is minimal. For example, the entrainment study completed for the 200,000 m³/day Huntington Beach Seawater

Desalination Project in California, USA and included in the environmental impact report (EIR) for this project (City of Huntington Beach, 2005) has determined that the co-location of this plant with the existing AES Power Generation Station allows reducing the additional entrainment effect attributed to the desalination plant intake to less than 0.5 %. A similar EIR study in Carlsbad, California, USA (City of Carlsbad, 2005), shows that the maximum entrainment potential of the proposed 200,000 m³/day seawater desalination plant is reduced to less than 1 % as a result of the co-location of this plant's intake with the Encina Power Generation Station's discharge. In both cases, because the desalination plants use warm cooling water collected from the power plant discharge and do not have a separate new open ocean intake and screening facilities, they do not cause an incremental impingement of aquatic organisms.

2.4 Pretreatment processes

2.4.1 General description

The pre-treatment process improves the quality of the raw feedwater to ensure consistent performance and the desired output volume of the desalination process. Almost all desalination processes require pre-treatment of some kind. The level and type of pretreatment required depends on the source and quality of the feedwater and the chosen desalination technology. For source water of poor quality, pretreatment can be a very significant portion of the overall plant infrastructure. The potential influences on public health and the environment from the pre-treatment process operations are associated with the chemical conditioning (addition of biocides, coagulants, flocculants, antiscalants, etc.) of the source water prior to pre-treatment and with the disposal of the residuals formed during the pre-treatment process. Pretreatment, when required, normally involves a form of filtration and other physical-chemical processes whose primary purpose is to remove the suspended solids (particles, silt, organics, algae, etc.) and oil and grease contained in the source water when membrane desalination is used for salt separation. For thermal desalination processes it protects downstream piping and equipment from corrosion and from formation of excessive scale of hard deposits on their surface (scaling). Biofouling is most often mitigated using an oxidant although non-oxidizing biocides are also utilized. Potential public health effects associated with pre-treatment are typically associated with the by-products formed during the chemical conditioning process and their potential propagation into the finished fresh water.

Screening of the intake water is the first step of the treatment process. The primary function of pretreatment is to ensure that turbidity/suspended solids and the quantity of organic and inorganic foulants are within the acceptable range for the desalination process equipment. Secondary functions may include the removal of other unwanted constituents that may be present (continuously or intermittently) such as hydrocarbons or algae.

2.4.2 Pretreatment for thermal desalination plants

For thermal desalination facilities the pretreatment process must address:

- Scaling of the heat exchanger surfaces primarily from calcium and magnesium salts (acid treated plants);

- Corrosion of the plant components primarily from dissolved gases;

Physical erosion by suspended solids;
Effects of other constituents such as oil, growth of aquatic organisms and heavy metals.

Thermal desalination systems are quite robust and normally do not include any physical treatment other than what is provided by the intake (i.e. no additional filters or screens). Chemical conditioning is utilized in thermal desalination in two treatment streams: the cooling water (which is the larger flow and generally returned to the feed source), and make up water (used within the desalination process). Cooling water is normally treated to control fouling using an oxidizing agent or biocide. The make up water is continuously treated with scale inhibitors (usually a polymer blend) and may be intermittently dosed with an anti-foam surfactant (typically during unusual feed water conditions).

2.4.3 Chemicals used in thermal desalination processes

Table 2.1 profiles chemicals which are most frequently used in seawater pre-treatment for thermal desalination. Dose rates are only indicative and are shown as mg/litre of chemical in the relevant process stream (MU = Make Up Water, CW = Cooling Water).

Table 2.1 Chemicals used in thermal desalination processes

Chemical Type	Purpose of Use	Dose And Feed Location	Application
Scale inhibitor (Usually phosphonates, polyphosphate, polymaleic or polycarboxylic acids, or a blend of several of these)	Usually crystal modifiers that avoid precipitation and development of deposits (primarily CaCO ₃ , Mg (OH) ₂ . Blends may include dispersant properties to prevent crystals adhering to equipment.	1-8 mg/litre, MU	Used in all thermal desalination processes.
Acid (usually sulphuric acid),	An alternative scale inhibitor. By lowering pH calcium carbonate and magnesium hydroxide scale formation is avoided.	≈100 mg/litre, MU	Used only in MSF desalination.
Antifoam (Poly Othelyne Ethylene Oxide or similar surfactant)	Uncorrected foaming due to unusual feed water conditions may overwhelm the process indicated by high product TDS (carryover).	≈0.1 mg/litre, MU	Used intermittently in all thermal processes but primarily MSF.
Oxidizing Agent: most often a form of chlorine, however biocides may have some use, particularly for smaller systems.	To control bio-fouling and aquatic organism growth in the intake and desalination equipment. Continuous dosing of 0.5-2 mg/L active Cl ₂ with intermittent shock dosing (site specific but may be 3.7 mg/L for 30-120 minutes every 1-5 days).	≈1.0 mg/litre, CW	Used for large surface and sea water intakes.

Sodium bisulfite.	Oxygen scavenger to remove traces of residual oxygen or chlorine in the brine recirculation.	≈0.5 mg/litre, MU	Used only in MSF desalination systems and in intermittent mode.
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2.4.4 Source water pretreatment for membrane desalination

Membrane desalination is used to desalinate water from many sources including brackish surface water from rivers and lakes, brackish groundwater from wells, municipal and industrial wastewater, and seawater from open ocean intakes and beach wells. Because of the great variability of the water quality depending on its source (brackish water or seawater) and the type of intake (open or subsurface) simple generalizations about pre-treatment requirements are not definitive.

For membrane desalination facilities the pre-treatment processes must address:

- Membrane fouling and scaling from metal oxides, colloids, and inorganic salts;
- Fouling or plugging by inorganic particles;
- Biofouling by organic materials;
- Chemical oxidation and halogenation by residual chlorine;
- Chemical reduction of chlorine
- Effects of other constituents such as oil, aquatic organisms and heavy metals.

Membrane desalination requires a higher degree of pre-treatment than thermal desalination processes. Membrane separation technologies were developed for the removal of dissolved salts but they also block the passage of filterable materials. Membranes are not designed to handle high loads of filterable solid materials and presence of suspended solids in the source water can reduce the quality and quantity of water produced, or lead to shorter than anticipated membrane life and inferior membrane performance. Filterable solid materials are removed by the pre-treatment process to achieve low content of suspended solids and silt in the water, which is measured by a cumulative parameter called silt density index (SDI). SDI values of the source water are indicative of its membrane fouling tendency and are calculated using a procedure which includes filtration of water sample, at constant pressure, through a 0.45 µm filter. Generally most membranes require feedwater with an SDI of less than 5 in order to maintain steady and predictable performance.

2.4.5 Chemicals used for pretreatment prior to membrane desalination

Table 2.2 profiles some chemicals that are used for pre-treatment of the source water prior to membrane desalination. Some chemicals are used continuously to optimize operations while others are used intermittently for cleaning of the filtration media of the pre-treatment system. Dose rates are only indicative and are shown as milligrams of chemical per litre of feedwater.

Table 2.2 Pretreatment chemicals used in membrane desalination systems

Chemical Type	Purpose of Use	Dose	Application
Scale inhibitors (polyelectrolyte polymer blends).	Increase of solubility of sparingly soluble salts such as calcium and magnesium carbonates and sulfates. Additional chemicals may be used to target specific species, such as silica.	≈2-5 mg/litre	Primarily in brackish water desalination and water reclamation using RO and ED/EDR operating at high recoveries.
Acid (usually sulfuric acid).	Reduction of pH for inhibition of scaling and for improved coagulation.	40-50mg/litre as required to reduce pH to ≈6-7	Primarily in seawater RO applications. Not used in all applications.
Coagulant (usually ferric chloride or ferric sulphate).	Improvement of suspended solids removal.	5 -15 mg/litre	Primarily in open intake seawater RO and surface water RO systems.
Flocculant Aid (usually cationic polymer).	Improvement of suspended solids removal.	1-5 mg/litre	Primarily in open intake seawater RO and surface water RO. May only be used intermittently when feed SDI is unusually high.
Oxidizing Agent: most often a form of chlorine. However biocides have found some use, particularly in smaller systems.	To control bio-fouling and aquatic organism growth in the intake and pre-treatment facilities. Chloramines may be used for pre-treatment in reclamation systems and their use should be avoided in seawater desalination systems.	Site specific but may be 3.7mg/litre for 30-120 minutes every 1-5 days	Used for large surface and sea water intakes. Small systems and those using wells, especially those in which source water is anaerobic may not require oxidation.
Reducing agent (usually a form of bisulfite); function of chlorine dosage	To eliminate oxidizing impacts on the RO membrane.	Generally 2 to 4 times higher than oxidizing agent dose.	In all membrane processes using polyamide RO membranes (Less common cellulose acetate membranes have greater tolerance of oxidants).
Membrane preservation and sterilization	Off line membranes must be sterilized and preserved. Sterilization may utilize hydrogen peroxide. In some cases acetic acid is also used to create peracetic acid. Preservation most commonly utilizes sodium bisulfite.		

The chemicals listed above are typically used for conventional granular media pretreatment systems. Microfiltration (MF) or ultrafiltration (UF) membrane systems can also be used as a pretreatment to desalination. Although typically the use of MF and UF pre-treatment systems does not require source water conditioning, these systems use significant amount of chemicals for chemically enhanced backwash (CEB) and cleaning of the pretreatment membranes. Typically, CEB is practiced once to two times per day, while deep chemical cleaning of the MF/UF membranes is completed every 60 to 90 days. Table 2.3 summarizes the type of chemicals used for membrane pretreatment.

Table 2.3 Chemicals used for cleaning membrane pretreatment systems

Chemical Type	Purpose of Use	Dose	Application
Acid (usually citric, phosphoric or hydrochloric acid)	Cleaning of solids and biological material from membrane filtration.	Batch size is a function of process train size. Frequency of batches is a function of number of process trains and site specific conditions.	MF/UF Membrane CEB and Periodic Cleaning.
Sodium hypochlorite	Cleaning biological material from membrane filtration.	Batch size is a function of process train size. Frequency of batches is a function of number of process trains and site specific conditions.	MF/UF Membrane CEB.
Phosphates (tri-polyphosphate or similar)	Cleaning of membranes	Batch size is a function of process train size. Frequency of batches is a function of number of process trains and site specific conditions.	Periodic MF/UF Membrane Cleaning.
EDTA	Cleaning of membranes	Batch size is a function of process train size. Frequency of batches is a function of number of process trains and site specific conditions.	Periodic MF/UF Membrane Cleaning.
Specialty cleaning chemicals	Unusual deposits on membrane surfaces may be removed, off line, using specific chemicals and treatments specified by the membrane manufacturers.	This may not only be off-line but in some cases off-site.	Periodic MF/UF Membrane Cleaning.

All chemicals utilized in the membrane desalination applications should always have an appropriate certification and quality control suitable for use in drinking water. Typically specialized governmental, public or private organizations certify products to those standards.

2.5 Thermal Desalination Processes

When saline solutions are boiled, the escaping vapour consists of pure water soluble gases and volatile organics (which are vented) while the salts and some organics remain in the unevaporated solution. The evaporation-based salt separation process yields water of very low salt content (usually below 5 mg/litre of TDS) but the *latent heat* required to evaporate the water is high. As a result several process configurations have been developed in an attempt to minimize energy consumption. The two most widely used thermal desalination processes are multistage flash distillation (MSF) and the multiple effect distillation (MED). Both, MSF and MED can be used for desalinating seawater and brackish water. However, majority of the existing MSF and MED plants seawater desalination facilities.

2.5.1 MSF Desalination

Until the early 1990's, multistage flash distillation was the most commonly employed method of seawater desalination. In the MSF process, a stream of heated seawater flows through the bottom of the vessel containing up to 40 chambers or stages, each operating at a slightly lower pressure than the previous one (Figure 2.4).

The lower pressure causes the hot seawater to begin boiling immediately upon entering each new stage. The rapid, violent boiling action triggers a portion of the seawater to instantly vaporize, or *flash* into steam. The flashing process cools the concentrated seawater and allows it to reach thermodynamic equilibrium with its new surrounding. Flashed vapour rises rapidly, passing through (wire mesh) demister pads to remove any entrained brine droplets. The cleansed vapour then passes around the outside of tube bundle carrying cool seawater, where it is condensed into pure, distilled water. Distillate is collected in a trough and flows into the distillate section of the following stage. Because the stage is operating at a lower pressure, a small portion of the distillate flashes in a manner similar to the concentrated seawater. This flashing reduces the temperature of the distillate until it reaches the last stage of the process where its temperature is usually >3 to 5°C warmer than the seawater.

Oxygen, carbon dioxide, and other gases dissolved in seawater are released during the evaporation process. The vacuum in which the system operates may also draw air into the effects through small leaks in the vessel walls. If these *non-condensable gases* (NCG) are allowed to accumulate, within the system, they may hinder heat transfer by a process known as *gas blanketing*. A venting system must be incorporated within the system to ensure the NCGs are continually swept away from the heat transfer surfaces. The venting systems usually use a combination of steam jet ejectors and small condensers to completely evacuate the NCGs to the atmosphere.

Multistage Flash with Brine Recirculation

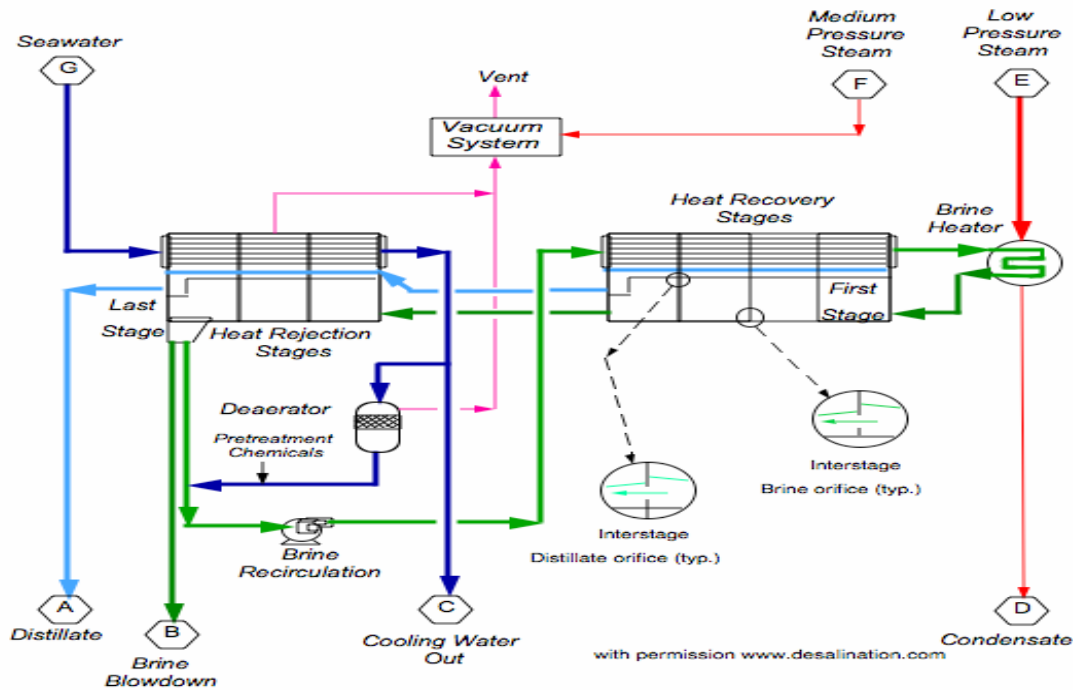


Figure 2.4 Schematic of a typical MSF thermal desalination system

MSF distillation is considered a *forced circulation* process because pressure inhibits evaporation of the hot brine until it passes through an orifice into a chamber below its boiling temperature. Upon entering the lower pressure chamber, a portion of the brine instantly flashes to vapour without the addition of heat. The vapour is naturally drawn towards the cooler tube surfaces where it is condensed. The *heat of condensation* passes through the tubes, heating the seawater inside. The stage remains at a constant temperature and pressure and is essentially self-regulating. The seawater temperature increases progressively as it passes through the tubes, stage-by-stage, until it reaches first – and hottest – stage. From stage 1, the preheated seawater enters a separate steam condenser, or *brine* or *feedwater heater*, where motive steam from a boiler or other source is used to heat the seawater to the *top brine temperature (TBT)*, which is typically 90° to 115°C. The pressure within the feedwater heater ensures that no boiling or flashing occurs before the hot seawater is re-introduced to the *shell side* of the tubes in the first stage. At this point, the brine flow resembles a turbulent, rapidly flowing river that may be up to 20 m wide and 100 m long in the largest MSF systems. Most plants occupy a single level but several have double levels, or decks, as a method to reduce the plot area.

Large scale MSF systems are used for municipal water supply, often in dual purpose power and water cogeneration facilities. Steam from back-pressure or condensing turbines typically provide the heat to drive the process. These systems are used in applications where there is a large demand for water coincident with a relatively large amount of (waste) heat.

Large systems produce between 10,000 and 65,000 cubic meters of water per day from each machine.

MSF desalination issues and considerations

The cooling water returned to the sea is generally 8-12°C warmer than the ambient conditions. It is not de-aerated and may contain small quantities of corrosion or disinfection by-products. MSF systems generally produce distilled water with a TDS of between 2 and 50 mg/litre. The distillate TDS comes from solids carryover or possible joint leakage or tube failure allowing bypassing of the separation process. The integrity of the tubes and joints can be checked and confirmed by hydro-testing, however failures are readily identified by rapid increases in distillate TDS. NCG gases are re-dissolved in the distillate, the primary impact of which is the reduction of pH to around 6.2 (due to CO₂). The small number of facilities which use acid to solubilize metal salts for scale control will produce distilled water with a more neutral pH. There is also the potential to distil volatile materials that may be in the feedwater source, unless these are removed by the external pre-treatment process or the de-aeration step, which is an integral part of an MSF system.

The process concentrate, frequently referred to as brine, is returned to the source (usually the sea). Most commonly the brine is blended with cooling water from the MSF process (as well as cooling water from other processes if available). The brine contains scale-inhibitor and anti-foam chemicals and is generally considered de-aerated (prior to blending with cooling water). The brine TDS concentration is generally 1.4 to 1.8 times higher than the raw seawater/make-up. The brine temperature is usually >3 to 5°C warmer than the ambient seawater (before blending with cooling water).

There is no direct contact between the heating steam system and the desalination process. Steam condensate does not mix with the seawater, the brine or the distilled water. However, in some systems there can be a vent connection between the steam system and the vapour space above the flashing brine which can introduce approximately 0.5-1.0% of the steam flow into the MSF process; vapour contaminants should be swept into the vacuum system. This vent connection provides useful heat recovery but usually can be (at some reduction in efficiency) directed to the more isolated vacuum system if the steam is suspected of containing contaminants. Condensate drains from the vacuum system could also contain dissolved or absorbed contaminants from seawater decomposition and/or from steam. These drains sometimes connect into the brine side of the process (for some minimal heat recovery prior to rejection from the process) however they can also be directly rejected if required. Similarly there should be consideration of possible contamination for special heat recovery systems (such as drain coolers) that while not common may still be utilized.

These systems can be manufactured from a variety of materials but alloys of copper and nickel and various molybdenum bearing grades of austenitic stainless steels predominate. Limits are normally placed on corrosion by-products detectable in the distilled water primarily to ensure equipment longevity. Copper and iron are often measured as trace substances in the distillate with limits of 0.02 mg/litre and 0.02 mg/litre respectively. Parts of the seawater and brine systems of these large systems may be coated with epoxy or lined using various elastomers. Piping systems for seawater and brine are largely non-metallic with HDPE (high density

polyethylene) and GRP (glass reinforced plastic) also known as reinforced thermosetting resin pipe (RTRP) being the most common. Distilled water piping is generally stainless steel or polyvinyl chloride (PVC) or polypropylene (PP), when the temperature is appropriate. Corrosion byproducts are not typically monitored in the brine or cooling water systems because they are not expected to be contained in large quantities in these sidestreams of the thermal desalination process.

2.5.2 MED desalination

Multiple effect distillation was originally developed in the 1820s but more recently, in the 1960s, it was reconfigured to use thin film evaporation techniques, making it more practical than the original concept. In the most common configuration of this process the saline water to be evaporated is distributed over the outer surface of heated tubes. Within each MED effect, cool seawater is sprayed over a heat exchanger tube bundle while steam flowing through the tubes is condensed into pure product water. Outside the tubes, the thin seawater film boils as it absorbs heat from the steam. The resulting vapour passes through *mist eliminators* to catch entrained brine droplets before the vapour is introduced into the tubes in the next effect. The process is repeated through the length of the plant. Alternative MED configurations that employ vertical tubes or plate-type heat transfer surfaces are also available.

Similar to the MSF process, a venting system must be incorporated within the MED system to ensure the NCGs are continually swept away from the heat transfer surfaces. The venting systems usually use a combination of steam jet ejectors and small condensers to completely evacuate the NCGs to the atmosphere.

MED-TC combines a conventional MED system with a steam jet ejector, or *thermo-compressor* device. The thermo-compressor makes use of the pressure of the motive steam to recycle the heat content, or *enthalpy*, of the process vapour from the final effect. By boosting the pressure of this process vapour, it can be recycled as heating steam in the first effect. Steam with a pressure greater than 1 bar can be used in a thermo-compressor. MED-TC systems differ from both MSF and MED systems because unless special steps are taken to isolate it, the distillate can include steam condensate. This is an important consideration for drinking water systems because steam condensate may include toxic boiler treatment chemicals. Additionally even though MED-TC may use high pressure and temperature steam, the maximum temperature within the process is rarely more than 75°C. Both MED and MED-TC systems have an advantage over MSF that the clean vapour side of the process is at a higher pressure than the saline side; any loss of integrity of the heat transfer surface will lead to a generally small loss of product, not contamination of all of the product water.

Large systems produce between 5000 and 25000 cubic metres of water per day from each plant with facilities having 4-10 or more machines. Small systems of 250 – 5000 cubic meters per day are common in industrial applications and serving small or island communities. Typically, the feedwater only undergoes relatively coarse screening as a pretreatment. The cooling water returned to the source is generally 8-12 °C warmer than the feedwater temperature and it is not de-aerated but may contain small quantities of corrosion or disinfection by-products. It is possible with MED or MED-TC to configure the process to function with less cooling water,

resulting in a higher temperature rise than with MSF. If environmental limits are not imposed and applied, this process can function with a temperature rise of over 20°C.

A portion of the cooling water return is used for make-up to the desalination process. This make up water flow rate is generally 3 to 4 times the desired production rate of distilled water. A scale inhibitor may be added to minimize deposition of mineral scale within the system. The scale-inhibiting chemicals are usually phosphate, polyphosphate or polymaleic acids and are dosed at 1 to 5 mg/litre. Periodically, anti-foaming surfactants may be added to counteract seasonal changes in the feedwater. The most common anti-foaming agent is polythelyne ethylene oxide which is added at rates of 0.1-0.2 mg/litre. In the process the make-up water is heated to a top brine temperature of between 60 and 75°C before being boiled (in successively lower pressure stages) to release water vapour which can then be condensed and collected.

The separation process is primarily boiling evaporation with agglomeration systems (demisters) to collect and remove liquid carry over from the system. MED/MED-TC systems generally produce distilled water with a TDS of between 20 and 50 mg/litre. The distillate TDS comes from solids carry-over from the separation process (or less likely from joint leakage or tube failure within the main or vacuum system condensers allowing bypassing of the separation process). The integrity of the tubes and joints is not usually considered an issue with most MED/MED-TC configurations because the distilled water side of the process is generally higher pressure than the saline side. The process releases dissolved gases from the seawater; these include air and carbon dioxide. The gases are vented to atmosphere from the process (otherwise they would impede heat transfer) and are generally not considered harmful. These gases are also re-dissolved in the distillate as predicted by Henry's Law. The primary impact of this is the reduction of pH to around 6.2 due to high CO₂.

The concentrate, frequently referred to as brine, is returned to the sea. Most commonly the brine is blended with cooling water from the MED/MED-TC process (as well as cooling water from other processes if available). The brine will contain scale-inhibitor and anti-foam chemicals and is generally considered de-aerated (prior to blending with cooling water). The brine TDS concentration is typically 1.4 to 1.8 times higher than the raw seawater/make-up. The brine temperature is usually 15°C higher than the seawater before blending with cooling water.

MED issues and considerations

The cooling water returned to the sea is generally 8-12 °C, or more, warmer than the ambient conditions it is not normally de-aerated but may contain small quantities of corrosion or disinfection by-products. MED systems generally produce distilled water with TDS concentration between ~20 and 50 mg/litre. The distillate TDS content typically originates from solids carryover but has a lower probability of arising from joint leakage or tube failure than other thermal processes. NCG gases are re-dissolved in the distillate the primary impact of this is the reduction of pH to around 6.2 (due to CO₂). Volatile materials in the feedwater source are also distilled.

The feedwater concentrate (brine), is returned to the source (usually the sea). Most commonly the brine is blended with cooling water from the MED process (as well as cooling

water from other processes if available). The brine typically contains scale-inhibitor and anti-foam chemicals and is de-aerated (prior to blending with cooling water). The brine TDS concentration is generally 1.4 to 1.8 times higher than the raw seawater/make-up. The brine temperature is usually 5-25°C warmer than the seawater (before blending with cooling water).

There is no direct contact between the heating steam system and the MED desalination process, however there is with the MED-TC process. Steam condensate does not mix with the seawater, brine or distilled water. In systems which utilize steam which may contain low-grade treatment chemicals a steam transformer or reboiler must be incorporated into the design. Condensate drains from the vacuum system could also contain dissolved or absorbed contaminants from feedwater decomposition and/or from steam. These drains sometimes connect into the brine side of the process (for some minimal heat recovery prior to rejection from the process). However, they can also be directly rejected if required.

As with MSF facilities, these systems can be manufactured from a variety of materials, but are usually constructed out of copper, nickel and various molybdenum bearing grades of austenitic stainless steels. Limits are normally placed on corrosion by-products detectable in the distilled water primarily to ensure equipment longevity. Copper and iron are often chosen as trace substances in the distillate with limit of 0.02 mg/litre and 0.02 mg/litre respectively. Parts of the seawater and brine systems of these plants may be coated with epoxy, or lined using various elastomers.

2.6 Membrane desalination

Membrane desalination is a process of separation of minerals from the source water using semi-permeable membranes. Two general types of technologies are currently applied for membrane desalination - reverse osmosis (RO) and electrodialysis (ED).

2.6.1 Desalination by electrodialysis

In electrodialysis-based treatment systems, the separation between water and salt is achieved by passing a direct current (DC) through the ion bearing water, which drives the ions in the source water through membranes to electrodes of opposite charge. A commonly used desalination technology which applies the ED principle is electrodialysis reversal (EDR). In EDR systems, the polarity of the electrodes is reversed periodically during the treatment process.

The ED based systems use ion-transfer (perm-selective) anion and cation membranes to separate the ions in the source water. These membranes are essentially ion exchange resin cast in sheet form of thickness of 0.5 mm. The membranes allow a unidirectional transfer of ions of a given charge through them, e.g. the cation-transfer membranes allow only positively charged ions to pass (This process is shown in its simplest form in Figure 2.5). The water flows across, not through, the membrane surfaces, and ions are electrically transferred through the membranes from the source water stream to the concentrate stream under the influence of the DC current. Desalted water is produced in the compartments on the left of the anion membrane, A.M., in the drawing and concentrate in the compartments on the right.

The energy use for ED desalination is directly proportional to the amount of salt removed from the source water. TDS concentration and source water quality determine to a great extent

which of the two membrane separation technologies (RO or ED) would be more suitable and cost-effective for a given application. Typically, ED membrane separation is found to be cost-competitive for source waters of TDS concentration lower than 3,000 mg/litre (FAO, 2005).

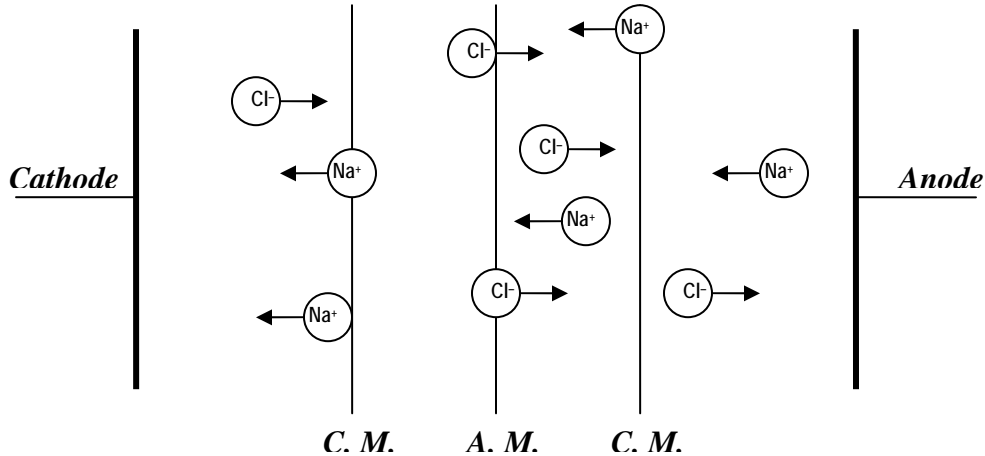


Figure 2.5 – General schematic of an electro dialysis system

2.6.2 Reverse osmosis desalination

Reverse osmosis is a process where the product water (permeate) is separated from the salts in the source water by pressure-driven transport through a membrane. As a result of the RO process, desalinated water is transported under pressure through the membrane while the minerals of the source water are concentrated and retained by the membrane. Applying high pressure for desalination is mainly needed to overcome the naturally occurring process of osmosis, which drives the desalinated water back through the membrane into the water of more concentrated mineral content. Nanofiltration (NF) is a process similar to RO where membranes with order of magnitude larger pore size are used to remove high molecular weight compounds and polyvalent ions that cause water hardness (i.e. calcium and magnesium).

Membrane desalination processes use semi-permeable membranes — with pumping pressure as the driving force — to separate a saline feedwater into two streams: low-salinity product (permeate), and a high-salinity stream (concentrate or reject). Although not technically correct, the concentrated reject stream is often referred to as *brine*. Reverse osmosis (RO) is not a true filtration process because dissolved salts and other matter are not removed solely because of their size. This process relies on the ability of water molecules to *diffuse* through the membrane more readily than salts and higher molecular weight compounds. The membrane is the heart of an RO or NF system, and it is the barrier by which dissolved solids separation is accomplished. The membranes are made of long chain high molecular weight organic *polymers*, which have an affinity for water. This hydrophilic characteristic allows water molecules to readily diffuse, or *permeate* through the membrane structure, while restricting the passage of other substances. Three characteristics are commonly used to describe membrane performance: flux, salt rejection, and recovery:

A membrane's **permeate flux** is the rate at which it will diffuse water molecules and dependent on the membrane characteristics (i.e., thickness and porosity), and system operating conditions (i.e., feed pressure, temperature, and salt concentration). It is expressed in terms of flow rate per unit area (i.e., litre/sq meter/hr (lmh); gallon per day per square foot (gpd/ft²)). Similarly, the rate at which salts or other solutes diffuse through a membrane is referred to a salt flux. The salt flux is proportional to the concentration difference between the feed and permeate solutions.

Salt rejection refers to the effectiveness of a membrane to remove salts from a solution. The salt rejection varies slightly for specific ions, and the total rejection is determined by dividing the difference in feed and product water salt concentrations by the feedwater concentration.

The proportion of feedwater that is recovered as product water is referred to as the **permeate recovery or conversion**. As system's recovery rate increases, so does the reject stream salt concentration, and consequently the osmotic pressure.

RO modules (units) can be arranged in various *arrays* to satisfy different application requirements. The simplest configuration is a single module. As the capacity of the system increases additional modules can be added in parallel. The system performance in terms of product water quality and recovery ratio will be essentially identical to a system having a single module. To obtain higher recovery ratios or to produce higher quality product water, it is often possible to arrange a system so that the concentrate or product from one stage becomes feedwater for a subsequent stage.

RO membrane desalination plants include the following key components: source water intake system; pretreatment facilities; high-pressure feed pumps; RO membrane trains, energy recovery, and a desalinated water conditioning system. The source water intake system could be an open surface water intake or series of seawater beach wells or brackish groundwater wells. Depending on the source water quality, the pretreatment system may include one or more of the following processes: screening, chemical conditioning, sedimentation and filtration. Figure 2.6 shows a typical configuration of a seawater RO membrane system. The filtered water produced by the plant's pretreatment system is conveyed by transfer pumps from a filtrate water storage tank through cartridge filters and into the suction pipe of the high pressure RO feed pumps. The cartridge filters are designed to retain particles of 1 to 20 microns which have remained in the source water after pretreatment. The main purpose of the cartridge filters is to protect the RO membranes from damage. The high pressure feed pumps are designed to deliver the source water to the RO membranes at pressure required for membrane separation of the fresh water from the salts (typically 15 to 35 bars) for brackish source water and 55 to 70 bars for seawater. The actual required feed pressure is site-specific and is mainly determined by the source water salinity and the configuration of the RO system.

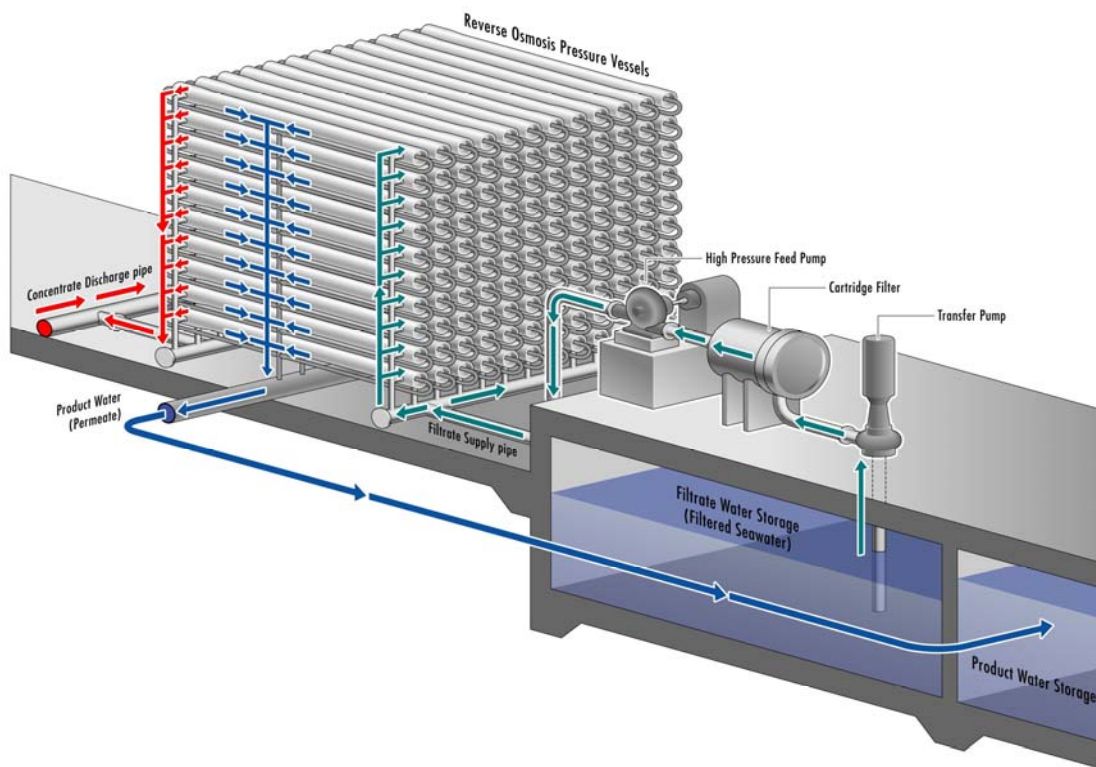


Figure 2.6 – RO membrane train with a high pressure pump

The most widely used type of RO membrane elements consist of two membrane sheets glued together and spirally wound around a perforated central tube through which the desalinated water exits the membrane element. The first membrane sheet, which actually retains the source water minerals on one side of the membrane surface, is typically made of thin-film composite polyamide material and has microscopic pores that can retain compounds of size smaller than 200 Daltons. This sheet however, is usually less than 0.2 microns thin and in order to withstand the high pressure required for salt separation, it is supported by a second thicker membrane sheet, which is typically made of higher-porosity polysulfone material that has several orders of magnitude larger pore openings.

The commercially available membrane RO elements are of standardized diameters and length, and salt rejection efficiency. For example, the RO membrane elements most commonly used for drinking water production in large-scale plants have 8-inch (~20.3 cm) diameter, 40-inch (~101.6 cm) length and can reject 99.5 % or more of the TDS in the source water. Typically SWRO membranes provide complete rejection of algal toxins, such as saxitoxin and domoic acid, as well as most man-made source water pollutants (pharmaceuticals, cosmetic products, etc.). These membranes can typically achieve over 4 logs of removal of *Giardia*, *Cryptosporidium*, viruses and other pathogens in the source water. Desalination technologies are usually more effective than conventional water treatment technologies (sedimentation, filtration, chlorination) in removing pathogens and man-made pollutants from source water. In addition,

typically seawater and source water from deep brackish aquifers is usually less polluted than most surface water resources (rivers, lakes or estuaries) in urbanized areas.

Additional discussion of membrane rejection capabilities of various chemical contaminants is discussed in Chapter 3. Chapter 4 provides analysis of the microbiological aspects of membrane desalination and its efficiency in terms of pathogen removal.

Standard membrane elements have limitations with respect to a number of performance parameters such as: feed water temperature (45°C); pH (minimum of 2 and maximum of 10); silt density index (less than 4); chlorine content (not tolerant to chlorine in measurable amounts); and feed water pressure (maximum of 80 to 100 bars).

Membrane issues and considerations

Pretreatment

An inadequate pretreatment system may severely impact RO system performance. In fact, most RO system failures are usually the result of a poorly designed/performing pretreatment system. It is of critical importance that the pretreatment system performance is satisfactory for the service intended.

Salt rejection by RO systems

Because salt rejection varies for different ions (generally multivalent ions are rejected better than monovalent ions) and may be affected by factors such as temperature, it is important that the system design takes into consideration all chemical constituents of the feedwater. Some constituents such as boron must be carefully considered under the full range of operating conditions to ensure that the maximum permeate levels are not exceeded. In addition, membrane's salt rejection deteriorates over time and it is standard practice to design a system based on the membranes projected performance at end of their normal operating life, (3 to 5 years).

Salt removal by ED-based systems

The TDS removal efficiency of ED desalination systems is not affected by non-ionized compounds or those with a weak ion charge (i.e., solids particles, silica, organics, and microorganisms). Therefore, the ED membrane desalination processes can treat source waters of higher turbidity, and bio-fouling and scaling potential than RO systems. However, the TDS removal efficiency of ED systems is typically lower than that of RO systems (15 to 90 % vs. 99 % to 99.8 %), and they do not remove pathogens and silica from the source water. Because of these key reasons the ED-based systems have found practical use mainly for brackish water desalination and wastewater reuse for irrigation.

Membrane integrity

Inorganic fouling, biofouling and/or scaling of membranes may be so severe as to result in their premature failure. In addition, manufacturing defects or mechanical problems with membranes or o-ring connectors can allow unrestricted passage of dissolved solids which could contaminate

permeate. It is therefore important that an appropriate permeate monitoring and/or testing system be employed to detect excursions in quality indicating loss of integrity.

Hydrolysis

Some RO membranes are made of cellulose acetate (CA) and are susceptible to chemical decomposition or *hydrolysis* if the feedwater is operated outside a pH range of 3.5 to 7.5. Such systems should use acid injection to maintain an adequate pH to obtain a minimum 3 year membrane life.

Energy recovery cross-contamination

RO energy recovery devices use the hydraulic pressure of the brine to pressurize feedwater. With some devices it may be possible for the brine to leak through to the feedwater side of the device, increasing feedwater TDS. Adequate precautions should be taken to ensure that if such an event occurs, it does not increase feedwater TDS to a point that could prove detrimental to the RO operation.

2.7 Post-treatment

Product water from desalination plants is characteristically low in mineral content, alkalinity, and pH. Therefore, desalinated water must be conditioned (post-treated) prior to final distribution and use. Typically, post-treatment of product water includes one or more of the following processes:

- Stabilization by addition of carbonate alkalinity;
- Corrosion inhibition;
- Re-mineralization by blending with high mineral content water;
- Disinfection;
- Water quality polishing for enhanced removal of specific compounds (i.e., boron, silica, NDMA, etc.).

Post-treatment of permeate produced by the desalination system is needed for two key reasons: to protect public health (by disinfection and mineral addition) and to safeguard the integrity of the water distribution system. In some cases the same post-treatment process and conditioning chemicals allow achievement of both goals. For example, addition of calcium and magnesium salts to permeate provides not only essential minerals but also stabilizes the product water and thereby protects the water distribution system against corrosion.

Usually, the ultimate application dosage of any multi-purpose chemical is determined by the minimum dosage needed to achieve all purposes for which the conditioning chemical is added. If the use of the same chemical is not found to be cost effective to achieve both the public health and the corrosion protection goals, than a combination of chemicals that yield the lowest overall cost of water production may be used to meet all post-treatment goals. For example, typically calcium hypochlorite addition for disinfection meets the public health goals for pathogen inactivation and also adds some calcium. Therefore, calcium hypochlorite addition is typically combined with the feed of corrosion inhibitor to the desalination plant permeate, thereby achieving both public health and corrosion protection goals at a minimal life-cycle cost.

2.7.1 Stabilization by addition of carbonate alkalinity

The lack of carbonate alkalinity makes permeate from desalination plants very unstable and prone to wide variations in pH due to the low buffering capacity. Lack of carbonate alkalinity and calcium may also contribute to increased corrosion, since protective calcium carbonate films cannot be deposited on pipe walls. In existing systems, deficient carbonate alkalinity may cause previously deposited calcium carbonate films to dissolve. Monovalent ions such as chlorides as well as gases like hydrogen sulfide, oxygen, ammonia and carbon dioxide, may pass RO membranes to a larger degree than other ions or molecules, thus they can also contribute to corrosion potential (Seacord et al., (2003)).

Corrosion can affect many aspects of drinking water supply: pumping costs, public acceptance of treated water, disinfection efficacy and public health due to exposure to heavy metals (i.e., lead, copper, and cadmium). In conventional water treatment, corrosion is defined as the degradation of pipe or pipe materials due to a reaction with water. This reaction can be physical, chemical, and electrically or biologically induced. Similarly, in a desalinated water supply, chemical reactions primarily cause the degradation of metallic pipe that comes in direct contact with water. Chemical reactions that cause corrosion of metallic surfaces are affected by many water quality parameters, including: pH, alkalinity, calcium, hardness, chlorides, silica, phosphate, and temperature. The significance of each of these parameters is summarized in Table 2.4. Although many other water quality parameters, such as total dissolved solids, dissolved oxygen, hydrogen sulfide, sulfate and biological activity affect corrosion as well, these parameters are not the emphasis of this document as they are not unique constituents of desalinated water.

Table 2.4 Factors affecting corrosion of desalinated water

Water Quality Parameter	Significance
pH	Low pH (typically below 7.0) may increase corrosion rates High pH (typically above 8.0, but not excessively) may reduce corrosion rates
Alkalinity	Provides water stability and prevents variations in pH May contribute to the deposition of protective films Highly alkaline water may cause corrosion in lead and copper pipes.
Calcium	May deposit as a calcium carbonate film on pipe walls to provide a physical barrier between metallic pipe and water Excess concentrations may decrease the water transmission capacity of pipes.
Hardness	Hard water is generally less corrosive than soft water if calcium and carbonate alkalinity concentrations are high and pH conditions are conducive to calcium carbonate deposition. Calcium carbonate does not form on cold water lead, copper or galvanized steel pipes, but calcium hardness may assist in buffering pH at the metal surface to prevent corrosion.
Chlorides	High concentrations may increase corrosion rates in iron, lead, and galvanized steel pipes.
Silica	Can react to form a protective film when present in dissolved form.

Phosphate	Can react to form protective film.
Temperature	Can impact solubility of protective films and rates of corrosion.

2.7.2 Corrosion indexes

Water stability and corrosion potential may be characterized by parameters (corrosion indexes) indicating the potential of the desalinated water to precipitate calcium carbonate, and by parameters that address corrosivity caused by specific compounds in permeate. Calcium carbonate-based corrosion (stability) indices include: Langelier saturation index (LSI); calcium carbonate precipitation potential (CCPP); and aggressiveness index (AI). The Larson ratio (LR) is a corrosion index that does not predict calcium carbonate deposition, but rather presents a qualitative relationship between molar concentrations of chloride and sulfate to bicarbonate alkalinity concentrations, and relates that ratio to corrosion potential.

Langelier Saturation Index

The LSI is a qualitative assessment of water's potential to precipitate calcium carbonate. This index is based on the difference between the pH of the unconditioned permeate and the pH of the permeate when it is just saturated with calcium carbonate. A negative LSI indicates that the water is under-saturated (i.e., calcium carbonate will dissolve) while a positive LSI may indicate that the water is over-saturated (i.e., calcium carbonate will precipitate). However, this index does not actually account for the amount of carbonate in water. Therefore, while calculations may indicate a positive LSI, it is possible that very little calcium carbonate may precipitate.

Variations of the LSI calculation exist. The original LSI was developed to predict the potential precipitation of calcium carbonate in a specific fresh surface water source rather than for desalination permeate and has limited suitability for assessment of the corrosion potential of desalinated water (permeate). The LSI is also subject to misinterpretation due to the fact that it overestimates saturated conditions at high pH when additional carbonate may not actually be available for precipitation, which may be interpreted as highly scaling conditions when water is actually under-saturated.

Calcium Carbonate Precipitation Potential (CCPP)

As opposed to the other carbonate-based corrosion indices, the CCPP is an index that quantifies the amount of calcium carbonate that may dissolve or precipitate. The CCPP is a true indication of water's potential to deposit calcium carbonate, thus forming a protective coating on pipe walls to inhibit corrosion. This index is the most useful tool for developing corrosion control and post-treatment strategies for desalinated seawater. Positive values of the CCPP indicate the concentration of calcium carbonate that exceeds the saturated condition, while negative values denote the amount of calcium carbonate that must dissolve to reach a saturated condition. The CCPP is a function of alkalinity and is defined and discussed in detail (Rossum & Merrill, 1983; Seacord et al., 2003). A recommended range for the CCPP in desalinated water is between 4 and 10 mg/litre as CaCO₃. Higher values can be acceptable when combined with the use of calcium complexing agents, such as polyphosphate-based scale inhibitors. However, when the CCPP is too high and scale inhibitors are not used, the water transmission capacity of a pipeline may be

reduced due to excessive calcium carbonate precipitation. The CCPP has not been widely used by water treatment engineers due to the analytical complexity of hand calculation. Spreadsheet models can be used to calculate the CCPP for a wide range of water qualities (AWWA, (1996)).

Aggressiveness Index

The AI was developed for asbestos-cement (A-C) pipe with water temperatures ranging from 4 to 27°C (40 to 80°F). The AI is calculated as a function of pH, calcium concentration and alkalinity (see Schock (1991)). Waters with AI less than 10 are considered highly aggressive; AI between 10 and 12 are considered mildly aggressive; and AI greater than 12 are considered non-corrosive and depositing.

The AI has significant limitations for predicting corrosion potential in A-C pipe. AI is only an approximation of the LSI and does not indicate the true potential for calcium carbonate precipitation. Similar to LSI, AI also overestimates saturation at high pH when conditions are under-saturated. Additionally, at pH of 8 to 9, when CCPP and LSI indicate saturated conditions, the AI underestimates saturated conditions, which further indicates the limitation of this index and its application to the development of corrosion control measures for desalinated seawater.

Larson Ratio

Research completed by Larson (1970) has demonstrated that chloride and sulfate can increase both corrosion rates and iron concentrations in water when water is conveyed in ferrous metal and alloy pipes. It is important to understand the effect of chloride in particular when designing desalination systems that treat both high chloride brackish waters and seawater. Pipes used to convey water to the desalination system and permeate piping must be compatible with high chloride concentrations. PVC is typically used for low-pressure piping, while high molybdenum content (i.e., 6 to 8% or higher) stainless steel alloys are often used for high-pressure piping. However, corrosion in distribution systems cannot be prevented by material selection alone. Post-treatment is still required since distribution piping may include ferrous metals that are prone to chloride attack.

The Larson Ratio is used to determine the potential impacts of chloride (Cl⁻) and sulfate (SO₄⁻²) on iron pipe corrosion. The LR is recommended to be maintained less than 5 for municipal applications. The LR is a ratio of the molar concentrations of chloride and sulfate to bicarbonate alkalinity. This index allows accounting for the fact that although desalinated water is often higher in chlorides than other water sources, typically it has an order of magnitude lower content of sulfates, and that chlorides and sulfates both have effect on corrosion. It also indicates that the LR of the water can be reduced (i.e. corrosion rate can be diminished) by increasing the bicarbonate level in the water.

2.7.3 Corrosion control methods

Widely used corrosion control strategies include the placement of a physical barrier between water and metallic pipes to protect the pipe from the corrosive properties of water. Physical barriers include chemical precipitants such as calcium carbonate, silica, and orthophosphate. Predominantly, the precipitation of calcium carbonate on pipe walls has been used to control

corrosion of desalinated drinking water. However, the amount of calcium carbonate deposited should be closely controlled to prevent pipes from losing their capacity to convey water because too much calcium carbonate is deposited. To develop post-treatment concepts for corrosion control following desalination, it is first necessary to have treatment goals. The following goals are used as a guide for developing post-treatment strategies:

Alkalinity ≥ 40 mg/litre as CaCO_3 ;
CCPP = 4 to 10 mg/litre as CaCO_3 (without the addition of calcium complexing agents);
Larson Ratio < 5 (for steel pipelines only);
LSI = +0.5 to +1.0
Total Hardness > 50 mg/litre as CaCO_3

Alkalinity greater than or equal to 40 mg/litre as CaCO_3 is a prime goal, because experience shows that alkalinity less than this value may result in poor buffering and pH variations in water systems. CCPP is preferred as the carbonate based scale formation index since, as discussed previously, other indices provide only a qualitative assessment of carbonate deposition potential.

Decarbonation

Decarbonation may be required due to the presence of high concentrations of carbonic acid that is typically accompanied by lowering product water pH. Presence of excess hydrogen ion (i.e., low pH) has been linked to increased corrosion potential due to the presence of an electron acceptor in corrosion reactions. Carbonic acid may result from the conversion of bicarbonate when acid is added to desalination facility feed water as a method of controlling calcium carbonate scaling on the RO membrane (i.e., membrane fouling). Decarbonation, or removal of excess carbonic acid, will help increase the finished water pH.

Decarbonation consists of an air transfer process, where carbonic acid (i.e., dissolved carbon dioxide) is in the air phase. Packed tower aeration (PTA), tray aeration, and more recently hollow fibre membrane aeration, can be used for removing carbonic acid from desalination permeate. Decarbonation is typically used in combination with other post-treatment processes, since it may be beneficial to convert some carbonic acid back to bicarbonate alkalinity. Combined use of decarbonation with pH adjustment may be more economical, since this will help control the cost of chemicals used to increase pH while still producing the desired pH, alkalinity, and CCPP.

Addition/Recovery of alkalinity

Carbonic acid is needed to maintain bicarbonate alkalinity, which in turn is critical for permeate stability and corrosion protection. Bicarbonates are buffers against significant pH variations, which is critical to achieve adequate corrosion protection and disinfection. When sufficiently high concentrations of carbonic acid are not available in desalination plant permeate to generate the desired amount of bicarbonate alkalinity with pH adjustment, it may be necessary to supplement alkalinity with chemical treatment. While hydroxide addition will increase the finished water alkalinity and pH, carbonate and bicarbonate alkalinity are required to produce a CCPP within the desired range, and also help provide buffering capacity which in turn will

prevent drinking water pH variation in the distribution system. The following post-treatment methods are widely used to add or recover alkalinity in desalination permeate:

- Addition of caustic soda or lime to permeate containing carbonic acid;
- Addition of carbonic acid followed by the addition of caustic soda or lime;
- Addition of sodium carbonate or sodium bicarbonate.

Caustic soda or lime addition to permeate containing carbonic acid is referred to as alkalinity recovery. As discussed previously, it may be necessary to combine alkalinity recovery with a decarbonation process to control chemical costs when carbonic acid concentrations are high. When desalination plant permeate water has a relatively low concentration of carbonic acid, carbonic acid can be added using a carbon dioxide gas feed system, and then converting the carbonic acid to bicarbonate alkalinity. This can be done with CO₂ that has been recovered during the desalination process. Caution should be exercised to prevent introduction of VOCs that may be present in the vent. An alternative method of increasing carbonate-based alkalinity is the addition of sodium carbonate or sodium bicarbonate. In practice, it may be necessary to monitor dose rates to make certain that finished water sodium concentrations are kept less than the 200 mg/litre limit that is suggested by the World Health Organization to avoid unacceptable taste or the 20 mg/litre drinking water concentration recommended by others for sodium-restricted diets.

Addition of hardness

As discussed previously, a calcium carbonate film deposited on pipe walls can be used as a physical barrier to prevent corrosion. There are a variety of post-treatment methods used to add hardness back to desalination plant permeate. These may include addition of lime or contact filtration through limestone (calcite or dolomite) filters. Slaked lime (calcium hydroxide) is added to permeate water to provide calcium and alkalinity (i.e., hydroxide alkalinity) as well as to adjust product water pH. When adding lime to desalination plant permeate, it is important to consider that the solubility of calcium carbonate is dependent upon pH and temperature (and also ionic strength). Lime may not dissolve easily and a residual turbidity may result, which is a disadvantage of this approach. Post-treatment may require the addition of acid (e.g., H₂CO₃) to help dissolve the lime and produce the desired hardness concentration and CCPP. If the permeate water is warm, the rate of lime dissolution will also be slowed.

There are a few approaches available to foster the dissolution of slaked lime in water with temperatures higher than 25 degrees Celsius. One approach is to provide multiple points for carbonic acid injection and a separate lime contact chamber that creates highly turbulent conditions and provides contact times of 5 to 10 minutes. Another approach used to enhance the reaction of relatively warm plant permeate with lime is mixing the lime suspension and plant permeate in the product water storage tank using large recirculation pumps. This approach is cost-effective only if the unit power cost is relatively low (i.e., \$0.02 to 0.03/kW-hr).

Limestone filters have been used extensively in Europe and the Middle East, often in conjunction with carbonic acid addition to adjust pH, alkalinity, and CCPP, in order to add hardness and to produce finished water that is stable. Limestone (calcite or dolomite) pebbles, are widely used for this application. While calcite pebbles provide only calcium hardness to the

water, use of dolomite contributes both calcium and magnesium, which could be an advantage if the water is used for irrigation of certain crops, or for nutrient embellishment of drinking water. Limestone filters combine two advantages: enhanced contact time and final filtration of the plant product water allowing the controllable production of low turbidity permeate. Limestone filter cells are usually concrete structures designed at loading rates several times higher than those used in conventional media filters. The limestone bed is typically 2.5 to 3 metres deep. The process can be designed with or without carbon dioxide. The limestone in the bed dissolves as the desalination plant permeate passes through the media. Typically, when the limestone bed loss is between 10 to 15% of the original height, additional limestone is added. Usually, the cost of limestone is higher than that of lime per ton. However, the use of limestone filters requires the construction of concrete filter cells and service facilities, which adds to the overall plant construction. Ultimately, the decision for use of lime feed system or limestone filters has to be based on a combination of life-cycle costs (which greatly depends on the cost of lime, limestone, and facilities construction costs) as well as operator skill level.

Corrosion inhibition

Corrosion inhibitors are widely used to reduce the corrosivity of desalination plant permeate. Phosphate and silicate inhibitors form protective films on pipe walls that limit corrosion or reduce metal solubility. Orthophosphates react with pipe metal ions directly to produce a passivating layer. Silicate inhibitors form a glass-like film on pipe walls. Often, these inhibitors are added after corrosion has already occurred. In such cases, typical practice is to add the inhibitor at approximately three times the normal concentration for several weeks to begin the protective film formation. Initial doses should be continuous, and water circulation is required to completely distribute the inhibitor to all parts of the distribution system. Use of corrosion inhibitors instead of alkalinity addition is often more suitable when the water distribution system is made of non-metallic piping (i.e. PVC, fiberglass or HDPE pipe). In this case the use of corrosion inhibitors avoids the potential problems that stem from the increase in product water turbidity associated with addition of lime or other calcium-based minerals and to reduce the overall chemical conditioning costs. See referenced supporting documents included at the end of this section for additional information on this topic.

Permeate remineralization by blending with source water

Permeate has a very low content of calcium, magnesium and other minerals. Therefore, often a small amount of minerals is added to permeate by blending it with source water. This practice is frequently used for both brackish water plants and thermal desalination plants and is acceptable only when the source water is of high quality or pretreated appropriately for both microbial and chemical concerns and the blend meets all applicable water quality standards. When seawater is the source of the blending water, blending is limited to about 1% due to taste considerations. At a 1/99 blending ratio with seawater, this could add 4 to 5 mg/litre of calcium and 12 to 17 mg/litre of magnesium, plus sodium chloride and other ions.

The source water used for blending must be treated prior to its mixing with the desalination plant permeate. The type and complexity of source water treatment depends on its quality. As a minimum the source water used for permeate re-mineralization has to be filtered through cartridge filters. Enhanced source water treatment such as granular activated carbon filtration is recommended for source water exposed to potential contamination from excessive

algal growth, surface runoff or other man-made sources of elevated organics or turbidity in the water. Pretreatment chemicals (such as acid) may need to be added, depending on where the blending source water is split from the feed water piping. The Larson Ratio should be checked in blending applications, especially if steel pipes are used for permeate conveyance.

2.7.4 Product Water Disinfection

Chlorine in various forms (sodium hypochlorite, chlorine gas) is generally used for disinfection because of its recognized efficiency as a disinfectant and because a reduced level of disinfection by-product precursors is generated in permeate. However, other final disinfectants such as chlorine dioxide or even chloramines as a secondary disinfectant, and ozone or UV could be used in combination with chlorination to control microbial regrowth depending on specific conditions.

Chlorination

Chlorination is the most widely used disinfection method. Chlorine gas and sodium hypochlorite are the two most popular chemicals used for chlorination. The desalination process has likely eliminated pathogens and other undesirable microorganisms. The typical target chlorine dosage that provides adequate disinfection depends on two key factors – permeate temperature and contact time. Usually chlorine dosage used for disinfection is 1.5 to 2.5 mg/litre. Although very popular worldwide, the use of chlorine gas is associated with potential safety considerations associated with accidental gas releases. Therefore, chlorine gas disinfection facilities have to be equipped with gas detection, containment and treatment facilities that provide adequate protection of public health. A 5 to 15% solution of sodium hypochlorite is safer to use, handle and store than chlorine gas. Sodium hypochlorite can be delivered to the desalination plant site as a commercial product or it can be produced on site using low bromide sodium chloride (salt). However, electrolysis of seawater to produce hypochlorite is not appropriate because its high bromide content produces large amounts of bromate and probably brominated DBPs

Chloramination

Chloramination is a widely used disinfection alternative. This disinfection method includes sequential addition of chlorine and ammonia to the product water to form chloramines. Chloramines have a significantly slower rate of decay than free chlorine and therefore are often favoured, especially for product water delivered to large distribution systems with high temperatures and long retention times and high potential for chlorine residual loss. Chloramination typically results in a creation of lower levels and different types of disinfection by-products than free chlorine disinfection. It may contribute to nitrite or NDMA production under some conditions. Since desalinated seawater has a very low content of organics, the use of chloramines for seawater desalination is not as advantageous as it may be for disinfection of drinking water produced from brackish or fresh water sources and therefore, is not widely practiced. However, chloramination of desalinated water may be necessary if this water is planned to be blended with other water sources disinfected with chloramines. If chlorinated desalinated water is blended with chloraminated drinking water produced from fresh surface water source, mixing of the two types of water may result in accelerated decay of chlorine residual of the blend of two waters. To avoid such decay the desalinated water is recommended

to be chloraminated at higher dosages than the fresh-source potable water/s with which is it will be blended.

Chlorine Dioxide

Chlorine dioxide is widely used in pre-oxidation and post-disinfection of drinking water as an alternative to chlorine gas/sodium hypochlorite. Chlorine dioxide does not form significant quantities of TTHM's and AOX (Molly et al, 1988) in comparison to other chlorinated disinfectants and no formation of bromate occurs even if the desalinated water is blended with other sources containing bromide ion. The main chlorine dioxide by-products are inorganic: chlorite and chlorate, plus some organic oxidation products. To minimise chlorate formation it is necessary to improve the on-site generation of ClO_2 by using properly designed generators capable of producing very pure ClO_2 solutions and reaching very high conversion of the reagents (Gordon, 2001). Chlorite is the main ClO_2 residue/by-product. When ClO_2 undergoes chemical reduction in water treatment processes, about 60% is converted to chlorite ion. However, in desalinated water the dosage of chlorine dioxide necessary to maintain a residual in the distribution network is quite low (< 0.4 mg/litre which is about one-fourth of the required chlorine dosage) (Belluati et al, 2006), and therefore the chlorite residue is expected to be much lower than the WHO limit (0.7 mg/litre).

Ozonation

Use of ozone is widely accepted practice for disinfection of product water from fresh water sources. However, ozonation of desalinated water is associated with potential formation of excessive amounts of AOC, and bromate due to the relatively high content of bromide in the permeate as compared to that in drinking water from other surface water sources. Additional information on this topic is provided by Perrins et al. (2006).

Ultraviolet Light Disinfection

Ultraviolet (UV) irradiation of desalination plant permeate is a viable disinfection alternative. The disinfection of desalinated water will typically require lower UV dosages than those used for UV disinfection of other surface-water sources due to the lower turbidity and lower content of pathogens in the desalinated water. Another advantage of UV disinfection is that it does not add any chemicals to the product water and therefore, has low content of disinfection byproducts. However, it also does not leave a disinfectant residual to control regrowth, which can be added later (chlorine or chloramine).

2.7.5 Water quality polishing

Water quality polishing is used for enhanced treatment of specific compounds (i.e. boron, silica, NDMA, etc.) when these compounds have to be removed from the water to meet water quality targets for drinking or industrial use. Depending on the compounds targeted for removal the treatment technologies may include: ion exchange, granular activated carbon filtration, additional multi-stage/multi-pass membrane RO treatment or a combination of treatment processes that could include advanced oxidation (AOP). Parekh (1988) and Wilf et al. (2006) provide additional information of permeate polishing.

2.7.6 Post-treatment issues and considerations

Effect of disinfection on corrosion control

It is important to consider the impact of disinfection processes on finished water pH and the resultant impact to the CCPP. Chlorine gas addition decreases pH and alkalinity due to the formation of hypochlorous acid, while use of sodium hypochlorite and calcium hypochlorite increases pH and alkalinity of the product water.

Use of sodium hypochlorite produced from seawater

As indicated previously, sodium hypochlorite used for disinfection can either be delivered to the desalination plant as a commercial product or alternatively could be generated on site using commercially available sodium chloride. The main advantages of sodium hypochlorite generation at the treatment plant site, especially for large plants, is that it minimizes space requirements for storage of sodium hypochlorite solution, and to prevent hypochlorite solution strength decay on the effectiveness of disinfection. Usually, sodium hypochlorite solutions decay rapidly over time and lose 10 to 20 % of their strength over a period of 10 to 15 days, while chlorate concentrations are increasing, especially in warm climates. The rate of solution strength decay mainly depends on the initial concentration of the sodium hypochlorite, the ambient temperature, and the exposure to sunlight.

On-site sodium hypochlorite generation using commercially available high-grade low bromide sodium chloride instead of seawater is recommended. Although the use of seawater as a source of chloride for the sodium hypochlorite generation process is less costly and simpler it results in generation of higher concentrations of disinfection by-products and bromate because of the naturally high level of bromide in the seawater. When blended with desalination plant permeate, the sodium hypochlorite generated from seawater increases the concentration of disinfection by-products and bromate in the drinking water.

Chloramination and total chlorine residual stability

Disinfection of seawater with chlorine results in a stable and long-lasting chlorine residual which provides adequate residual disinfection in the distribution system in many conditions. However, ammonia addition to permeate to form chloramines may result in an accelerated decay of the total chlorine residual if the bromide concentration of permeate is above 0.4 mg/litre (McGuire Environmental & Poseidon Resources (2004)). Applying a combination of chlorine and ammonia to desalinated water with bromide levels above 0.4 mg/litre may yield an unstable total chlorine residual that decays at an accelerated rate (within several hours). The destabilizing effect of bromide on the chloramination process can be mitigated by super-chlorination (i.e., applying initial chlorine to the permeate at dosages of 3.0 to 4.0 mg/litre) or by producing permeate with a bromide level below 0.4 mg/litre.

Ozonation and DBP and Bromate Formation

Ozonated permeate may contain high concentrations of bromate. This can be addressed by reducing the bromide level below the threshold at which excessive amounts of bromate and

brominated disinfection by-products are formed. As indicated previously, ozonation does not leave a disinfectant residual to suppress regrowth of microorganisms.

Blending and Compatibility of Desalinated Water with Other Water Sources

Usually, blending of desalinated water with surface water or groundwater of elevated salinity has a very positive effect on the quality of the water blend and is therefore highly desirable. Blending of low DBP desalinated seawater with surface water with high disinfection by-product content can effectively be used to reduce the overall disinfection by-product levels of the drinking water. However, when desalinated water has high content of some minerals such as bromides, boron, sodium, chlorides, calcium and magnesium, the blending of this desalinated water with drinking water produced from other sources (river, lake or groundwater) may have a negative effect on the blended water quality. Therefore, the compatibility of the various water sources has to be taken into consideration prior to their blending. Specific issues that must be investigated before blending drinking waters of various origins include:

- Bromide and total organic carbon concentrations in the various waters and their effect on the disinfection by-product formation and concentration in the blend;
- Type of disinfection used for the various water sources and their effect on disinfection by-product formation and chlorine residual stability;
- Sodium and chloride levels in various sources – desalination plant permeate may have higher sodium levels than other fresh-water sources;
- Temperature of various water sources – the higher temperature may result in accelerated nitrification and corrosion in the distribution system. On the other hand the desalinated water is void of organics and the overall blending effect may be positive and may negate the temperature effect on the growth rate of the nitrifying organisms.
- Calcium and magnesium in the various sources – before blending desalinated water usually has significantly lower levels of calcium and magnesium than other water sources. Blending of desalinated water with water of high hardness may be sufficient to provide the needed water stability without additional chemical addition, except for corrosion inhibition, if needed.
- Conveyance of desalinated water in long pipelines may pose chlorination and corrosion problems, especially in warm climates. Loss of disinfectant residual is one of the main challenges in such systems, mainly because of residual disinfectant decay caused by high-temperature water. This may be addressed by either superchlorination (i.e., feeding chlorine at dosages resulting in break-point chlorination (3.5 to 4 mg/litre); reinjection of chlorine along the length of the pipeline, which could be activated when the chlorine residual drops below 0.5 mg/litre; or by use of chloramine instead of chlorine for disinfection because of its lower chemical reactivity. Chloramines have slower decay rates than free chlorine and may provide a more reliable residual in long pipelines.
- Loss of calcium alkalinity may also occur over the length of the pipeline, and thereby may result in corrosion problems. There are several alternatives to address this challenge: (1) to re-inject calcium conditioning chemicals or corrosion inhibitors along the pipeline route at locations where the water LSI is reduced to a negative level; (2) to use non-metal pipeline materials such as HDPE, which are not sensitive to low levels of calcium alkalinity in the water.

- The condition of the existing water distribution system. In an existing system, the piping has probably reached a steady-state condition with the water being delivered. This steady-state can be disturbed by introducing desalted water of a notably different character.

2.8 Concentrates management

One of the key limiting factors for the construction of new desalination plants is the availability of suitable conditions and location for disposal of the high-salinity side-stream commonly referred to as concentrate or brine.

2.8.1 Concentrate characterization and quality

Concentrate is generated as a side product of the separation of the minerals from the source water used for desalination. Therefore, this liquid stream contains most of the minerals and contaminants of the source water and pretreatment additives in concentrated form. The concentration of minerals and contaminants in the concentrate is usually 2 to 10 times higher than that in the source water depending upon the recovery of the desalination plant. If chemical pretreatment is used, such as coagulants, anti-scalants, polymers or disinfectants, some or all of these chemicals may reach or may be disposed along with the plant concentrate and ultimately may increase the ion content and residual organics in the plant discharge.

The quantity of the concentrate is largely a function of the plant recovery, which in turn is highly dependent on the total dissolved solids concentration of the source water. Usually, brackish water desalination plants operate in recovery ranges of 80 to 90 % and 65 to 85 %, respectively, depending upon the influent TDS. Seawater desalination plant recovery is typically limited to 40 to 65 %. Nanofiltration plants primarily reject divalent ions (e.g., calcium, magnesium and sulfate) and therefore, the concentrate from these plants is of somewhat lower salinity and sodium and chloride content than that of brackish and seawater RO plants. The TDS level of concentrate from seawater desalination plants usually is in a range of 65,000 to 85,000 mg/litre, while that from brackish plants may vary between 1,500 mg/litre and 25,000 mg/litre. The amount of particles, total suspended solids (TSS) and biological oxidation demand (BOD) in the concentrate is usually below 5 mg/litre because these constituents are removed by the plant's pretreatment system. However, if plant pretreatment waste streams are discharged along with the concentrate, the blend may contain elevated turbidity, TSS and occasionally BOD. If acids and scale inhibitors are added to the desalination plant source water, they will be rejected in the concentrate and will impact its overall mineral content and quality. Often scale inhibitors contain phosphates or organic polymers. The concentration of scale inhibitors in the concentrate may reach 20 to 30 mg/litre.

An important unique aspect of the thermal desalination plant discharge is that this discharge has an elevated temperature and therefore is a source of thermal pollution. For comparison, the temperature of the discharge of a typical membrane seawater desalination plant is similar to that of the ambient ocean water. This is quite important as the energy dissipated in the environment (i.e., the thermal pollution load) of a thermal desalination plant is very high and, as it can be seen from Table 2-5, it is substantially higher than the thermal discharge associated to a similar size power plant.

Table 2-5 Environmental impacts of power generation and desalination processes			
Reference process	Type of process	Energy dissipated in the environment MW	TDS increase with respect to the uptake
Power generation 150 MW	Conventional cycle	50	0
	Combined cycle	10	0
Desalination plant 7.2 MIGD	MSF (performance ratio 9)	120	15-20 %
	MED (performance ratio 9)	100	15-20 %
	SWRO	0	50-80 %

The thermal discharge load of a thermal desalination plant could be reduced by increasing the MSF and MED plant performance ratio.

Figure 2-7 shows the amount of thermal energy dissipated to the sea through the heat reject section of a MSF plant against the plant performance ratio (PR) at various distiller capacities. The figure clearly indicates that the thermal discharge from a MSF plant can be decreased significantly if the plant PR ratio is increased.

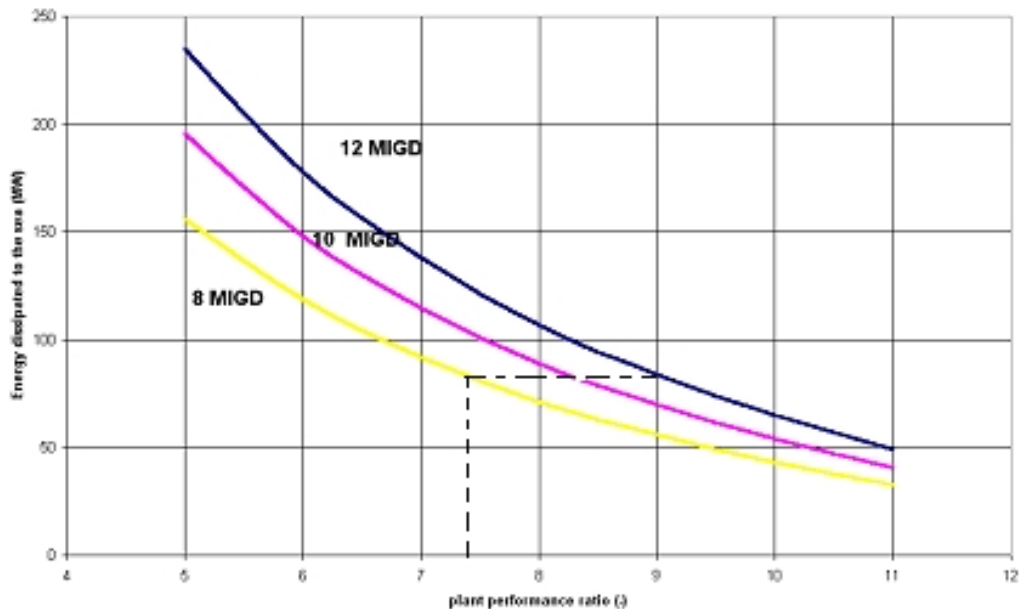


Figure 2-7 Thermal energy discharge load of MSF plants

As seen on Figure 2-7, an MSF plant of 12 MGD (~45420 m³) with performance ratio (PR) of 9 dissipates the same energy in the sea as an MSF plant of 8 MGD (~30280 m³) with a

performance ratio of 7. New thermal desalination plants are generally specified with high performance ratios because this also decreases CO₂ and NO_X emissions. However there are a number of old installations operating with PR 5. It is important that this thermal load discharge issue is given proper consideration, especially for large thermal plants.

2.8.2 Overview of concentrate management alternatives

Chapter 6 of this document provides guidance for preparation of environmental impact assessments of desalination plants, part of which deals with concentrates management. The following sections of this chapter discuss the most widely used concentrate disposal alternatives. These include:

- Discharge to Surface Waters;
- Discharge to Sanitary Sewer;
- Deep Well Injection;
- Evaporation Ponds;
- Spray Irrigation;
- Zero Liquid Discharge.

According to a study by the Bureau of Reclamation (Mickley (2001)) the concentrate disposal methods most widely used in the USA are those shown in Table 2.6. These results are based on a survey completed in year 2000 of 203 desalination plants. The survey included only plants with capacity larger than 200 m³/day. Approximately 85 % of the surveyed plants were nanofiltration, brackish water, or seawater reverse osmosis (SWRO) facilities. Although based on information from desalination plants in the US, Table 2.5 reflects typical concentrate management practices worldwide.

Table 2.6 Concentrate disposal methods and their frequency of use

Concentrate Disposal Method	Frequency of Use (% of Surveyed Plants)
Surface Water Discharge	45 %
Sanitary Sewer Discharge	42 %
Deep Well Injection	9 %
Evaporation Ponds	2 %
Spray Irrigation	2 %
Zero Liquid Discharge	0 %

In addition to the listed methods, two additional trends in concentrate management are gaining acceptance worldwide:

- Regional Concentrate Management;

- Beneficial Concentrate Use.

A brief description of each of the concentrate disposal methods and associated key issues, considerations and mitigation measures associated with their implementation are summarized below.

2.8.3 Concentrate discharge

Discharge of concentrate to surface waters

This disposal method involves the discharge of the desalination concentrate to a surface water body i.e. the nearby ocean or sea, river, estuary, bay or lake. Discharge of desalination plant concentrate through a new ocean outfall is widely practiced worldwide and is very popular for projects of all sizes. Over 90 % of the large desalination plants in operation dispose of their concentrates through a new ocean outfall specifically designed and built for that purpose. Ocean discharge is typically completed using one of the following three methods:

- Direct Discharge Through New Ocean Outfall
- Discharge Through Existing Wastewater Treatment Plant Outfall
- Discharge Through Existing Power Plant Outfall

Discharge through a new ocean outfall

The purpose of an ocean outfall is to dispose of the plant concentrate in environmentally safe manner, which mainly means to minimize the size of the zone of discharge in which the salinity is elevated outside of the typical range of tolerance of the aquatic organisms inhabiting the discharge area. The two key options available to accelerate concentrate mixing from an ocean outfall discharge are to either rely on the naturally occurring mixing capacity of the tidal (surf) zone, or to discharge the concentrate beyond the tidal zone and to install diffusers at the end of the discharge outfall in order to improve mixing.

Although the tidal zone carries a significant amount of turbulent energy and usually provides much better mixing than the end-of-pipe type of diffuser outfall system, this zone has a limited capacity to transport the saline discharge load to the open ocean. If the mass of the saline discharge exceeds the threshold of the tidal zone's salinity load transport capacity, the excess salinity would begin to accumulate in the tidal zone and could ultimately result in a long-term salinity increment in this zone beyond the level of tolerance of the aquatic life. Therefore, the tidal zone is usually a suitable location for discharge only when it has adequate capacity to receive, mix and transport the salinity discharge from a desalination plant to the open ocean. This salinity threshold mixing/transport capacity of the tidal zone can be determined using hydrodynamic modelling. If the desalination plant total dissolved solids discharge load is lower than the tidal zone threshold mixing/transport capacity, then concentrate disposal to this zone is preferable and much more cost effective than the use of a long open outfall equipped with a diffuser system.

For very small plants (i.e., plants with production capacity of 400 m³/day or less), the ocean outfall is usually constructed as an open-ended pipe that extends up to 100 meters into the tidal (surf) zone of the ocean. These discharges usually rely on the mixing turbulence of the tidal

zone to dissipate the concentrate and to quickly bring the discharge salinity of the small volume to ambient conditions. Ocean outfalls for large seawater desalination plants typically extend beyond the tidal zone. Large ocean outfalls are equipped with diffusers in order to provide the mixing necessary to prevent the heavy saline discharge plume to accumulate at the ocean bottom in the immediate vicinity of the discharge. The length, size and configuration of the outfall and diffuser structure for a large desalination plant are typically determined based on hydrodynamic modelling for the site specific conditions of the discharge location.

Discharge through an existing wastewater treatment plant outfall

The key feature of this combined discharge method is the benefit of accelerated mixing that stems from blending the heavier high-salinity concentrate with the lighter low-salinity wastewater discharge. Depending on the volume of the concentrate and on how well the two waste streams are mixed prior to the point of discharge, the blending may allow reducing the size of the wastewater discharge plume and dilute some of its constituents. Co-discharge with the lighter-than-seawater wastewater effluent would also accelerate the dissipation of the saline plume by floating this plume upwards and expanding the volume of the ocean water with which it mixes.

Direct discharge through an existing wastewater treatment plant outfall has found a limited application to date, especially for medium and large seawater desalination plants. Key considerations are: the availability and cost of wastewater outfall capacity and the potential for whole effluent toxicity (WET) of the blended discharge that may result from ion imbalance of the blend of the two waste streams (Mickley, 2001)). For this concentrate disposal option to be feasible there must be an existing wastewater treatment plant in the vicinity of the desalination plant, and this wastewater plant has to have available extra outfall discharge capacity. The fees associated with the use of the wastewater treatment plant outfall have to be reasonable, and the wastewater treatment plant utility that would allow the use of their outfall for concentrate discharge must be comfortable with the arrangement of handling and separation of liability for environmental impacts of the blended discharge between the owner of the desalination plant and the owner of the wastewater treatment plant. Usually, this beneficial combination of conditions is not easy to find, especially for discharging large concentrate volumes.

Bioassay tests completed on blends of desalination plant concentrate and wastewater effluent from the El Estero wastewater treatment in Santa Barbara, California (Bay & Greenstein, 1992/93) indicate that this blend can exhibit toxicity on fertilized sea urchin (*Strongylocentrotus purpuratus*) eggs. Parallel tests on desalination plant concentrate diluted to similar TDS concentration with seawater rather than wastewater effluent did not show such toxicity effects on sea urchins. Long-term exposure of red sea urchins on the blend of concentrate and ambient seawater confirm the fact that sea urchins can survive elevated salinity conditions when the discharge is not mixed with wastewater. Thus, the wastewater component is the critical issue.

These findings clearly indicate that blending of wastewater effluent and desalination plant concentrate may have negative effects on some aquatic species and needs careful consideration when analyzing the advantages and disadvantages of using existing wastewater treatment plant outfalls for concentrate discharge. The aquatic organisms that are recommended

to be tested for toxicity effects of the blend of wastewater effluent and desalination plant concentrate are the echinoderms (*Phylum Echinodermata*), which include species such as the urchins, starfish, sand dollars, and serpent stars. The echinoderms are the aquatic organisms most sensitive to the exposure of a blend of wastewater and concentrate because they are the only major marine taxa that do not extend into fresh water.

The most likely factor causing the toxicity effect on the sensitive marine species is the difference in ratios between the major ions (calcium, magnesium, sodium, chloride and sulfate) and TDS that occurs in the wastewater effluent-concentrate blend as compared to the concentrate-seawater blend and the ambient ocean water. Since the RO membranes reject key seawater ions except some complex ions like borate at approximately the same level, the ratios between the concentrations of those ions and the TDS in the concentrate are approximately the same as these ratios in the ambient seawater. Therefore, marine organisms are not exposed to conditions of ion ratio imbalance, if this concentrate is directly disposed to the ocean. Since wastewater effluent has a fresh water origin, and fresh water often has very different ratios of key ions to TDS, blending this effluent with seawater concentrate may yield a discharge which has ratios of the key ions to TDS significantly different from these of the ambient seawater. This significant ion make-up shift (ion ratio imbalance) caused by blending of the two waste streams is considered to be the most likely cause for the toxic effect of the concentrate-wastewater blend on sensitive marine species.

Discharge through an existing power plant outfall (co-location)

The key feature of the co-location concept is the direct connection of the desalination plant intake and discharge facilities to the discharge outfall of an adjacently located coastal power generation plant (Voutchkov, 2004). This approach allows using the power plant cooling water both as source water for the desalination plant and as a blending water to reduce the salinity of the desalination plant concentrate prior to the discharge to the ocean.

For co-location to be cost-effective and possible to implement, the power plant cooling water discharge flow must be larger than the desalination plant capacity and the power plant outfall configuration must be adequate to avoid entrainment and recirculation of concentrate into the desalination plant intake. It is preferable that the length of the power plant outfall downstream of the point of connection of the desalination plant discharge is adequate to achieve complete mixing prior to the point of entrance into the sea. Special consideration must be given to the effect of the power plant operations on the cooling water quality, since this discharge is used as source water for the desalination plant. For example, if the power plant discharge contains levels of copper, nickel or iron significantly higher than these of the ambient seawater, this power plant discharge may not be suitable for co-location of a membrane plant because these metals may cause irreversible fouling of the membrane elements.

Under the co-location configuration, the power plant discharge serves both as an intake and discharge for the desalination plant. This arrangement yields four key benefits: (1) the construction of separate desalination plant intake and outfall structures is avoided thereby reducing the overall cost of desalinated water; (2) the salinity of the desalination plant discharge is reduced as a result of the mixing and dilution of the membrane concentrate with the power plant discharge, which has ambient seawater salinity; (3) because a portion of the discharge

water is converted into drinking water, the power plant thermal discharge load is decreased, which in turn lessens the negative effect of the power plant thermal plume on the aquatic environment; (4) the blending of the desalination plant and the power plant discharges results in accelerated dissipation of both the salinity and the thermal discharges.

Avoiding the cost of construction of a separate ocean outfall would result in a measurable reduction of plant construction expenditures. In addition, the length and configuration of the desalination plant concentrate discharge outfall are closely related to the discharge salinity. Usually, the lower the discharge salinity, the shorter the outfall and the less sophisticated the discharge diffuser configuration needed to achieve environmentally safe concentrate discharge. Blending the desalination plant concentrate with the lower salinity power plant cooling water often allows reducing the overall salinity of the ocean discharge within the range of natural variability of the seawater at the end of the discharge pipe, thereby completely alleviating the need for complex and costly discharge diffuser structures. In addition, the power plant thermal discharge is lighter than the ambient ocean water because of its elevated temperature and therefore, it tends to float on the ocean surface. The heavier saline discharge from the desalination plant draws the lighter cooling water downwards and thereby engages the entire depth of the ocean water column into the heat and salinity dissipation process. As a result the time for dissipation of both discharges shortens significantly and the area of their impact is reduced.

Concentrate surface water discharge - issues and considerations

The key challenges associated with selecting the most appropriate location for the desalination plant's ocean outfall discharge are: finding an area devoid of endangered species and stressed marine habitats; identifying a location with strong ocean currents that allows quick and effective dissipation of the concentrate discharge; avoiding areas with busy naval vessel traffic, which could damage the outfall facility and change mixing patterns, and finding a discharge location in relatively shallow waters that at the same time is close to the shoreline in order to minimize outfall construction expenditures. Key environmental issues and considerations associated with concentrate disposal to surface waters include:

- Salinity increase beyond the tolerance thresholds of the species in the area of the discharge;
- Concentration of metals and radioactive ions to harmful levels;
- Concentration and discharge of nutrients that trigger change in marine flora and fauna in the area of the discharge;
- Compatibility between the composition of the desalination plant concentrate and receiving waters (ion-imbalance driven toxicity);
- Elevated temperature from thermal desalination processes;
- Disturbance of bottom marine flora and fauna during outfall installation.

Key issues associated with the feasibility of disposal of seawater desalination plant concentrate to the ocean under any of the discharge methods described above include: (1) evaluation of discharge dispersion and recirculation of the discharge plume to the plant intake; (2) establishment of the marine organism salinity tolerance threshold for the site-specific conditions of the discharge location and outfall configuration; (3) evaluation of the potential for whole

effluent toxicity of the discharge; and (4) assessment whether the discharge water quality meets the numeric and qualitative effluent water quality standards applicable to the point of concentrate discharge.

Evaluation of concentrate dispersion

The main purpose of the evaluation of the concentrate dispersion from the point of discharge is to establish the size of the zone of initial dilution (ZID) required to dissipate the discharge salinity plume to ambient seawater TDS levels and to determine the TDS concentrations at the surface, mid level of the water column, and at the ocean bottom in the ZID. The TDS concentration fields at these three levels are then compared to the salinity tolerance of the marine organisms inhabiting the surface (mostly plankton), the water column (predominantly invertebrate) and the bottom dwellers in order to determine the impact of the concentrate salinity discharge on these organisms.

The discharge salinity field in the ZID and the ZID boundaries is established using hydrodynamic modelling. This modelling allows determining the most suitable location, design configuration and size of the ocean outfall and diffusers if a new outfall is needed, or to assess the feasibility of using existing wastewater or power plant outfall facilities. The model selected for determining the boundaries of the desalination plant discharge should be used to depict the concentrate plume dissipation under a variety of outfall and diffuser configurations and operational conditions. The evaluation of concentrate dispersion and recirculation for very large seawater desalination plants usually requires sophisticated plume analysis and is completed using various computational fluid dynamics (CDF) software packages which are tailor made for a given application.

Aquatic life salinity tolerance threshold

Many marine organisms are naturally adapted to changes in seawater salinity. These changes occur seasonally and are mostly driven by the evaporation rate from the ocean surface, by rain/snow deposition and runoff events and by surface water discharges. The natural range of seawater salinity fluctuations could be determined based on information from sampling stations located in the vicinity of the discharge and operated by national, state or local agencies and research centers responsible for ocean water quality monitoring. Typically, the range of natural salinity fluctuation is at least $\pm 10\%$ of the average annual ambient seawater salinity concentration. The “10 % increment above ambient ocean salinity” threshold is a conservative measure of aquatic life tolerance to elevated salinity. The actual salinity tolerance of most marine organisms is usually significantly higher than this level.

Whole effluent toxicity evaluation

Whole effluent toxicity testing is an important element of the comprehensive evaluation of the effect of the concentrate discharge on the aquatic life. Completion of both acute and chronic toxicity testing is recommended for the salinity levels that may occur under worst-case combination of conditions in the discharge (Voutchkov 2006). Use of at least one species endogenous to the targeted discharge is desirable. In the case of concentrate discharge through an existing wastewater treatment plant outfall, at least one species of the echinoderms taxa (i.e. urchins, starfish, sand dollars, or serpent stars) is recommended to be tested for a worst-case

scenario blend of concentrate and wastewater effluent (typically, maximum wastewater effluent flow discharge combined with average concentrate flow).

Compliance with numeric effluent discharge water quality standards

The key parameters which should be given attention regarding concentrate compliance with the numeric effluent discharge water quality standards are: total dissolved solids, metals, turbidity and radionuclides. At present, most countries do not have numeric standards for total TDS discharges.

Because metal content in ocean water is naturally low, compliance with the numeric standards for toxic metals usually does not present a challenge. However, concentrate co-discharge with wastewater treatment plant effluent may occasionally present a concern, because wastewater plant effluent contains metal concentrations which sometimes may be higher than these in the ambient ocean water. Similar attention to the metal levels in the combined discharge should be given to co-disposal of power plant cooling water and concentrate, especially if the power plant equipment leaches metals such as copper and nickel, which may then be concentrated in the desalination plant discharge. If the desalination plant has a pretreatment system that uses a coagulant (such as ferric sulfate or chloride), the waste discharges from the source water pretreatment may contain elevated concentrations of iron and turbidity which must be accounted for when assessing the total discharge concentration for these compounds.

Radionuclide levels in the ocean water often exceed the effluent water quality standards and the RO system concentrate is likely to contain elevated gross Alpha radioactivity. This condition is not unusual for both Pacific and Atlantic Ocean water and has to be well documented with adequate water quality sampling in order to avoid potential permitting challenges.

One important challenge with all concentrate water quality analyses is that most of the laboratory analysis guidelines worldwide are developed for testing fresh water rather than for seawater or high-salinity concentrate. The elevated salt content of the concentrate samples could interfere with the standard analytical procedures and could often produce erroneous results. Therefore, concentrate analysis has to be completed by an analytical laboratory experienced with and properly equipped for seawater analysis. The same recommendation applies for the laboratory retained to complete the whole effluent toxicity testing and source water quality characterization using techniques designed for saline water. This topic is addressed in Chapter 6 of this Guidance.

2.8.4 Concentrate discharge to sanitary sewer

Discharge to the nearby wastewater collection system is one of the most widely used methods for disposal of concentrate from brackish water desalination plants (Table 2.5). This concentrate discharge method however, is only suitable for disposal of concentrate from very small brackish water and seawater desalination plants into large-capacity wastewater treatment facilities mainly because of the potential negative effects of the concentrate's high TDS content on the wastewater treatment plant operations. Discharging concentrate to the sanitary sewer is regulated by the requirements applicable to industrial discharges and the applicable discharge regulations of the utility/municipality which is responsible for wastewater collection system management.

The feasibility of this disposal method is limited by the hydraulic capacity of the wastewater collection system and by the treatment capacity of the wastewater treatment plant receiving the discharge. Typically, wastewater treatment plant's biological treatment process is inhibited by high salinity when the plant influent TDS concentration exceeds 3000 mg/litre. Therefore, before directing desalination plant concentrate to the sanitary sewer the increase in the wastewater treatment plant influent salinity must be assessed and its effect on the plant's biological treatment system has to be investigated. Taking under consideration that wastewater treatment plant influent TDS may be up to 1000 mg/litre in many facilities located along the ocean coast, and that the seawater desalination plant concentrate TDS is likely to be 65000 mg/litre or higher, the capacity of the wastewater treatment plant must be at least 30 to 35 times higher than the daily volume of concentrate discharge in order to maintain the wastewater plant influent TDS concentration below 3000 mg/litre. For example, a 38000 m³/day wastewater treatment plant would likely not be able to accept more than 1000 m³/day of concentrate (i.e. serve a seawater desalination plant of capacity higher than 1000 m³/day).

If the effluent from the wastewater treatment plant is designated for water reuse, the amount of concentrate that can be accepted by the wastewater treatment plant is limited not only by the concentrate salinity, but by the content of sodium, chlorides, boron and bromides in the blend as well. All of these compounds could have a profound adverse effect on the reclaimed water quality, especially if the effluent is used for irrigation. Treatment processes in a typical municipal wastewater treatment plant, such as sedimentation, activated sludge treatment, and sand filtration, do not remove a measurable amount of these concentrate constituents.

Many crops and plants cannot tolerate irrigation water that contains over 1000 mg/litre of TDS. However, TDS is not the only parameter of concern in terms of irrigation water quality. Boron/borate levels in the effluent could also limit agricultural reuse because borates are herbicides. Chlorides and sodium may also have measurable effects on the irrigated plants. Most plants cannot tolerate chloride levels above 250 mg/litre. The typical wastewater plant effluent has chloride levels of less than 150 mg/litre, while the seawater treatment plant concentrate would have chloride concentration of 50000 mg/litre or more. Using the chloride levels indicated above, a 38000 m³/day wastewater treatment plant could not accept more than 75 m³/day of concentrate, if the plant's effluent would be used for irrigation. This limitation could be even more stringent if the wastewater effluent is used for irrigation of salinity-sensitive ornamental plants. For concentrate discharge from brackish plants, the issues discussed above are usually of lesser significance because the salinity of the concentrate in most cases is not higher than the wastewater influent TDS threshold of 3,000 mg/litre. Therefore, direct concentrate discharge to a sanitary sewer is most widely used for brackish water desalination plants and rarely practiced for seawater desalination applications.

2.8.5 Concentrate deep well injection

This disposal method involves the injection of desalination plant concentrate into an acceptable confined deep underground aquifer below a freshwater aquifer using a system of disposal wells. The deep well injection concentrate disposal system also includes a set of monitoring wells to confirm that the concentrate is not propagating to the adjacent aquifers. A variation of this

disposal alternative is the injection of concentrate into existing oil and gas fields to aid field recovery. Deep well injection is usually used for concentrate disposal from all sizes of brackish water desalination plants while beach well disposal is practiced for small and medium-size seawater desalination plants.

Key issues and considerations associated with deep well injection include:

- Limited to site specific conditions of confined aquifers of large storage capacity which have good soil transmissivity (Swartz, 2000).
- Not feasible for areas of elevated seismic activity or near geologic faults that can provide a direct hydraulic connection between the discharge aquifer and a water supply aquifer.
- Potential for contamination of groundwater with concentrated pollutants, if the discharge aquifer is not adequately separated from the water supply aquifer in the area of discharge.
- Potential for leakage from the wells.
- Potential scaling and decrease of well discharge capacity over time.
- A back up concentrate disposal method is required for periods of time when the injection wells are tested and maintained.
- High well construction and monitoring costs.

2.8.6 Evaporation ponds

This method is based on natural solar evaporation of the concentrate in man-made lined earthen ponds or other basins. Evaporation ponds are zero-discharge technology. Holding ponds are needed for concentrate storage while the evaporation pond reaches high salinity needed for normal pond operations. Use of evaporation ponds is limited by the following issues and considerations:

- Solar evaporation is suitable only for disposal of concentrate from small plants in arid areas with low land costs.
- Land requirements are significant.
- Require leveled land area;
- Climate dependence;
- Evaporation rate decreases as solids and salinity levels in the ponds increase;
- If the evaporation ponds are not lined a portion of the concentrate may percolate to the fresh water aquifer beneath the pond
- Leakage risk.
- The salts accumulated at the bottom of the ponds have to ultimately be disposed to a suitable landfill.

2.8.7 Spray irrigation

This disposal technology uses concentrates for irrigation of salinity-tolerant crops or ornamental plants (lawns, parks, golf fields, etc.). The key issues and constraints associated with spray irrigation are:

- Seasonal nature.
- Restricted to small-size desalination plants.
- A back up disposal alternative is required during times when crop irrigation is not needed.
- Feasibility determined by climate, land availability, irrigation demand and salinity tolerance of the irrigated plants.
- The type of crops and ornamental plants that can be grown on high-salinity water is very limited.
- May have a negative impact on groundwater aquifer beneath the irrigated area. Use of this method may cause significant concerns if the concentrate contains arsenic, nitrates, metals or other regulated contaminants.

2.8.8 Zero liquid discharge

Zero-liquid discharge technologies, such as brine concentrators, crystallizers and dryers convert concentrate to highly purified water and solid dry product suitable for landfill disposal or perhaps recovery of useful salts.

Concentrators (Thermal Evaporators). Concentrators are single-effect thermal evaporator systems in which the vapour produced from boiling concentrate is pressurized by a vapour compressor. The compressed vapour is then re-circulated for more vapour production from the concentrate. The concentrators are typically used for water reuse applications. Usually the concentrator technology allows evaporation of 90 to 98 % of the concentrate and produces low-salinity fresh water. The concentrated stream can be further dewatered and disposed to a landfill as a solid waste. Ultimately, the concentrated salt product could be designated for commercial applications. Vapour compression driven concentrators are very energy efficient – they use approximately 10 times less energy than single-effect steam-driven evaporators. Typically energy for the concentrators is supplied by mechanical vacuum compression system.

Crystallizers. Crystallizers are used to extract highly soluble salts from concentrate. The crystallization vessels are vertical units operated using steam supplied by a package boiler or heat provided by vacuum compressors for evaporation. Concentrate is fed to the crystallizer vessel and passed through shell-and-tube heat exchanger and heated by vapour introduced by the vacuum compressor. The low-salinity water separated from the concentrate is collected as distillate at the end of the condenser. The heated concentrate then enters the crystallizer where it is rotated in a vortex. Concentrate crystals are formed in the vessel and the crystalline mineral mass is fed to a centrifuge or a filter press to be dewatered to a solid state. The mineral cake removed from the concentrate contains 85 % solids and is the only waste stream produced by the crystallizer.

The cost of energy for concentrate evaporation and crystallization is high (100 to 250 kWh/1,000 gallons, 3.78 m³), and the equipment costs are usually several times larger than the capital investment needed for the other concentrate disposal alternatives. Because of the high capital and operation and maintenance costs, the zero-discharge technologies are not practical unless no other concentrate management alternatives are available. Usually, the zero-discharge concentrate management systems are justifiable for in-land brackish water desalination plants where the site-specific constraints limit the use of natural evaporation or wastewater treatment

plant disposal. Use of high-recovery desalination systems in front of the evaporators can reduce energy and capital costs.

2.8.9 Regional concentrate management

Regional concentrate management includes two alternative approaches which can be used separately or co-implemented at the same facility:

- Regional collection and centralized disposal of seawater concentrate through one location applying one or more of the methods described in the previous sections;
- Use of concentrate from brackish water desalination plants as source water to seawater desalination plant.

The first approach takes advantage of site-specific beneficial conditions for disposal which may not be available at other locations and of the economies of scale of constructing larger concentrate disposal facilities. The second approach takes advantage of the fact that concentrate from brackish water plants is of significantly lower salinity than seawater, and when blended with the ocean water fed to a seawater desalination plant will reduce the overall plant salinity. The use of concentrate from brackish water desalination plant as feed water to a seawater desalination plant is mutually beneficial for both the brackish water desalination plant and the seawater plant. Usually, in-land brackish water desalination plant capacity is limited by lack of suitable discharge location of the plant concentrate. If the seawater desalination plant can accept the brackish water desalination plant concentrate and process it, the brackish water desalination plant capacity could be increased beyond the threshold driven by brine discharge limitations, and the desalination plant source salinity could be reduced at the same time. While the seawater TDS concentration is usually in a range of 3000 to 4000 mg/litre, the TDS of the concentrate from brackish water desalination plants is typically several times lower (i.e. typically 2000 to 15000 mg/litre). Therefore, when blended with the source seawater it would reduce the overall desalination plant feed water salinity, which in turn would have a positive effect on the overall desalination plant power use, recovery factor and cost of water. The key issues and considerations associated with regional concentrate disposal stem from the location of a large volume of discharge in a single point. This may amplify the negative effect of disposal on the marine organisms in the area of discharge.

2.8.10 Technologies for beneficial use of concentrate

Concentrate from seawater desalination plants contains large quantities of minerals that may have commercial value when extracted. The most valuable minerals are: magnesium, calcium and sodium chlorides, and bromine. Magnesium compounds in seawater have agricultural, nutritional, chemical, construction and industrial applications. Calcium sulfate (gypsum) is used as construction material for wallboard, plaster, building cement, and road building and repair. Sodium chloride can be used for production of chlorine and caustic soda, highway de-icing, and food products. Technologies for beneficial recovery of minerals from concentrate can be used for management of concentrate from both inland brackish water desalination plants and coastal seawater desalination plants. These technologies have the potential to decrease the volume and cost of transporting concentrate as well. Specific emerging technologies for beneficial reuse of desalination plant concentrate are discussed below.

Salt solidification and recovery

The existing salt recovery technologies extract salts by fractional crystallization or precipitation. Crystallization of a given salt can be achieved by concentrate evaporation or temperature control. Fractional precipitation is attained by adding a precipitating chemical agent to selectively remove a target mineral from the concentrate solution. For example, an Australian company has developed a commercially available technology for extraction of magnesium and calcium salts from concentrate and for production of structural materials from these salts.

Disposal to brackish or saltwater wetlands

This method is site-specific and suitable for conditions where the concentrate quality is compatible with the native flora and fauna of the saltwater march or wetland. Usually, the type of wetlands or marches that would be used for concentrate discharge are hydraulically interconnected with the ocean or a brackish water body and therefore, this essentially is an indirect method for concentrate disposal to surface waters. Wetland vegetation may assimilate some of the nitrate and selenium in the concentrate thereby providing effective reduction of these contaminants.

Concentrate use as cooling water

Use of concentrate for power plant cooling and is typically practiced for small power plants with limited cooling needs and cooling towers that are made of materials suitable to withstand the highly-corrosive concentrate. A key concern regarding this concentrate use is its high scaling potential.

Other beneficial uses

Small volumes of concentrate have been used occasionally for dust suppression, roadbed stabilization, soil remediation, and de-icing. Such applications however are very site-specific and can only be used as a supplemental concentrate disposal alternative.

2.9 Management of residuals generated at desalination plants

2.9.1 Pretreatment process residuals

Table 2.7 identifies residuals that may be produced in the pretreatment process when applying membrane desalination. The amount of residuals produced is primarily a function of the feedwater quality relative to the constituents which must be removed prior to the membrane desalination process. Surface, seawater and wastewater to be treated for reuse all have significant levels of suspended solids, for example. These solids must be removed prior to treatment with reverse osmosis, either in a backwash stream or as sludge. Other than the concentrate stream, these solids create the most significant residual stream from a desalination plant.

Table 2.7 Residuals from membrane desalination processes

Residual	Source or cause	Application
Backwash Solids/Sludge	Suspended solids in the feedwater	Open intake seawater, brackish surface water
Backwash water	From removal of suspended	Open intake seawater, brackish

	solids in the feedwater	surface water
Cleaning Solutions (see Table 3.3)	Cleaning of filtration membranes (MF/UF) and process membranes (RO, NF, ED)	Open intake seawater, brackish surface water
Concentrate or blowdown (if cross flow)	Filtration membranes operating in a cross flow mode	Open intake seawater, brackish surface water
Spent media (sand, anthracite and/or garnet)	From the removal of suspended solids in the feedwater	Open intake seawater, brackish surface water
Cartridge Filters – polypropylene	Final fine filtration prior to RO, periodic replacement	Most membrane desalination processes, except those using MF/UF filtration membranes
MF/UF membranes – polymeric material (polypropylene, polysulphone, polyvinylidene-fluoride (PVDF), cellulose acetate)	Membrane replacement for MF/UF systems	Open intake seawater, brackish surface water
RO membranes (polyamide thin film composite, cellulose acetate)	Membrane replacements.	Open intake seawater, brackish surface water

2.9.2 Management of spent pretreatment filter backwash water

Spent filter backwash water is a waste stream produced by the membrane plant's pretreatment filtration system. Depending on the type of pretreatment system used (granular or membrane filters) the spent filter backwash water will vary in quantity and quality. In general, the membrane pretreatment systems produce 1.5 to 2 times larger volume of spent filter backwash water than the granular media filters. However, contrary to the MF or UF membrane pretreatment filters, the granular media filters require their feed water to be preconditioned with coagulant (usually iron salt) prior to filtration. This typically adds 60 to 80 percent of additional solids load to the spent filter discharge, and therefore its disposal typically results in higher solids handling costs. Spent pre-treatment filter backwash water may include filter aids and coagulants. The spent filter backwash water can be handled in one of the following methods.

Discharge to a surface water body along with plant concentrate without treatment is one of the most widely practiced filter backwash water disposal methods. This method is typically the lowest cost disposal method because it does not involve any treatment prior to disposal. This method is suitable for discharge to large water bodies with good flushing – such as open oceans or large rivers.

On-site treatment prior to surface water discharge or recycle upstream of the filtration system are possible options. The filter backwash water must be treated at the membrane treatment plant when its direct discharge does not meet surface body water quality requirements, or if it is not suitable for a direct disposal to deep injection wells. Typically, the most widely used granular media backwash treatment method is gravity settling in conventional or lamella plate sedimentation tanks. Spent wash water from membrane pretreatment systems is usually treated in separate MF or UF membrane modules. Filter backwash sedimentation tanks are often designed for a retention time of 3 to 4 hours and allow removing more than 90 percent of the backwash solids. The settled filter backwash water can be either disposed with the membrane plant concentrate or can be recycled at the head of the pretreatment filtration system. In many

cases it is more cost-effective to recycle and reuse the settled filter backwash water rather than to dispose it with the concentrate. However, blending and disposal with the concentrate may be more beneficial, if the concentrate water quality is inferior and therefore, it cannot be disposed of to a surface water body without prior dilution with a stream of lesser salinity. The solid residuals (sludge) retained in the sedimentation basin are often discharged to the sanitary sewer in a liquid form (typically practiced at small to medium size plants) or dewatered onsite in a designated solids handling facility.

2.9.3 Management of spent (used) membrane cleaning solutions

The accumulation of silt or scale on the membranes causes fouling which reduces membrane performance. The desalination system membranes have to be cleaned periodically to remove foulants and extend the membrane useful life. Typical cleaning frequency of the membranes is twice to four times per year. Typically one membrane train is cleaned at a time. To clean the membranes, a chemical cleaning solution is circulated through the membrane train for a preset time. After the cleaning solution circulation is completed, the spent cleaning solution is evacuated from the train to a storage tank and the membranes are flushed with permeate (flush water). The flush water is used to remove all the residual cleaning solution from the RO train in order to prepare the train for normal operation. The flush water for membrane cleaning is stored separately from the rest of the plant permeate in a flush tank.

The various waste discharge volumes which are generated during the membrane train cleaning process are described below:

- Concentrated waste cleaning solution is the actual spent membrane cleaning chemical.
- Flush water-residual cleaning solution (first flush) is the first batch of clean product water used to flush the membranes after the recirculation of cleaning solution is discontinued. This first flush contains diluted residual cleaning solution.
- Flush water-permeate is the spent cleaning water used for several consecutive membrane flushes after the first flush. This flush water is of low salinity and contains only trace amounts of cleaning solution.
- Flush water concentrate is the flush water removed from the concentrate lines of the membrane system during the flushing process. This water contains very little cleaning chemicals and is of slightly higher salinity concentration than the permeate used for flushing.

All the membrane cleaning streams listed above are typically conveyed to one washwater tank often named “scavenger tank” for waste cleaning solution retention and treatment. This tank has to be designed to be able to retain the waste cleaning solution from the simultaneous cleaning of a minimum of two membrane trains. The scavenger tank should be equipped with mixing and pH neutralization systems. The mixing system is recommended to be installed at the bottom of the tanks to provide complete mixing of all four cleaning solution streams listed above. After mixing with the flush water, the concentration of the cleaning solution chemicals will be reduced significantly. The used cleaning solution should be neutralized to pH level compatible with the pH requirements for discharge to the wastewater collection system. At

many plants, only the most concentrated first flush is discharged to the wastewater collection system. The rest of the flush water usually has only trace levels of contaminants and is most often suitable for a surface water discharge (i.e., discharge to the ocean or other nearby water body).

2.10 Small desalination systems

Small desalination systems are defined as facilities that produce 4000 m³/day (about 1 MGD) or less of drinking water. In most cases, small desalination systems use treatment technologies similar to those applied for large desalination plants. Small desalination systems may be classified in various categories depending on the used technology; on their mobility; and their service. In terms of technology, small desalination systems, similar to large plants, can be divided into two groups: membrane and thermal facilities. In terms of mobility, small plants can be divided into stationary and mobile units. Depending on their service, small plants are classified as: single point of use (POU) and multiple-point-of use systems. All of these systems should be tested against performance standards and should demonstrate their ability to reliably produce safe drinking water under their appropriate use conditions. The specific areas of allocation and technology used for the various small desalination systems are described below.

2.10.1 Small applications for thermal desalination

Mechanical vapour compression (MVC) systems are a special subset of MED evaporators which incorporate a rotating mechanical vapour compressor as the means of heating the process (see Figure 2.8). Typically MVC compressors are rotated by electric motors or sometimes engines. MVC systems were very common for small applications prior to the commercial availability of reverse osmosis plants. These plants can produce distilled water from almost any salinity of feedwater yet do not require a heat source (and therefore do not need cooling water). Typically a MVC unit has recovery of 40-50% when operating on seawater and can yield much higher recoveries (70 to 85 %) when using brackish water. MVC systems have found applications in remote locations with robust equipment requirements, such as oil rigs and some marine vessels, and for production of boiler feedwater for power plants from seawater. Other MVC applications include the production of potable water for bottling and various pharmaceutical grades of water. Most MVC plants produce 10-200 m³/d of distilled water although a few installations producing up to 2500 m³/d have been built.

Small distillers (Figure 2.9) are another special subset of MED systems which are usually configured to use hot water from engines or other industrial processes. Typically the systems have only one or two effects making them thermodynamically inefficient. However, they are designed for small volume applications in situations concurrent with large quantities of heat (which generally use once-through cooling whether desalination is present or not). Similar to MVC plants, small stills have found some application in oil rigs, marine vessels (including cruise ships) and for boiler water production for power plants. These units typically have capacities between 1 and 50 m³/d and usually have maximum evaporation temperatures of 60-80°C.

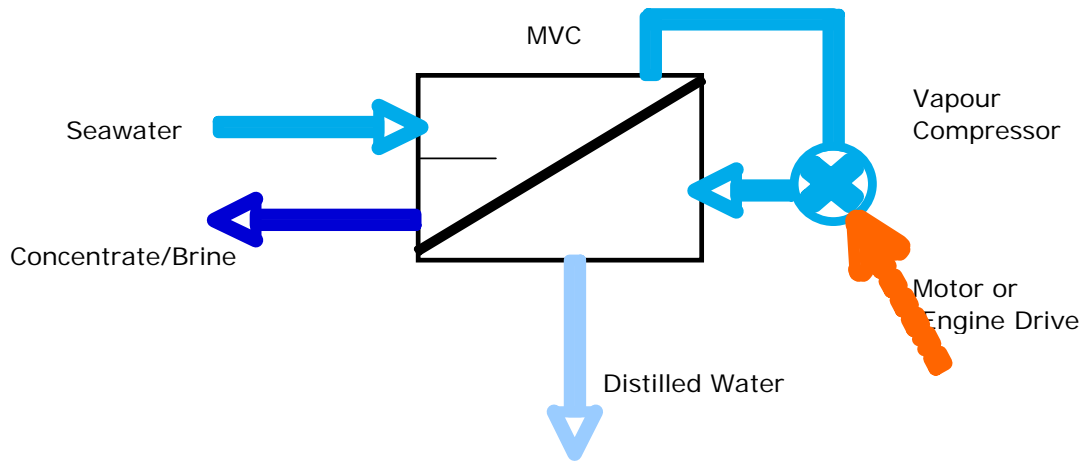


Figure 2.8 General schematic of a mechanical vapour compression unit

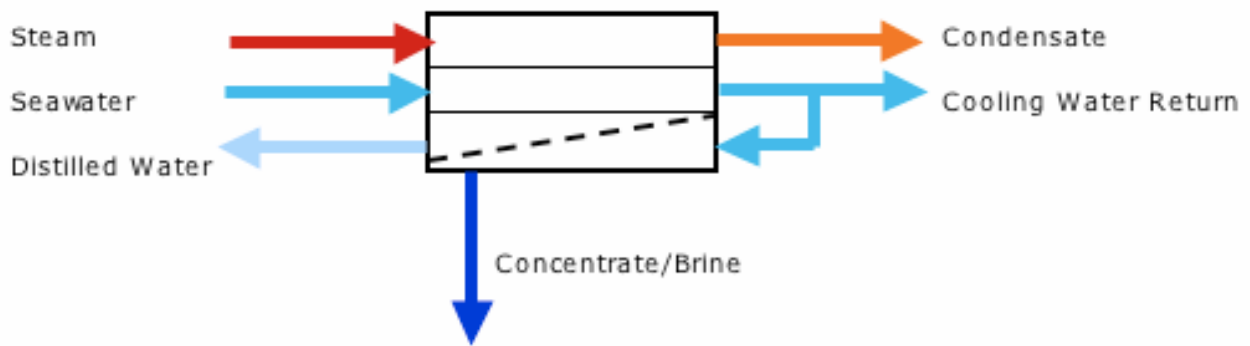


Figure 2.9 General schematic of a small distiller unit

Small MSF systems are often found in merchant marine, naval and commercial cruise ships. Steam or hot water from marine diesel engines may provide the heat to drive the process. Typically these systems are used in applications where there is a small localized demand for water coincident with a relatively large amount of (waste) heat. Small thermal MSF systems produce between 100 and 1000 cubic metres of water per day. These systems are typically not used to produce drinking water and are typically applied for industrial purposes.

The key issues for small thermal systems are the same as for large units. The only exception is that small stills and small MSF systems are typically designed for offshore marine applications with the result that on-shore use may require a disproportionately high cooling water flow.

2.10.2 Small membrane desalination plants

Small membrane desalination plants have found wide use in land-based applications: for supplying potable water to hotels and resorts, to small and remote residential communities and to military installations. This type of plants is also very popular for sea-based mobile applications. Small membrane desalination plants are typically compact seawater or brackish water treatment systems that are configured in one skid and often referred to as package plants. For small skid mounted systems, it is common to have the pretreatment chemical injection points, cartridge filter, feed pump, and membranes and pressure vessels on the skid. For larger systems, the pretreatment components and feed pumps are typically not located on the rack supporting the membranes and the pressure vessels. In contrast to large membrane desalination systems, which are designed to minimize overall lifecycle water production costs, small systems are typically configured and designed with features that aim to simplify facility installation and operation. Often these systems are built and assembled in a manufacturing shop away from their point of application, and then shipped in a container to the location of their installation and use. Large desalination plants typically use 8-inch (~20 cm) membrane elements; small membrane desalination units may be designed to operate with smaller size (2-inch ~5 cm or 4-inch ~10 cm) membranes. In addition, these plants often apply a more simplified pretreatment system that may include just a series of 20-micrometre 10-micrometre and 1-micrometre cartridge filters, rather than granular or membrane pretreatment filters. Small membrane desalination units often use a number of water quality polishing technologies such as activated carbon filters, ion-exchange filters and UV disinfection systems.

Although small membrane desalination plants use similar reverse osmosis or nanofiltration membranes as large-size plants, these systems are often not as sophisticated in terms of automated source and product water quality monitoring and control. Therefore, operator training and skills are very important in order to maintain safe and cost-effective drinking water production. If skilled operations staff is not readily available, the system owner should request the system supplier to design the system with automated shut-down provisions which trigger discontinuation of system operations when the integrity of the pretreatment system or membrane system equipment is breached or when unusually high values of key parameters such as turbidity and conductivity are reached. Use of series of disinfection and pathogen control devices such as carbon filters followed by 1-micron cartridge filters followed by UV irradiation or chemical disinfection is recommended rather than reliance on a single technology for disinfection, especially if the system is not run by skilled operator or is unmanned for the majority of the time.

2.10.3 Small stationary desalination plants

Small stationary desalination plants may use both thermal and membrane desalination technologies, however, unless an easy-to-access steam source exists, membrane desalination systems are usually the preferred choice for small stationary applications due to their more compact size and lower overall energy demand. A typical stationary membrane desalination system will have the following key elements located on one skid: (1) connection piping to a water source; (2) booster pump to pretreatment system; (3) sand/solids separator; (4) granular multi-media pressure filters or membrane filters; (5) 1 to 8 membrane vessels with salt-separation membranes; (6) chemical injection systems for coagulant; biocides, sodium bisulfite and antiscalant (9) disinfection system using UV irradiation or chlorination.

2.10.4 Mobile desalination plants for emergency water supply

Mobile desalination plants are easy to transport modular water treatment systems that are designed to be deployed in zones of natural calamities (earthquakes, floods, etc.), military operations and other humanitarian crisis conditions, and to operate with practically any water supply source, including waters contaminated with raw wastewater, high solids content, oil and grease, organics, pesticides and wastewater. The water treatment equipment incorporated in these types of systems is installed in sturdy metal frames (racks) designed to withstand the weather elements and long-distance transportation on trucks and airplanes. The source water pretreatment system typically includes chemical chlorination and dechlorination, strainers, grit separators and centrifuges for solids removal, granular media filtration, including sand filters and activated carbon filters, followed by cartridge filters and reverse osmosis membrane system. In some cases, pretreatment may be provided by ultrafiltration system instead of granular media filter. Drinking water disinfection for such systems is provided by chlorination and UV irradiation. Usually these units are supplied with electricity by a diesel-powered generator.

Compared to stationary and large desalination plants, the operation of mobile systems requires substantially larger amounts of consumables, especially if the source water is contaminated with oils and is very turbid. The operation of these systems is limited by the source of energy available for their operation. Water quality produced by some of these systems may not always meet drinking water regulations for all parameters, but the systems can be designed to produce water of quality adequate for protection of health.

2.10.5 Marine vessel (ship/boat) desalination plants

Most marine vessel installations, including cruise ships, military ships, yachts, and boats use membrane seawater desalination for fresh water supply. This type of small desalination plants are typically constructed with light weight epoxy powder-coated aluminium or steel frames and can be provided with explosion proofing and fully automated monitoring and control systems that maintain consistent water quality at all times. Usually, the marine-vessel membrane desalination plants have the following elements: source water connection pipe; booster pump, dual media granular filters; oil/water separator; high-pressure feed pump; high-rejection/high-flux reverse osmosis membrane elements; corrosion proof fiberglass pressure vessels; product water post-filtration skid with activated carbon unit and UV disinfection system. For applications with seawater of potentially high solids content, hydrocyclone separators are added ahead of the granular media filters for longer cartridge filter and RO membrane life.

2.10.6 Off-shore seawater desalination facilities

Currently, there are commercially available membrane seawater desalination plants installed on large ships, which are specifically designed and build with the prime purpose to produce fresh water (Sessions & Hawkins (2006)). These facilities offer some benefits over the land-based desalination facilities, such as: avoiding the construction of costly source water intake and ocean outfall discharge facilities; reducing the impact of the concentrate discharge on the marine environment; collecting source water from pristine off-shore waters, and simplifying the plant permitting process. The intake structure of the vessel is constructed as a part of the vessel hull and is equipped with screening facilities. The pretreatment system is simplified bag-filtration facility housed in a high density polyethylene (HDPE) casting. The RO system incorporates high

pressure pumps and membrane racks and is equipped with energy recovery equipment. The produced water is stored on the ship. The marine vessel that is used for this floating water production facility will be connected to a shore terminal via seabed pipeline, which will deliver the potable water to the shore. The actual water production will be completed off-shore. During the production of desalinated water, the ship is typically located adjacent to natural gas platform in the sea, which will be used to run the desalination plant pumps. These pumps are equipped with dual-fuel gas turbines.

The systems discussed above must be suited to the particular application to provide reliable and consistent performance. The marine-based systems must meet the safety standards applicable for the marine industry. Independent performance testing is recommended to confirm conformance with applicable regulations prior to deployment. The system should be equipped with automated fresh water flush at each shut down and approximately every 7 days to maintain the performance integrity of the membranes.

2.10.7 Point-of-use systems

Point-of-use (POU) systems are small desalination facilities which are designed to serve individual households and small industrial and commercial establishments. Since only a very small percentage (~1 %) of the total water use is for direct consumption, POU systems could be a very cost effective way of treatment of specific water quality issues associated with the distribution systems and/or the source water. Most of these are used to upgrade distributed fresh waters. POU reverse osmosis devices typically use two to four litres of distribution system water to produce one litre of drinking water – i.e. their installation would result in an elevated use of water at a given location. The fluctuation in RO efficiency is due to many factors that continually change within the RO membrane system, including incoming water pressure, backpressure produced by the storage tank and age and condition of the RO membrane itself. The elevated water use associated with the installation of POU systems is an important concern in areas with stringent water conservation programs where excessive use of water is penalized by additional fees.

POU systems are typically installed at a single tap such as the kitchen sink. Usually, these systems consist of containerized treatment equipment that is combined in a treatment sequence mainly to address concerns with taste, odour, colour, hardness, or other aesthetic problems associated with the use of the treated potable water. The POU system configuration is very dependent on the water quality challenges this system is addressing. Usually, POU systems are not intended for reliable treatment of microbial contamination, but some have been tested and approved for those situations. Typically, the POU systems are not subjected, on a daily operational basis, to local authority scrutiny, but rely more on “class” or accepted standards usually established by a national or international standards and certification organization, which outlines guides and specifications for the expected performance characteristics. The following issues should be taken into consideration during POU system installation and operation:

- Location of equipment;
- Installer’s and operator’s skill levels;
- Installer’s and operator’s training and certifications;

- Local installation Codes;
- Installation documentation.
- Maintainer's skills, training, certifications;
- Component regeneration/replacement.

In remote areas customer may not be fully aware of desalination concepts or principles. Cultural adjustments may be required especially if some degree of individual expenses are involved for the water delivered. Each POU equipment should have a performance indication device (PID) which alerts the user when the unit is no longer meeting treatment standards.

2.11 Conclusions and Recommendations: Desalination technology and technical issues

2.11.1 Summary guidance

Seawater is typically desalinated using two general types of water treatment technologies: thermal evaporation (distillation) and reverse osmosis (RO) membrane separation. Both types of technologies are very reliable and are capable of producing high-quality drinking water of consistent quality and quantity.

Desalination systems intake facilities

Two general types of intake facilities are used to obtain source water for the desalination plants: subsurface intakes (wells, infiltration galleries, etc.) and open intakes. Wells are either vertical or horizontal source water collectors typically located on the seashore, in a close vicinity to the ocean. These intake facilities are relatively simple to build and the seawater they collect is naturally pretreated via slow filtration through the subsurface sand/seabed formations in the area of source water extraction. Raw seawater collected using wells is usually of better quality in terms of solids, silt, oil & grease, natural organic contamination and aquatic microorganisms, as compared to open seawater intakes. Sometimes, beach intakes may also yield source water of lower salinity. Vertical beach wells are usually less costly than the horizontal wells; however their productivity is relatively small (typically, 400 m³/day to 4000 m³/day) and therefore, the use of vertical wells for large plants is less favourable. The most widely used type of horizontal collector beach wells are often referred to as Ranney collector wells.

Open ocean intakes for large seawater desalination plants are often complex structures including intake piping which typically extends several hundred to several thousand meters into the ocean. Source water collected through open intakes usually requires pretreatment prior to reverse osmosis desalination. The cost and time for construction of a new open ocean intake could be significant and could reach 10 to 20 percent of the overall desalination plant construction cost. Open ocean intakes would result in some entrainment of aquatic organisms as compared to beach wells because they take raw seawater directly from the ocean rather than source water pre-filtered through the coastal sand formations.

Well intake considerations

Key drinking water quality considerations when using well intakes include:

- The subsurface conditions and sustainable capacity of the source water aquifer have to be commensurate with the size and quality of the drinking water. Well intakes are usually suitable for desalination plants of capacity lower than 20,000 m³/day ;
- Source water aquifer contamination with man-made pollutants such as: NDMA, dioxins, petroleum products, pesticides, pharmaceuticals, groundwater leakage from industrial facilities, mortuaries, etc., may make the brackish or coastal aquifer unsuitable for production of drinking water or require very elaborate and costly pretreatment and product water conditioning to inactivate these pollutants.
- The levels of iron and manganese in the brackish water or coastal aquifers may exceed the WHO guideline levels. Therefore, elevated content of iron and manganese in the source water may require the use of elaborated technology for their removal, such as greensand filters, etc. The levels of iron and manganese in the brackish water or coastal aquifers may exceed the WHO guideline levels; pretreatment may be required.
- Elevated content of hydrogen sulfide (H₂S) in the source water aquifer may have negative impact on taste and odour of the drinking water;
- Installation of well intakes in wetland areas is not desirable because it may cause wetland drainage and significant environmental impacts. In addition, such source water may be of fluctuating quality, which in turn would require more elaborate treatment.
- Intake wells usually collect colder water than open-ocean intakes. Desalination of colder water requires more energy and would be more costly.

Open intake considerations

- Open intakes are suitable for desalination plants of all sizes.
- Source water from open intakes is typically of higher turbidity, silt and organic content than well water. Therefore, the use of this type of intake usually requires more elaborate source water pretreatment to produce the same drinking water quality.
- Avoid locating open intakes of desalination plants near to (within 500 meters of) a water and wastewater treatment plant discharge. Water and wastewater plant discharges typically contain elevated concentrations of metals such as iron, copper, nickel, aluminium, lead, etc., which may cause irreversible fouling of desalination membranes and interrupt drinking water production.
- Avoid locating open intakes in large industrial and municipal ports due to increased potential for source and drinking water contamination with petroleum products, raw wastewater, and waste from chemical spills.
- Avoid locating seawater open intakes in the vicinity of fresh water discharges to the ocean, such as river estuaries, coastal marshes and large storm drain canals, because these discharges may carry large amounts of silt and organic materials which may cause significant biofouling of the membranes and equipment of the desalination systems and may increase the disinfection by-product content of the drinking water.

- Algal blooms negatively impact source water quality and may result in elevated organics in the source water and accelerated biofouling of seawater reverse osmosis (SWRO) installations. Red tide algal blooms may result in the release of algal toxins of small molecular weight, such as domoic acid and saxitoxin, which may impact product water quality, however, these are well removed by desalination treatment. In order to minimize the entrance of algal material in the open intake, locate the source water intake structure at least 5 meters under the ocean surface and design the intake so the water entrance velocity is less than 0.2 meters per second. The low entrance velocity would also allow minimizing entrainment of marine organisms with the collected source water.
- Use the intake or discharge of existing power plant to collect source water for the desalination plant, if feasible, in order to minimize the need for construction of new intake and discharge and the associated disturbance of the benthic organisms in the intake area.
- Avoid locating the desalination plant's source water intake in ocean zones of endangered or rare species to minimize the environmental impact associated with the construction of desalination plants.

Source water pretreatment facilities and chemicals

The need and type of source water pretreatment depends on the source water quality and the type of technology used: thermal or membrane desalination. In all cases the chemicals used for pretreatment should be of high-quality ("food-grade") and should contain very low levels of impurities, such as metals, dust, etc. Use of lower quality, industrial-grade water chemicals for production of drinking water should be avoided.

Specific guidelines associated with pretreatment systems for membrane and thermal desalination are discussed below:

Pretreatment for membrane desalination operations

The following drinking water quality related issues should be taken under consideration when selecting pretreatment for membrane desalination systems:

- Continuous source water chlorination is not recommended because chlorine addition creates large amount of disinfection byproducts (TTHMs of 500 to 2,000 mg/litre or higher), especially if the source water is of high organic levels. Apply intermittent chlorination instead.
- Dechlorinate the pretreatment system effluent after chlorination in order to protect the structural integrity of the SWRO membranes and to produce consistent product water quality.
- Do not chloramine raw seawater prior to membrane separation. Chloramination generates both chloramines and bromamines. While chloramines are disinfectants with low oxidation potential and do not present threat for the SWRO membranes, bromamines have order-of-magnitude higher oxidation strength and their presence in the feed water to

the SWRO system can cause rapid loss of membrane integrity and deterioration of drinking water quality. Chlorine or chlorine dioxide are preferred to control excessive bio-growth in the intake, pretreatment and RO systems.

- Use of ferric salts for source water coagulation prior to filtration may result in reddish discolouring of the plant discharge. Treat the spent filter backwash water from granular media pretreatment systems using coagulants (ferric sulfate, ferric chloride, etc.) and settle this sidestream prior to discharge to surface waters in order to avoid the discolouring of the desalination plant discharge.
- MF and UF membrane pretreatment systems do not require chemical conditioning of the source water to produce effluent suitable for SWRO desalination. Therefore, the spent backwash water from these systems typically has a less significant environmental impact

Pretreatment for Thermal Desalination Systems

- Performance of thermal desalination systems is significantly less sensitive to source water quality than membrane desalination plants. Therefore, physical pretreatment of the source water is simpler and is often limited to screening to remove coarse debris in order to prevent equipment erosion by suspended solids.
- Chemical pretreatment of thermal desalination systems is more robust than that of membrane systems and is aimed at minimising scaling and corrosion of the heat exchanger surfaces, and minimising effects of oil and grease from the source water.
- Cooling water stream is typically treated to control fouling using an oxidizing agent or biocide.
- Makeup water is conditioned with scale inhibitors.

Thermal desalination processes

- Thermal desalination is the predominant technology for seawater desalination under conditions where power generation and water production are combined. The three key technologies used for thermal desalination are MSF, MED and VC.
- Multi-stage flash distillation is the most widely used thermal desalination technology.
- Thermal desalination plants produce distilled water of very low TDS (2 to 50 mg/L), boron, sodium and bromides;
- A potential exists for thermal desalination processes to distil volatile organic compounds, if they are present in the source water, unless they are removed by venting, external pretreatment or re-aeration.
- Thermal desalination results in a cooling water discharge of elevated temperature (8 to 12 °C). Most commonly this cooling water is blended with the brine from the distillation process. Brine's temperature is typically 5 to 25 °C warmer than the ambient seawater.
- Cooling water from thermal desalination treatment processes may contain trace amounts of corrosion inhibitors and disinfection by-products.

Membrane desalination systems

- Membrane desalination is a prime choice for areas of the world where low-cost fuel sources are not readily available and power and water production facilities are separated.
- Membrane desalination is practiced using brackish water, seawater and highly treated wastewater effluent as source water.
- There are two principal types of membrane desalination: reverse osmosis (RO) and electrodialysis (ED). ED-based desalination is widely used for low-salinity water sources (TDS < 3000 mg/litre). Reverse osmosis and nanofiltration are used for source water of any salinity and type.
- Seawater RO membrane systems provide efficient removal of pathogens (bacteria, viruses, Giardia and Cryptosporidium); organics of molecular size of 200 Daltons or larger, e.g.: disinfection by-products; algal toxins; and so-called endocrine-disruptor-type compounds.
- ED systems do not provide pathogen reduction.
- RO system performance and efficiency are dependent on source water quality (TDS, temperature, scaling compounds, etc.) and physical and chemical pretreatment.
- The level of pretreatment needed for successful operation is primarily a function of source water quality of solids, oxidizing agents, oil and grease, and temperature.
- Membrane material integrity is depended on various factors, including source water pH, temperature, organic content, concentration of oxidants and oil and grease in the water, and solids content.

Post-treatment

- Post-treatment of the product water from the desalination processes includes: stabilization by addition of carbonate alkalinity; corrosion inhibition; re-mineralization by blending with source water; disinfection and enhanced removal of specific compounds (i.e., boron, silica, NDMA, etc.).
- Stabilization by addition of calcium carbonate alkalinity is the most widely used approach for corrosion control of metallic pipelines and distribution systems;
- Corrosion inhibition is the most popular post-treatment method for plastic pipelines and distribution systems;
- Sodium hypochlorite and chlorine gas are most widely used for disinfection of desalinated water;
- Use of chloramines instead of chlorine for disinfection is more advantageous when product water must be conveyed over long distances (over 100 km) or stored for long periods of time (several days) due to the significantly lower decay rate of chloramines compared to free chlorine.
- Use of ozone as a disinfectant for desalinated water has the potential of forming disinfection by-products and bromate.
- Blending of desalinated water for re-mineralization is suitable with brackish water, and only up to about 1% with seawater. The raw water used for blending should be pretreated for chemical and microbial control prior to mixing with the desalinated water.

Concentrate management

- Concentrate (brine) generated during the desalination process should be disposed of in an environmentally safe manner.
- Concentration of minerals in the brine is usually 2 to 10 times higher than that of the source water and is function of the TDS of the source water and the plant recovery.
- Most widely used method of disposal of concentrate from seawater desalination plants is discharge to a nearby surface water body via outfall;
- Co-discharge of desalination plant concentrate and cooling water from power plants is advantageous where possible because it accelerates dissipation of both the high-salinity plume from the desalination plant and the thermal plume from the power plant.
- Co-discharge with wastewater treatment plant effluent may cause potential toxicity problems with certain marine organisms (i.e., red sea urchins, stars, sand dollars, etc.) that may not adapt easily to the blend.
- Concentrate discharge to sanitary sewers impact wastewater treatment plant performance and the suitability of the treatment plant effluent for reuse.
- Technologies for beneficial reuse of concentrate may offer a number of benefits if viable.

Management of residuals from pretreatment systems

- Use of ferric salts for source water coagulation prior to filtration may result in reddish discolouring of the plant discharge. See ***Pretreatment for membrane desalination operations.***

Use of MF and UF pretreatment systems results in production of 50 to 80 % less residual solids than that of conventional granular media filtration. However, UF and MF systems generate 3 to 5 % larger volume of waste backwash water than granular media filters.

- MF and UF membrane pretreatment systems do not require chemical conditioning of the source water to produce effluent suitable for SWRO desalination. Therefore, the spent backwash water from these systems is less harmful for the environment.
- Currently spent backwash water from pretreatment filter systems is typically discharged to the ocean without treatment. However, if the spent backwash water is planned to be discharged to areas with impaired marine life, than spent filter backwash treatment by sedimentation and sludge dewatering is recommended. The dewatered solids removed from the source water are recommended to be disposed to a sanitary landfill.
- Spent chemical cleaning solutions from UF, MF and SWRO membrane treatment are recommended to be discharged to the ocean but to be disposed to the sanitary sewer instead. Membrane flush water generated after the disposal of the membrane cleaning chemicals is typically safe to dispose to the ocean.

Small desalination systems

- Small membrane desalination systems have found wide application for production of drinking water on cruise ships, military marine vessels, and boats.
- Easy-to-transport package desalination plants are very suitable to provide emergency water supplies to areas impacted by natural disasters.

- Point-of-use (POU) desalination units installed on the water tap are often installed to improve the quality of the delivered drinking water and/or to provide additional water treatment in terms of taste, odour and specific contaminants (i.e., arsenic, iron, manganese).
- POU membrane units should not be relied upon to provide consistent pathogen removal and protection, unless they have been independently tested and certified for pathogen control.
- Installation of desalination POU systems results in an increase of the total amount of water used at a given location and would result in increased water costs for the user.

2.11.2 Research

Develop analytical methods for analysis of metals, suspended solids and organic compounds in brackish and seawater to be able to better characterize source water quality. Existing standard analytical methods are developed for analysis of low-salinity (fresh) water and the results from their use are affected by the high level of dissolved solids in seawater and brackish water.

- Document the rejection of frequently encountered algal toxins (saxitoxin; domoic acid, okadaic acid, etc.) from seawater by reverse osmosis membranes and the removal of these compounds by thermal desalination systems;
- Document the rejection of frequently encountered man-made organic contaminants (pharmaceuticals, cosmetic products, NDMA, etc.) by seawater and brackish water membranes and determine the removal of these compounds by thermal desalination systems.
- Determine strategies for reliable disinfection and corrosion inhibition of desalinated water conveyed over long distances in warm climates.
- Develop reliable methods for on-line assessment of the integrity of seawater reverse osmosis membranes.
- Document log-removal of key pathogens (total coliforms, *Giardia*, *Cryptosporidium*, *Legionella*, bacteria and viruses) by brackish water and seawater desalination membranes and thermal desalination systems.
- Study effect of ozonation on disinfection by-product formation in desalinated seawater and brackish water.
- Study the use of chlorine dioxide for pretreatment of seawater treated by reverse osmosis.
- Document the effect of various pretreatment disinfectants on the level and type of disinfection by-products in the desalinated seawater produced by SWRO systems.

Note: Figures in this chapter courtesy of Corrado Sommariva
Tables in this chapter courtesy of Nikolay Voutchkov

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Chemical Aspects of Desalinated Water

The internationally recognized compendium of information on the health and safety considerations associated with drinking water is the Guidelines for Drinking-water Quality (GDWQ) (WHO, 2004) along with the other associated technical documents and guidances produced by the World Health Organization. Those guidelines are developed with respect to the more traditional fresh water sources of drinking water and the technologies and approaches for assuring the healthfulness of the drinking water that is produced. This volume and this chapter deal specifically with production and distribution of drinking water by desalination processes from saline sources. Virtually all of the principles and information in the GDWQ are applicable in desalinated water; however, this assessment was undertaken because there are some additional matters that arise from desalination that are not normally issues for fresh water supplies.. The guidance developed from this process is intended to augment what is in the GDWQ, and provide recommendations for desalination related issues to be considered for incorporation in future revisions of the GDWQ.

3.1 Chemicals and desalination

Chemicals occur in the desalination process from a series of origins. These include from the source water, and chemicals that are used in the process to aid its efficient functioning, to ensure microbiological safety, or to stabilize the water before it enters the distribution system, and to control corrosion from contact surfaces during storage and distribution to consumers. Many of these are the same as would be encountered in conventional drinking water sources and supplies but there are a number that are of particular relevance for desalination. Since the process is based on removal of inorganic salts most of them will not reach the final water in more than trace quantities and so will not pose a risk to consumers; others will be significantly reduced in concentration. However, chemicals will not be entirely removed and some will be added post-process and will, therefore, reach consumers. In addition, some of the inorganic ions that are removed may be of nutritional significance and, therefore, potentially beneficial.

The different processes used in desalination will have, to some extent, different requirements for chemical additives and differences in the removal of chemicals from the source water but there will be a considerable overlap.

The assessment process includes:

- Natural and anthropogenic chemicals in source water
- Chemicals used or introduced during pre-treatment
- Added chemicals and by-products of chemical reactions
- Chemicals added to aid the better performance of the process
- Chemicals added post-treatment
- Contaminants and corrosion products from contact surfaces

Consideration of any potential risks will depend on a number of factors, not least of which is vulnerable sub-populations that might be exposed. Groups such as dialysis patients are not considered here as the primary focus is drinking water and this is a medical intervention that will require further water treatment to ensure that it meets the very stringent requirements. However, bottle-fed infants are one such group because of their proportionally high intake of water and their developing physiology, which means that they may be less able to handle high concentrations of some natural constituents such as sodium.

In addition, many desalination-dependant locations and countries are in arid regions, where consumption of water may be higher than the norm of 2 litres per day for adults, 1 litre/day for 10 kg child, and 0.75 litres per day for the 5 kg infant used by WHO in developing guidelines for drinking water quality, therefore, water consumption rates and dietary habits also need to be considered by health authorities when establishing local standards or guideline values (WHO, 2004).

As with other water supplies, the approach to assuring the safety of desalinated water for drinking water should follow the Water Safety Plan approach applied to an individual supply. This requires identification of the hazards and assessment of the risks, determination that appropriate barriers are in place to remove the hazards or mitigate the risks and action to ensure the barriers are always optimised. It also requires that consideration be given as to whether an intervention to control or mitigate risks from one hazard will impact on other hazards and risks. In this respect it is also important to make a comparative assessment of risks so that minor risks are not solved at the expense of increasing more significant risks (WHO, 2005). This is particularly relevant for chemicals in relation to desalination processes. The following discussion considers the chemicals and sources of chemicals that could, potentially, be present in raw source water or introduced during the various stages of producing desalinated water and its final preparation for drinking water. One potential difference with desalination is the use of sea water or other water sources for blending with the final desalinated water. Water used for blending also needs to be considered and treated appropriately under the water safety plan since such water could be a source of contamination of the final drinking water.

3.2 Chemicals in source water

The term source water applies to both the saline water that will be the feed to the desalination process and also the potentially saline water source that is used for blending. As with water that will undergo desalination, the level and type of pre-treatment applied to blending water will be a significant consideration.

Many inorganic chemicals are found naturally in the seawater or brackish water used as the feed for desalination. These include all of the inorganic chemicals that the process is designed to remove, including sodium chloride, but it will include some that may impact on the pre-treatment, and potentially post-treatment, stage, such as bromide and, to a lesser extent, iodide.

Boron and bromide

Most of the inorganic components will be significantly removed in the desalination process, either thermal or RO, although some sodium chloride and bromide may be present in the treated

water from membrane plants and possibly from some older distillation plants. In terms of key contaminants of direct interest for health and environment, the most important is probably boron, which can be of significance in reverse osmosis plants since the rejection ratio of boron (probably mostly as borate) is less than that for most other inorganics. The current WHO guideline value for boron (borate) in drinking water is 0.5 mg/litre, however, this is due to be reconsidered under the rolling revision of the Guidelines (WHO, 2004). Although a health based guideline might possibly be 1 mg/litre or higher, there are plants that are sensitive at 0.5 mg/litre. The latter might become the principal issue for residual boron i.e. its effect as an herbicide if present in sufficient amount in irrigation water, particularly in areas where rainfall is so low as to not cause leaching of salts from soils.

Bromide is initially present in seawater in relatively large amounts (~70 to 80 mg/litre), so even high (e.g. >95%) percentage removals will allow some bromide on the order of 1 to several mg/litre to be present in the finished water. The concentrations of bromide in desalinated water will be somewhat in proportion to the chloride concentration. Inorganic bromide is also present in many fresh waters at milligram levels, especially ground waters. If ozonation is applied to waters with sufficient residual bromide, bromate will be formed and likely exceed the current GDWQ value of 10 µg/litre. Packaged waters produced by bottling distributed desalinated waters derived from high bromide source water are often treated by ozonation prior to bottling. This would increase the bromate levels in the bottled water beyond the original distributed water if residual bromide is present. Production of chlorine by electrolysis of sea water will also produce large amounts of bromate. WHO/FAO JMPR (1988) has developed an ADI for bromide of 1 mg/kg body weight and assuming a 60 kg adult drinking 2 litres of water per day with a 20% allocation of the ADI to drinking water could give a health-based reference value in the range of 6 mg/litre. Inorganic bromide in desalinated water would generally not be expected to constitute a threat to health, even if sea water were added, however a WHO Guideline would be appropriate to remove any uncertainty among water producers.

Sodium and potassium

There is no health-based guideline value for sodium, which is normally present in relatively low concentrations in drinking waters derived from fresh water sources but with significant exceptions. The taste threshold is in the region of 250 mg/litre depending on the associated anions. Sodium is essential for adequate functioning of human physiology although the requirement of infants for sodium is lower than for children and adults, and high sodium intake may lead to hypernatraemia. This is a problem for bottle-fed infants and is the reason why sodium levels in infant formulae have been reduced significantly over time. There have been concerns expressed about the importance of sodium intake for increasing hypertension across populations, A number of member states are concerned about overall intake of salt from all sources but particularly food, which is the major source of sodium intake, and are seeking to persuade their populations to decrease salt intake. On the other hand hyponatraemia can be a serious including fatal acute risk if significant perspiration causes high loss of sodium and there is inadequate sodium intake from the total diet. Seawater and brackish water also usually contain potassium, at significantly higher concentrations than fresh waters, which is removed in a broadly similar proportion to sodium during desalination. Potassium is an essential nutrient and the recommended daily dietary requirement is more than 3000 mg/day. There is currently no

specific guideline value for potassium; residual concentrations in final water will be well below any significant contribution to recommended daily dietary intakes.

Magnesium and calcium

Magnesium and calcium are essential nutrients and are present in sea waters at significant levels but not necessarily in brackish waters. They are efficiently removed by desalination but may be added back to finished water by some processes used to stabilize the water and reduce corrosivity. They will be discussed later in this chapter.

Organic chemicals found naturally in source waters

Naturally occurring chemicals will also include organic matter (NOM) such as humic and fulvic acids, and the by-products of algal and seaweed growth, where this growth occurs to a significant extent. Such chemicals can include substances that can impact on the odour of the final water such as geosmin from cyanobacteria, particularly in brackish water, and a range of toxins from a variety of different organisms including cyanobacteria and dinoflagellates, which can form significant blooms, although these are usually intermittent in nature. The only one of these potential contaminants for which there is currently a guideline value is the cyanotoxin Microcystin LR which arises from freshwater cyanobacteria blooms and for which WHO has set a provisional guideline value of 1.0 µg/litre (WHO, 2004). Work is underway to explore possible drinking water guidelines for other toxins of these types.

The nature of the natural organic molecules is such that most of them are sufficiently high molecular weights and/or low volatilities so they would not be expected to significantly carry over in thermal desalination processes although the potential for carry over by steam distillation remains uncertain. Volatile organics are usually vented as part of the distillation process. The carry over would be expected to be small but for substances such as geosmin, which has an odour threshold measured in ng/l, this could still be of concern for the potential acceptability of the final product. Most of the organic molecules are relatively large and would be expected to be excluded by membranes used in desalination, although more data are required concerning the potential for low MW polar compounds to cross the membrane. Solvent type low molecular weight neutral organics may pass through membranes to a significant degree. Two of the main marine toxins, saxitoxin and domoic acid have been shown to be rejected by membranes used in desalination (Voutchkov 2006 Personal Communication).

There is also a significant potential for anthropogenic contamination of source waters, particularly seawater and estuarine waters, as a consequence of discharges from sewage treatment and from industry. The contaminants present at a particular site will depend on both the industry and shipping activity present in the wastewater catchment or that discharges directly to sea and on the size of the population served. Many of the substances that can reach source waters are covered in the GDWQ and in the associated document, Chemical safety of drinking-water: Assessing priorities for risk management (WHO 2007). A number of potential contaminants such as pharmaceuticals and hormones reaching drinking water supplies from upstream wastewater discharges have attracted significant media attention, however, these have been largely shown not to cross the desalination membranes (McGuire, 2005). The great majority of these molecules would not be expected to be present in the distillate from thermal processes, but there is a potential issue regarding public perception. Providing reassurance of the

adequacy of the barriers to the consuming public would be an important step in a water safety plan. There is also a significant potential for contamination by petroleum hydrocarbons, particularly in regions where there is substantial activity in the extraction of oil. There is the possibility that more volatile substances may be carried over into product water in thermal distillation processes; these include the BTEX compounds (benzene, toluene, xylenes, ethylbenzene) and solvents such as carbon tetrachloride, tri and tetrachlorethene. Those processes are designed to vent those gases during processing but it is important to assure that those types of substances are being well removed. There may also be potential for these substances, if present in sufficient quantities, to dissolve in reverse osmosis membranes and thus appear in finished waters. Although there are drinking water guideline values for all of these substances, except for benzene which is a human carcinogen, the primary issue regarding the BTEX compounds is the potential for them to cause unacceptable taste and odour at concentrations much lower than the health-based guideline value (WHO, 2004). Prevention of source water contamination is the best method to prevent contamination of finished waters. The assessment of potential hazards and risks from pollutants will require an evaluation of the sources and types of pollutant in the local circumstance.

There have also been suggestions of contamination by metals, particularly mercury in regions of oil production, and there is a possible issue for distillation plants with the volatilisation potential for mercury if it is in the metallic form. Data on actual concentrations in feed waters are very limited; however, there is an existing GDWQ value for inorganic mercury of 6 µg/litre.

3.3 Pretreatment

Pre-treatment of the source after intake water is normally designed to remove contaminants that will interfere with the desalination process such as by scale formation or fouling membranes. This treatment can include coagulation and filtration, or microfiltration processes and other membranes which will remove particulate and organic matter, including significantly reducing NOM. The usual disinfectant is chlorine.

Humic and fulvic acids and other related substances that constitute NOM can react with chlorine (and other disinfectants) to produce a wide range of halogenated by-products. In the presence of high bromide, as found in seawater and many brackish waters, the bromide is oxidised to bromine or hypobromite, which will take part in the halogenation reactions and produce organobromine products. Data from studies on the chlorination of seawater show that the yield of disinfection by-products (DBPs) in the form of trihalomethanes (THMs) is dominated by the brominated THMs, particularly bromoform and to a lesser extent chlorodibromomethane. The WHO guideline values for these two substances are both 100 µg/litre while the guideline values for the other THMs are 200 µg/litre for chloroform and 60 µg/litre for bromodichloromethane. Numerous other organobromine and organochlorine compounds are also formed at low levels and there are studies underway that continue to identify more of them. There may also be small quantities of iodinated THMs present, but there are no guideline values for these substances and there is limited data on their presence in disinfected fresh waters (Plewa et al, 2004), and some on their occurrence in disinfected waters with high salt content (Richardson et al, 2003). The levels of other potential chlorination by-products, such

as the haloacetic acids will also be a function of the precursors. Again, either distillation or membranes will remove most of these disinfection by-products.

Organonitrogen compounds, particularly dimethylnitrosamine (NDMA) and other nitrosamines (NDEA) may be formed during chloramination, especially during distribution when the appropriate secondary amines are present in the source water or possibly in coagulants. There are limited but increasing data on the formation of these compounds in drinking water and there appear to be no data on the formation in seawater. There is also evidence of formation of nitrosamines in chlorinated wastewater, where there will also be ammonia present, and so where chlorinated sewage effluents are likely to impact the raw water there may be potential for these compounds to volatilise and be carried over into the product into the product, or to pass through membranes, although a reduction in the initial concentration would be apparent in both cases.

Where hypochlorite is produced by electrolytic generation from seawater/brine with a high bromide level, this will lead to the formation of bromate. Bromate is not likely to pass membranes and would not be expected to carry over in thermal systems, but studies should be conducted to assess these possibilities. Where hypochlorite is allowed to age there is also a potential for the formation and build up of chlorate. It should also be well removed by either distillation or membranes.

Theoretically a number of organic contaminants, both raw water contaminants and those resulting from disinfection, could transfer into the product as a consequence of steam distillation. There is a need to determine how important this is and under what circumstances it will take place.

Membranes provide a barrier to most chemical compounds, although not always a complete barrier. The propensity of boron (as borate or boric acid) and also arsenite to pass through membranes raises the question as to what other anions and small neutral organic molecules will pass through membranes. There is a need for more specific data from actual desalination facilities and for specific types of membranes.

An additional potential concern for which there appear to be no firm data is the use of hydrazine in power plants as an oxygen scavenger. Although hydrazine itself is no longer used, alternatives appear to break down to hydrazine. Where these compounds are used it is important that there be no potential to transfer, through steam leaks, into the desalination stream.

3.4 Chemicals from treatment processes

When cleaning agents for membranes are used, they are applied either on- or off-line and those chemicals can be present in the system at high concentrations. Therefore the membranes should be properly flushed before installation and before the system goes back on-line and the flushing solutions disposed of to waste. Pretreatment of the waste will be necessary and it is important that this waste stream is disposed of in such a way that it cannot contaminate either source waters or waters that might be used for subsequent blending with desalinated water.

Materials such as piping and contact surfaces in treatment systems and processes that come into contact with drinking water need to be assessed to ensure that no chemicals leach that

could cause the guideline values to be exceeded or introduce other substances that could be of hazard to health or adversely impact on the acceptability of the final water. Procedures to ensure that this is the case are an important component of the water safety plan.

3.5 Post-treatment

There are four primary issues concerning the post-treatment water. These relate to blending, remineralisation, disinfection and materials used for storage and transport of the water to the tap. Desalinated water is often blended with other sources that contribute minerals to the final blended water. Seawater as a source for blending has both advantages and disadvantages (see Chapter 4), particularly in terms of corrosion and taste if the blending levels exceed about 1%. In addition blending with seawater results in the addition of sodium and some potassium, calcium and magnesium to drinking-water. Consideration should be given to the natural minerals present and whether these will result in finished water not meeting the Guidelines or having unacceptable taste. There is also an issue regarding potential anthropogenic pollutants from a range of sources which need to be considered on a local basis, whenever any external and potentially minimally treated source is used, taking into account potential pollution sources and threats. Disinfection and possibly filtration of the blending water will be necessary if there is any possibility of microbiological contamination (see Chapter 4) , in which case similar considerations regarding the formation of by-products in the blending water apply as discussed under pre-treatment processes. There are currently WHO Guidelines for individual THMs and dibromoacetonitrile. Generally the NOM content in finished water is very low and the yield of by-products from final disinfection would be expected to be low as a consequence (McGuire Environmental, 2004).

3.5.1 Remineralization

In a number of cases, water is remineralised to reduce its potential for corrosion. Under these circumstances it is appropriate to consider whether the methods used, such as percolation through limestone, can also increase the concentrations of important nutritional minerals, particularly calcium and magnesium. WHO expert consultations on calcium and magnesium in drinking water (WHO, 2005a; WHO, 2006; Cotruvo, 2006) concluded that there was evidence of dietary deficiency of both calcium and magnesium in many parts of the world. This would be particularly acute in developing countries and in women, and also in some sectors of the population, such as the ageing who are also at highest risk of ischaemic heart and cerebrovascular disease. Hard water and particularly magnesium, a component of hardness, have been negatively (i.e. beneficially) associated with these conditions in a number of epidemiological studies. Although uncertainties about this association remain, in circumstances where a supply is moving from a source that has significant levels of calcium and magnesium to low mineral desalinated water it would be appropriate to consider remineralizing with calcium and magnesium salts. The science behind these findings is discussed in detail below. Currently the evidence supports the view that a magnesium concentration on the order of 10 mg/litre and a calcium concentration of 30 mg/litre would be appropriate for addition. However, any decision should be taken in conjunction with health and nutrition authorities in the light of dietary intakes of nutrient minerals. Blending with 1% seawater provides about 15 mg/litre of magnesium and about 5 mg/litre of calcium to the finished water. It is appropriate for WHO to continue to consider the importance of calcium and magnesium for protection against ischemic heart disease and to determine the optimum levels of calcium and magnesium and the importance of Ca/Mg

ratio, in order to provide guidance as to the required the optimum levels of addition, if appropriate. In particular, there are significant considerations with regard to both cost benefit in particular circumstances and public perception.

Low fluoride intake is also a potential consideration with regard to loss of fluoride from the bones. A recommendation of a WHO working group was for a minimum fluoride concentration of 0.2 mg/litre but this recommendation may require refinement and confirmation. The recommended GDWQ value fluoride is up to 1.5 mg/litre. This value provides a balance between allowing fluoridation of drinking-water and minimising the occurrence of dental fluorosis. However, use of the guideline value to develop local standards should take into account climate and water consumption, because the guideline value is associated with an intake of 2 litres of drinking water per day. It is, therefore necessary to set a lower standard where the water intake is above this as in areas of high ambient temperature. This is also a consideration with regard to artificial fluoridation used to protect against dental caries, where this is a significant problem or there is a significant risk that cannot be addressed through other means. (WHO, 2005a; WHO, 2006). Whether to add fluoride to finished water for dental health is a function of the status of tooth decay incidence in the location, diet (sugar consumption levels), and the ready availability and use of dental care in the area throughout the population. These can be determined by appropriate studies in the area.

With regard to sodium levels in the final water, this requires specific consideration of potentially sensitive populations, such as bottle-fed infants.

In addition other corrosion inhibiting chemicals, primarily silicates, orthophosphate or polyphosphate, may be added to the water. Such chemicals are widely used in many parts of the world and are not of direct consequence for health. However, it is important that they are of a suitable quality for addition to drinking water and that there are no contaminants of concern, particularly those covered in the GDWQ, that would make a significant contribution to the concentrations of such contaminants in drinking-water. It is also important that they are verified to be always of an appropriate quality. Approval systems for chemicals that specify the quality and acceptable levels of contaminants are available. Guidance on how such systems can and should operate is under consideration by WHO.

3.5.2 Calcium/Magnesium/Cardiovascular Disease/Osteoporosis

This issue was examined in detail in three scientific meetings that were generated by this desalination guidance development process. The first was an experts meeting assembled by the WHO in Rome in 2003. Their task was to examine potential health consequences of long term consumption of water that had been ‘manufactured’ or ‘modified’ to add or delete minerals. Specifically, this was applied to consumption of desalinated seawater and brackish water, as well as some membrane treated fresh waters, and their optimal reconstitution from the health perspective. The latter is economically important because desalinated waters require stabilization by some form of remineralization, often with calcium carbonate (lime) to control their corrosivity toward pipe and fixtures while in storage and transit to consumers. That group concluded among other things that the hypothesis that consumption of hard water is associated with a somewhat lowered risk of certain types of cardiovascular disease was probably valid (WHO, 2005a). It also concluded that only a few minerals in natural waters had sufficient

concentrations and distribution to expect that drinking water might sometimes be a significant supplement to dietary intake. These included calcium, magnesium, selenium, fluoride, copper and zinc. It recommended that a detailed state-of-the-art review should be conducted prior to consideration of the matter in WHO drinking water guidelines.

That report led to the Symposium entitled *Health Aspects of Calcium and Magnesium in Drinking Water* (Cotruvo, 2006), and a subsequent WHO Expert Meeting (WHO, 2006) on the subject. The Symposium presented information that large portions of the population are deficient in calcium and magnesium, and that water could be a source of significant incremental contributions of calcium and magnesium to the daily diet. For desalinated water, remineralization methods that include addition of calcium and magnesium are more desirable because they also contribute nutrient minerals. Seawater blending also adds back magnesium and calcium.

Finally, WHO organized a meeting of experts to further assess drinking water epidemiology, clinical and mechanistic studies that involved calcium or magnesium or hard water that contains calcium and sometimes magnesium. (WHO, 2006) A large number of studies have investigated the potential health effects of drinking-water *hardness*. Most of these have been *ecologic* studies and have found an inverse (beneficial) relationship between water hardness and cardiovascular mortality. The best correlations were usually with magnesium. Inherent weaknesses in the ecologic studies design limit the conclusions that can be drawn from ecologic studies. The several analytic *case-control* and *cohort studies* did show a negative (beneficial) association between cardiovascular mortality and drinking-water magnesium levels (but not hardness or calcium) in water. Effects at about 10 mg/litre were significant. Although this association does not necessarily demonstrate causality, it is consistent with the well known effects of magnesium on cardiovascular function, but further studies are necessary to further examine the effects of water composition. (WHO, 2006) Those *case-control* and *cohort* water epidemiology studies did not indicate evidence of an association between water hardness or calcium and acute myocardial infarction or deaths from cardiovascular disease (acute myocardial infarction, stroke and hypertension), or between drinking-water magnesium and acute myocardial infarction.

3.5.3 Dietary supplementation

The geographic distribution of the nutrients in source waters used for drinking water production will be varied and inconsistent so an appropriate diet should be the principal source. In general, drinking water should not be relied upon as a major contributor of significant trace nutrients to daily intake. However, drinking water can provide supplementation to dietary intakes in some locations. Dietary supplementation is, widely practiced for general benefit e.g., Vitamin D in milk, Vitamin C in drinks, iron and B Vitamins and folic acid in bread and other foods. The only therapeutic substances added to drinking water in some areas are fluoride with the intent of strengthening dental enamel and reducing the incidence of tooth decay (dental caries), and ferric iron/EDTA complex in some dietary iron deficient areas in South America, and possibly iodine in some areas in some high goiter incidence areas in Russia.. WHO states that there is clear evidence that long-term exposure to an optimal level of fluoride results in diminishing levels of caries in both child and adult populations, and that fluoride is being widely used on a global scale, with much benefit. (WHO, 2006a) Water fluoridation is controversial in some quarters but generally believed by the dental community and many public health officials

to be beneficial and without demonstrable risk. Water fluoridation is a matter of national policy. Seawater is naturally low in fluoride and the fluoride is further depleted by the desalination process. Optimal fluoridation of the desalinated water can be a significant contributor to daily intake and can reduce the incidence of dental caries just as it does with fluoridated freshwaters.

3.6 Distribution systems

Desalinated water is potentially more corrosive than many other drinking-water sources and it is important, as indicated above, that the water is stabilised to minimise corrosion of metallic pipes and fittings used in distribution and in buildings. Where distribution is through tankers then the potential for corrosion of the tankers must also be considered. The requirement is that corrosion should not give rise to levels of metals that exceed the guidelines or add unacceptable appearance or taste, or physically damage water contact surfaces. (McGuire/Malcolm Pirnie, 2006) These can include metals from primary distribution and storage, particularly iron and possibly nickel, and from plumbing and fittings in buildings, including lead and copper. Iron has, in the past given rise to problems with discoloured water that significantly reduces the acceptability of the water for both drinking and for household uses. In many cases a range of coatings and materials will be used to coat pipes or storage reservoirs, or for storage tanks in buildings in order to protect against corrosion. It is important that these materials are of a suitable quality for use with potable water and as indicated above approval schemes have an important part to play in ensuring their safety and reducing the potential impact on consumer acceptability. There is a particular consideration in the approval of materials since in many of these circumstances they will be used at elevated temperatures, which can exacerbate leaching of component metals.

3.7 Additional Issues

There have been suggestions that drinking very low mineral water can lead to a number of adverse effects on humans, particularly on the gastrointestinal tract, even with a diet that provides an adequate level of essential minerals (Kozisek, 2004). This is unresolved and there is a need to investigate this subject in order to determine if there is a significant issue that needs to be taken into account.

Desalination has been used in some parts of the world for many decades and this experience potentially provides a basis for epidemiological studies of various health outcomes. Such studies if properly controlled and with proper consideration of potentially confounding factors, would be of considerable value in assuring the safety of desalinated water.

3.8 Chemicals-Related Health Recommendations

- The WHO and Desalination Guidelines encourage governments to adopt existing systems or establish systems for specifying the appropriateness and quality of additives encountered in desalination, or to adopt existing credible recognized standards for those products that would be tailored to desalination conditions.
- WHO GDWQ are encouraged to reassess the toxicity of boron and to provide revised WHO recommended guideline values.
- WHO GDWQ are encouraged to develop a GDWQ for bromide for reference purposes due to its widespread presence in fresh waters and desalinated waters.

- There is need to consider sodium and other minerals in water in relation to bottled infants. WHO is encouraged to provide guidance as to the impact of higher sodium for infant formula.
- There should be a re-examination of the low dose carcinogenic risks of bromate in the GDWQ in light of new information and followed by possible modification of the guideline.
- Countries should carry out dietary and dental care studies, if necessary, to determine the possible and appropriate role of their water supplies including desalinated water as a contributor to total dietary intake requirements of fluoride and minerals.
- There is need to consider the importance of mineral balance in drinking water, particularly calcium and magnesium, with regard to risks of osteoporosis, and ischemic heart disease, respectively, as well as fluoride in relation to loss of fluoride from the skeleton.
- There is the need to examine in more detail the possibility of adverse effects arising from drinking ultra-low mineral water.

Disinfection by-products (DBPs) formation is an important quality issue in many projects. Desalinated water has low total organic carbon (TOC) so it should not in itself produce significant amounts of DBPs in finished water depending upon the type of post disinfection and the length and conditions of distribution.. However, some practices such as producing hypochlorite from electrolysis of seawater will produce significant amounts of bromate and also of organohalogenes, and probably particularly brominated organics to a greater degree than would occur in most conventional fresh water production. Post treatment blending can be a source of additional DBP precursors.

3.9 Chemicals research issues

- If hydrazine is shown to be a real problem, there should a determination of a guideline value and deferring to the WHO Chemicals Group.
- Document especially DBPs occurrence in desalination systems from seawater and brackish water. Attention should be given to systems that use blending.
- Determine the nature and quantities of organo-bromine disinfection by-products.
- Examine the issue of the potential of entrainment of high molecular weight compounds in steam in thermal systems, and on carry over of volatiles, and the performance of methods to reduce carryover. Membrane process performance for low molecular weight chemicals should also be quantified.
- Daily drinking water consumption should be examined and quantified in warm climates for use in improved risk and benefit assessments.
- There should be an assessment of the consequences of long-term consumption of desalinated water in areas with long term experience e.g. Gulf States.
- Consider in more detail the possibility of adverse effects arising from drinking ultra-low mineral water.
- Document process performance for removal of various contaminants in source water and added by treatment

- Safe management and disposal of desalination concentrates should be studied further and guidelines provided.

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Sanitary Microbiology of Production and Distribution of Desalinated Drinking-water

4.1 Sources and survival of pathogenic organisms

Survival of pathogens in the environment has been extensively studied. While some pathogenic organisms are able to persist in source water and finished drinking-water for days to months, they generally do not grow or proliferate in water (Wait and Sobsey, 2001; Tamburrini and Pozio, 1999; Fayer et al, 1998; Graczyk et al, 1999), with a few exceptions (e.g. *Legionella*, *Vibrio*, *Naegleria* and *Acanthamoeba*). Survival of these pathogens is strongly related to water temperature, solar radiation, osmotic pressure, and the abundance and activities of predators (i.e. protozoa). Increased water temperature results in an active development of the indigenous flora and fauna, which utilize many microorganisms including human pathogens as food sources, resulting in accelerated removal of pathogens in warmer waters compared to waters below 15°C. Sunlight (UV) has been identified as an important factor in the inactivation of pathogens (Fujioka and Yoneyama, 2002; Sinton et al, 1999). In addition, most human enteric bacteria also decay more rapidly in saline water than in freshwater due to the higher osmotic pressure (Nasser et al, 2003). Coastal currents and surface waves can transport pathogens over long distances (Kim et al, 2004; Reeves et al, 2004).

In addition to pathogens associated with anthropogenic sources, some indigenous marine bacteria such as those belonging to the *Vibrio* genus (*cholerae*, *varahaemolyticus*, *vulnificus*, *minicus*) and toxin-producing algae are potential sources of waterborne human health risk. Harmful algal blooms are sources of paralytic, neurotoxic, amnesic shellfish poisoning. Toxin-producing algal species include red tide organism *Karenia brevis* (previously named *Gymnodinium breve*) (producer of neurotoxic shellfish poisoning), *Alexandrium sp.* (producer of paralytic shellfish poisoning), *Pseudo-nitzschia* (producer of amnesic shellfish poisoning), *Pfiesteria piscicida*, brown tide organism (*Aureococcus* and *Aureoumbra*), and cyanobacteria (blue green algae). *Vibrio cholerae* can be found in waters that are contaminated by human excreta from populations where the infection is occurring and constitute a significant health risk in populations using these waters. Indigenous bacterial pathogens and toxin-producing algae display strong seasonal and temporal variability generally due to rapid multiplication when water is warming during spring and summer months and with the availability of additional nutrients. Temperature, salinity and nutrient sources will have effects on the occurrence of vibrios and algal blooms. (Jiang et al, 2000; Jiang and Lu, 2001; Louis et al, 2003) Blooms of toxin-producing algae can be triggered by coastal upwelling that brings in nutrient-rich deep water or by anthropogenic nutrients from waste discharge to coastal waters. (Li and Daler, 2004; Yang and Hodgkiss, 2004)

Ground waters are usually less subject to pathogen contamination due to the effect of soil infiltration. However, the efficiency of pathogen removal during infiltration is largely due to the characteristics of soil substrates. Paul et al (Paul et al, 2000; Paul et al, 1997; Paul et al 1995a; Paul et al, 1995b) have demonstrated that in the Florida Keys where porous limestone is the major composition of soil substrate, microbial tracers injected into the ground water injection

wells that were used for standard sewage disposal, migrate rapidly through ground aquifer and seep through the bottom of the seafloor to surrounding seawater. Human enteric viruses are found frequently in the canal and marine water around the Florida Keys due to seepage from septic tanks and ground water injection wells. (Griffini et al, 1999; Lipp et al, 2002)

4.2 Monitoring for pathogens and indicator organisms

Pathogen monitoring has been the subject of numerous discussions. The current consensus is that routine or occasional sampling of source waters for pathogens is not a very efficient approach for managing drinking water quality and treatment processes. The WHO Guidelines for Drinking-water Quality, 3rd (current) edition, including the first addendum (WHO, 2006) provide guidance and a framework for safe drinking-water through water safety plans that include monitoring for various parameters. In that framework, gathering knowledge and data on pathogens in the environment is an integral part of the process. As more emerging pathogens are identified (WHO, 2003; AWWA, 2006) data obtained by researchers provide useful information on various parameters that can be used as index, indicator or surrogates for waterborne pathogens. Routine monitoring of source water may be needed to understand the quality of the source water, for consideration in the desalination treatment process utilizing that source water, and for an integrated management approach to the watershed. Fortunately, desalination processes should be particularly effective at removing undesirable microorganisms of all types prior to their reaching finished drinking water. Indicator monitoring and pre-treatment would be a particular concern for blending waters that may not receive treatment. In addition, pathogen monitoring of watersheds is useful for research-driven ecological modelling initiatives. Routine pathogen monitoring is generally not justified and a good combination of microbial, indicator and non-microbial parameters is probably a more cost-effective monitoring solution. (Dufour et al, 2003)

4.3 Microbial considerations for desalination processes

The efficiency of desalination plants to remove or inactivate microbial contaminants can be assessed by examining the expected performance and factors affecting the quality of each flow that may be produced or combined into the final treated water. The potential for survival of microorganisms depends on the capabilities and operating conditions of the process units for their removal and/or inactivation. The issue of disinfection or elimination of micro-organisms of health concern can be evaluated for the water from the pretreatment, the water produced by membrane processes or the water resulting from thermal treatment processes, and especially for post-treatment blending waters.

4.3.1 Pretreatment

The specifics of pretreatment are usually determined by the type of down flow process used for the removal of dissolved solids. For example, membranes need to be protected from particulates to prevent clogging and fouling. The objective of pretreatment for microbials using oxidants and biocides is to prevent fouling of the RO membranes and does not specifically address

disinfection goals because oxidant doses applied are not sufficient to reach residual concentrations required for efficient disinfection.

Other pretreatments include use of membranes to prepare the water for the subsequent desalination process (Chapter 2). These pretreatment membranes include micro- and nanofiltration, and they have a substantial capacity to physically remove a substantial proportion of particulate-associated microorganisms (Chapters 1 and 2) as well as some dissolved solids. They can effectively remove up to 6 logs of microorganisms according their pore size distribution but the actual removal should be validated before application as a pretreatment. (Lechevallier and Kwok-Keung, 2004) If partial flow of these pretreated waters is used to blend with the final processed desalinated water, then an evaluation of the disinfection/removal requirements for this added flow must be completed in order to attain the same level of protection as the one attained by the treatment itself. Dilution only is unacceptable.

4.3.2 Blending source water with desalinated water

The quality of the blended water is particularly relevant if mixing of incompletely treated water with desalinated water occurs prior to distribution. This is of primary importance to the evaluation of the microbial risk of the blended water as well as to the consequences of the formation of disinfection by-products. The amount of blended water may vary from less than 1% to 10% and can include partially treated seawater and untreated groundwater. Short circuiting of the treatment process should not allow pathogens and other undesirable microorganisms to be mixed with the finished desalinated water. General guidelines for drinking water and guidelines specific to the minimization of microbial risks, should be used in the context of a complete system assessment to determine whether the drinking-water supply (from source through treatment to the point of consumption) as a whole can deliver water that meets the health-based targets (WHO, 2006; Lechevallier and Kwok-Keung, 2004). In addition, there should be specific regulations in each country specifying the minimum requirements for disinfection and particle removal. The required performance for the removal of bacteria, viruses and protozoan parasites should also be adjusted to the level of contamination of the raw water used for blending. In addition, if the blended water contains high TOC or bromide, then chemical disinfection by chlorine or ozone might not be advisable due to formation of undesirable by-products.

To evaluate the need for additional treatment of the blended water, general guidelines for drinking water and guidelines specific to the minimization of microbial risks, should be used in the context of a complete system assessment to determine whether the drinking-water supply (from source through treatment to the point of consumption) as a whole can deliver water that meets the health-based targets (LeChevallier and Au, 2004; WHO, 2004a; WHO, 2006). WHO and other organizations provide guidance and information on removals of bacteria, viruses and protozoa that are achieved by typical and enhanced water treatment processes. Table 4.1 provides an example of the performance of several common disinfectants to achieve various logs of inactivation of viruses in drinking water using CT (Concentration x Time) values as the measure and viruses as the challenge. (USEPA, 1999) These CT values are based upon water temperatures of 10°C and pH in the range of 6 to 9. CT values for chlorine are based upon a free chlorine residual, and chlorine is less effective as the pH increases from pH 6 to pH 9. At a given CT value a lower C (concentration) and longer T (contact time) are more effective than the reverse. For all of these disinfectants the effectiveness increases as the temperature increases.

CTs for vegetative bacteria would be less than for viruses, whereas CTs for protozoa (more resistant to disinfection) would be higher. Spores would be much more resistant than vegetative bacteria. Additional performance information is available for various treatment methods and conditions in USEPA 1999, AWWA 1991, and the WHO Guidelines for Drinking-water Quality, 3rd edition Table 7.6 at p. 138 to p. 141.

Table 4.1 CT Values for Inactivation of Viruses (mg-minutes/L)

Disinfectant	Inactivation		
	2 log	3 log	4 log
Chlorine ¹	3	4	6
Chloramine ²	643	1067	1491
Chlorine Dioxide ³	4.2	12.8	25.1

CT values from AWWA 1991

¹Based on temperature 10°C, pH range of 6 to 9, free chlorine residual of 0.2 to 0.5 mg/L

²Based on temperature 10°C, pH 8

³Based on temperature 10°C, pH range of 6 to 9

Table 4.2 provides an illustration of the temperature dependence of CT values for disinfection using viruses and chloramines as the example. Inactivation improves significantly with increasing temperature. Even so, chloramines are much less effective than chlorine or chlorine dioxide, but they have the benefit of being more persistent during storage and distribution.

Table 4.2 CT Values for Inactivation of Viruses (mg-minutes/L) using Chloramines

Temperature in °C	Inactivation		
	2 log	3 log	4 log
5	857	1423	1988
10	643	1067	1491
15	428	712	994
20	321	534	746
25	214	356	497

CT values from AWWA 1991

In addition, there could be specific regulations in each country specifying the minimum requirements for disinfection and particle removal. If the blended water contains high TOC or bromide, the potential for the formation of additional disinfection by-products (DBPs) such as bromate, organochlorinated and organobrominated by-products should be evaluated when selecting the best processes to achieve the performance target. Ozonation of seawater and post chlorination may produce significant amounts of DBPs.

4.4 Reverse osmosis (RO)

RO has been shown to remove bacteria and larger pathogens and, depending on the membrane applied, to remove all or a large fraction of viruses. Even if the primary application of RO membranes is desalination, RO and NF are increasingly applied to treat surface water with the objective of removing pesticides, precursors of disinfection by-products and pathogens (Gagliardo et al, 1997; Adham et al, 1998; van der Hoek et al, 2000). With the performance reported at bench and full-scale, high quality RO processes are good treatment barriers to pathogens if properly selected and maintained.

WHO provides guidance on target removals for bacteria, viruses and protozoa, removals that are achieved by typical and enhanced water treatment processes (WHO 2006: Table 7.6). Removal of viruses by RO membranes may vary significantly and is both a function of the membrane itself, as well as its condition and the integrity of the entire system including seals. Removals ranging from 2.7 to more than 6.8 logs depending on the type of RO membrane have been reported at bench scale using MS2 bacteriophage as the model virus and the authors suggested that the selection of membranes is an important factor of virus removal (Adham et al. 1998). Kitis et al (2002, 2003) reported removals of MS2 ranging from 5 logs for dual element unit to more than 6.8 logs for multistage unit. Pilot-scale studies were conducted to investigate the potential of integrated ultrafiltration and nanofiltration membrane systems for the removal of various microorganisms including viruses, protozoa (*Cryptosporidium* oocysts and *Giardia* cysts), bacterial spores (*Clostridium perfringens*) and bacteriophage (MS2 & PRD-1). Lovins et al (1999) observed that removals including those resulting from pretreatment ranged from 6.1 to 10.1 logs showing that membrane treatment exceeds microbial removal attained by other combinations of process units, such as coagulation, filtration and disinfection of surface water. Since microorganisms are frequently bound to particulates, some turbidity might actually improve the removals by membranes.

4.4.1 Integrity of the RO system

Although RO constitutes an excellent barrier to microorganisms, the maintenance of that barrier depends on the integrity of the system. Breaches of integrity in the membranes or the O-rings could lead to the passage of pathogens into the process water and must be monitored by integrity testing. Building on bench scale studies done by Colvin et al. (2000), Kitis et al (2002) critically compared three integrity testing methodologies at pilot scale. They investigated the ability of these tests: 1) to quantify virus removal (bacteriophage MS2) in single element and two-stage configurations, and 2) to determine the changes in virus removal capability when systems are subject to different types of membrane and gasket compromising and fouling. These authors conclude that the loss of membrane integrity decreased virus removal from 5.3 to 2.3 logs when

the compromised unit was placed in the lead position, and from 5.3 to 4.2 logs when the compromised unit was in the trailing position. Fouling appeared to limit the impact of imperfections by a combination of cake formation and pinhole filling. Cracking of the O-rings did not lead to significant decreases in the removals of MS2 or indicators and the location of the damage influences the extent of the small decrease in performance. They also concluded that Rhodamine-WT could be used as an indicator of virus removal but its feasibility at fullscale was questioned.

Effective methods to measure the integrity of RO membranes should be used to achieve target removals (WHO, 2006). Currently, the measurement of conductivity is utilized but its sensitivity limits its application to about 2 logs of removal. Online measurement of integrity using safe easily detected high molecular weight chemical such as Rhodamine WT and new developments in biomonitoring may eventually provide innovative tools to ensure adequate performance monitoring.

Bacteria have been found in permeate samples of nanofiltration and reverse osmosis effluent and they can proliferate in discharge lines. This does not mean that pathogens are not rejected but rather that sterile conditions cannot be maintained (Taylor et al, 1996). Since bacteria have been shown to traverse through membrane defects, membranes cannot be considered as completely effective for disinfection and are commonly succeeded by a disinfection step.

4.4.2 Fouling and biofouling

Since bacteria can traverse through membrane defects, passage as well as microbial growth (biofouling) may affect quality of the product. Of potential concern is the impact of biofilm growth on membranes and the potential for retaining pathogens and growth of bacterial pathogens. Biofilms can impact membrane integrity directly (negatively) or by plugging holes and imperfections (positively).

Fouling of membranes is the progressive accumulation of material on the membrane surface or in its pores. The influence of the quality of feed water on fouling, notably the characteristics and composition of natural organic matter (NOM), the pre-treatment applied, the types of coagulants and the membrane characteristics, have been studied intensively. (Lahoussine-Turcaud et al, 1992; Ridgway and Flehming, 1996; Cho et al, 2000; Carroll et al, 2000; Fan et al., 2001; Fonseca et al, 2003; Gabelich et al, 2003)

Biofouling occurs when microorganisms accumulate and/or grow on the membrane surface, resulting in a premature decrease of flux through the membrane and/or increase in pressure drops. According to Flemming et al. (1997) practically every membrane system operating with water supports biofilms but not all systems experience operational problems because of excessive biofilm formation. Fifty-eight out of 70 RO plants in the U.S. reported biofouling problems (Paul, 1991). In a survey of NF and RO treatment plants in Holland, Vrouwenvelder and van der Kooij (2001) observed biofouling problems in 12 of the 13 plants studied.

There are several reasons why it is important for drinking water suppliers to avoid growth in distribution systems, including regulatory requirements, aesthetic and organoleptic acceptability, and the difficulty in maintaining a residual disinfectant. (Prévost et al, 2005) Regulatory issues associated with bacterial growth include: interference between the high abundance of background heterotrophic bacteria, and coliform detection when lactose-based growth media are used, violation of heterotrophic plate count regulations in some countries, and violation of coliform rules. The development of HPCs during distribution is no longer considered a significant health risk *per se* but its value as a water quality indicator of water quality and treatment has been reiterated (WHO, 2003).

4.5 Organic matter and growth of microorganisms in desalinated water

Desalinated water typically has low or very low organic carbon concentrations (TOC), and most likely very low biodegradable organic carbon (BOM) concentrations that can be partially or almost completely removed by RO. NF and RO appear to be the most efficient processes available for the removal of BOM at this time. Laurent et al. (Laurent et al, 2005) provide a summary of DOC and BOM removals by RO. Even if RO has excellent potential for the complete removal of BOM, the documented removals by full scale RO membranes are rare. (Escobar et al, 2000) Hong et al. (2005) report that assimilable organic carbon (AOC) removals by a hybrid NF-RO system demonstrate as expected that low levels of low molecular weight AOC pass through. Although not reporting actual levels of BOM, MacAree et al. (2005) report bulk water densities in HPCs (<6 CFU/mL) and total direct counts by epifluorescence microscopy (<6000 cells/mL) typical of starved systems.

The impact of biodegradable organic matter (BOM) on the potential for the establishment and subsequent development of opportunistic and frank pathogens in biofilms fixed on RO membranes has not been quantified directly. However some information is available on the colonization and survival of pathogens on filter media, activated carbon fines, pipe surfaces, POE, POU, softening systems, cooling towers and air conditioning systems. Overall, indications are that non-parasitic pathogens are not competitive in establishing and developing in mixed heterotrophic indigenous biofilms with the noted exception of *Legionella* as the presence of microbial contaminants in RO treated water would be mostly related to breakthrough rather than to multiplication/colonization in the system itself (Laurent et al, 2005). Furthermore, occurrence in the distribution system could also be due to ingress of contaminated water (Ainsworth 2004).

The passage of bacterial pathogens from the biofilm or the pretreated water depends on the availability of orifices in the membranes and O-rings. These issues do not differ from the general issues of membrane integrity that must be addressed to prevent the passage of pathogens in the bulk liquid. Some bacteria have been shown to survive the RO membrane process and to be carried throughout the distribution system. Identified species include capsulated bacteria such as *Novosphingobium capsulatum* (MacAree, 2005).

4.6 Thermal processes

When thermal processes are used for desalination, microbial inactivation will be controlled by the temperature attained and the time the water remains at that temperature. Typical temperatures

and temperatures to ensure the inactivation of vegetative cells by humid heat vary from 50° to 60°C when maintained for 5-30 minutes to achieve pasteurization. Spores, endospores and other resistant forms are more resistant to heat and require higher temperatures (70-100°C) held for longer periods of time. Most vegetative pathogens are inactivated under flash pasteurization conditions (temperature of 72°C for 15 seconds). The condensate is unlikely to contain pathogens after the distillation process because of the killing impact of heat and because pathogens are unlikely to be entrained. However, reduced pressures are used in some desalination processes to reduce the boiling point and reduce energy demand. Temperatures as low as 50°C may be utilized (USBR, 2003) and might not achieve the required inactivation targets. Inactivation levels expected at temperatures typical of distillation processes are considered sufficient to inactivate most pathogens since they are equivalent or in excess to those used for pasteurization.

4.7 Disinfection of desalinated waters

Desalinated waters constitute a relatively easy disinfection challenge because of their low TOC and particle content, low microbial loads and minimal oxidant demand after desalination treatments. Turbidity is not likely to affect chemical disinfectant performance by since turbidity values of desalinated water are relatively low. Posttreatment (e.g. lime) can cause an increase of inorganic turbidity that would not interfere with disinfection. The target levels of inactivation for pathogens remaining in desalinated waters can readily be achieved by appropriate disinfection processes, discussed elsewhere (WHO, 2004). Once the target levels of disinfection have been achieved and as part of a water safety plan, an appropriate level of chlorine-based residual disinfectant should be maintained during distribution .

Issues to be considered as specific to the disinfection of desalinated water are:

- The potential passage of virus through some RO membranes which brings the point of adequate virus inactivation requirements downstream of RO;
- The potential loss of integrity of membranes that could lead to the passage of various pathogens in process water;
- The practice of blending non-desalinated water to remineralise the treated water that raises the need to define appropriate targets for treatment and disinfection of the water used for blending.

Except for blending water which should usually be treated, these issues can be addressed in most cases by applying effective post desalination disinfection using chlorine-based or alternative disinfection processes (UV, ozone, etc.) as an additional barrier in a risk reduction water safety plan approach (WHO, 2006).

4.8 Storage and distribution of processed water

The challenge of maintaining water quality during storage and distribution is not specific to desalinated water. Microorganisms will grow during distribution especially in the absence of an effective residual disinfectant and at the high water temperatures often encountered in countries using desalination.(Block 1992) A broad spectrum of microbial species, such as *Legionella*, *Aeromonas* and *Pseudomonas*, *Burkholderia pseudomallei* and atypical mycobacteria some of

which include opportunistic pathogen strains can be present in distributed waters. The routes of transmission of these bacteria include inhalation and contact (bathing), with infections occurring in the respiratory tract, in skin lesions or in the brain. (Craun and Calderon, 2001) There is no evidence of an association of any of these organisms with gastrointestinal infection through ingestion of drinking water (Ainsworth, 2004) but *Legionella* can grow to significant numbers at temperatures of 25°C to 50°C. Water temperature is an important element of the control strategies. Wherever possible, water temperatures should be kept outside the range of 25–50°C. In hot water systems, storage should be maintained above 55°C, and similar temperatures throughout associated pipework will prevent growth of the organism. However, maintaining temperatures of hot water above 50°C may represent a scalding risk (WPC/WHO 2006). Where temperatures in hot or cold water distribution systems cannot be maintained outside the range of 25–50°C, greater attention to disinfection and strategies aimed at limiting development of biofilms are required. Accumulation of sludge, scale, rust, algae or slime deposits in water distribution systems supports the growth of *Legionella* spp., as does stagnant water (Lin et al. 1998). Systems that are kept clean and flowing are less likely to support excess growth of *Legionella* spp. Care should also be taken to select plumbing materials that do not support microbial growth and the development of biofilms. The WHO guidelines (2006) section 11.1.9 *Legionella*) provides more information on the subject.

The maintenance of water quality during storage and distribution depends on a number of factors including:

- The amount of biodegradable organic matter available and trace nutrients to support the growth of suspended and fixed bacteria.
- The chemical balance to limit the release of iron, lead and copper.
- The maintenance of an oxidant residual.
- The availability and nature of attachment surfaces, in particular the pipe and reservoir surfaces and the presence of corrosion.
- The maintenance of integrity in the pipes and reservoirs.
- The growth conditions such as residence time, hydraulic conditions and temperature.

WHO guidelines of Safe Piped Water set a risk reduction framework to limit the health risk associated with the distribution of piped water (Ainsworth, 2004), and these guidelines also apply to desalinated water. Those water quality concerns should be considered in light of the potential for microbial regrowth, disinfection by-product formation and the control of pipe corrosion.

High water temperatures will limit the maintenance of an effective residual throughout the distribution system due to the increased chemical reactivity of the disinfectant. The use of chloramines constitutes an advantageous alternative to free chlorine in distribution systems with long residence times and elevated temperatures. However, nitrification can occur from chloramines when *Nitrosomonas* bacteria are present.

4.9 Issues with blending product water with other sources

Blending of the desalinated water with groundwater or other sources of potable water may be utilized. This practice does not raise any special issues for desalinated water with the exception that special care should be taken regarding the chemical stability of water to prevent the release of iron, lead and copper. Taylor and al. (2006) provide an excellent review of issues to take into consideration and results from an extensive pilot study of the impact of blending RO treated water with potable water from groundwater and surface water in various pipe material. Of special relevance is the maintenance of conditions to minimize iron, lead and copper release (selection of disinfectant and dosage adjustment), and the control of nitrification when chloramines are used as the secondary disinfectant.

4.10 Recommendations

As with all drinking water supplies, desalinated drinking water production should strive to utilize the best available source water. The desalination plants should be located away from sewage outfalls, storm drains, and areas with recurring harmful algal blooms. The level of impact from sewage discharge will depend on the local conditions but special attention should be given to the location of water intakes and wastewater outfalls, especially if costing is considered. Suitable monitoring of biological and physiochemical parameters of source water during plant operation will ensure that the treatment processes are not overcome by high levels of pollutants.

Monitoring of source water quality for pathogens in a desalination process is not an effective operational approach due to issues similar to those encountered for monitoring of freshwater source. However, it is useful to provide baseline information that is capable of indicating significant changes of water quality to ensure treatment efficiency. This baseline information includes various biological and physiochemical parameters that are described in Table 5.1 in Chapter 5. Information on potential risks to human health can be obtained through use of indicators of faecal pollution such as *E. coli* and enterococci, which are suggestive of the presence of pathogens. Furthermore, since enterococci bacteria are more resistant to environmental degradation conditions in the marine environment than are *E. coli* (WHO, 2003), they are likely to be a better indicator of faecal pollution in seawater and the presence of enteric pathogens. Coliphages, which are viruses that infect coliform bacteria and are similar to human viruses in respect to survival and decay in seawater, have also been suggested as useful indicators of source quality as well as treatment process performance. Heterotrophic Plate Counts (HPC) are not an independent indicator of faecal pollution, yet they may be used as a baseline parameter to understand microbial community changes. Development and proper applications of analytical methods better adapted to saline water are needed to improve the monitoring of saline source waters. Some specific recommendations include:

- Maintain final disinfection after desalination to ensure the inactivation of bacteria and viruses and maintenance of a residual during storage and distribution.
- Water used for blending should be treated to reach microbial quality goals set on the basis of raw water contamination and risk reduction. Contaminated water should not be blended with desalinated process water.

- Treatment should be designed to ensure the presence of multiple barriers including a final disinfection barrier.
- Maintenance of water quality during storage and distribution including the presence of a disinfectant residual is important to ensure that product water quality is maintained to the consumer.
- WHO guidelines applicable to storage and distribution systems should be applied to minimize growth and recontamination.
- Desalinated water is very low in nutrients and possesses a low microbial growth potential. However, high temperatures (30 to 45°C) that are frequent in some countries using desalination may enhance growth of pathogens such as *Legionella*, and nitrification when chloramines are used.

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Monitoring, Surveillance and Regulation

The most effective means of ensuring drinking water safety is through the application of a comprehensive risk assessment and risk management approach. In the WHO *Guidelines for Drinking-water Quality* (2004) this approach is based on application of water safety plans (WSPs) within a Framework for Safe Drinking-water (Framework). The Framework includes:

- health-based targets which provide the “benchmarks” for water suppliers;
- the three components of WSPs
 - system assessment
 - operational monitoring and
 - management planswhich in combination describe the actions undertaken by water suppliers to ensure that safety, as defined by health-based targets, is achieved; and
- independent surveillance to assess the effectiveness of WSPs in meeting the targets

Monitoring plays a key role in ensuring that WSPs function as intended and achieve the provision of safe drinking water. It includes validation, operational monitoring, verification and surveillance. Validation is the process of obtaining evidence that control measures and the WSP as a whole are capable of achieving health-based targets, operational monitoring is used to determine that individual components of a drinking water system are working as intended, verification provides assurance that a system as a whole is providing safe water while surveillance reviews compliance with identified guidelines standards and regulations.

5.1 Validation

Validation of control measures including treatment processes is necessary to demonstrate that they are capable of operating as required. It is an investigative activity undertaken when a system is designed and constructed or modified. Validation should assess performance specifications for each control measure taking into account source water characteristics. The first step of validation is to consider existing data available from scientific literature, industry bodies, other users of the equipment and manufacturers or suppliers. As identified in Chapter 2 a body of evidence is available on the performance of a range of standard processes used to desalinate water. Validation should confirm that specific pieces of equipment achieve accepted performance standards. Monitoring associated with validation is normally an intensive activity undertaken typically in pilot trials or precommissioning and commissioning of systems. Monitoring requirements will generally be more extensive for non-standard or innovative processes. Validation can assist in identifying operating modes, operational monitoring parameters and criteria as well as maintenance requirements.

5.1.1 Operational monitoring

Operational monitoring is the planned series of observations or measurements undertaken to assess the ongoing performance of individual control measures in preventing, eliminating or reducing hazards. Operational monitoring will normally be based on simple and rapid procedures

such as measurement of turbidity and chlorine residuals or inspection of distribution system integrity.

Parameters used for operational monitoring should:

- be readily measured;
- reflect the effectiveness of each control measure;
- provide a timely indication of effectiveness based on compliance with operational limits; and
- provide opportunity for implementation of corrective measures where required.

Operational limits separate acceptable from unacceptable performance of control measures. If unacceptable performance is detected then predetermined corrective actions need to be applied. The aim is that measurement of operational parameters and implementation of any required corrective action should be undertaken within a time frame that prevents unsafe water from being supplied to consumers. In some cases operational target criteria that are more stringent than operational limits can be used to provide early warnings to operators to enable changes to be implemented prior to limits being reached or exceeded.

5.1.2 Verification

In addition to operational monitoring of individual components of a drinking water system it is necessary to undertake verification to provide assurance that the system as a whole is operating safely. The range of parameters included in verification will be directed by established drinking water standards and guidelines and will typically include testing for indicators of microbial quality as well as chemical hazards. Verification can be undertaken by the water supplier as part of quality control, by an independent surveillance agency or by a combination of these two.

5.1.3 Surveillance

Surveillance is the “continuous and vigilant public health assessment and review of the safety and acceptability of drinking water supplies.”(WHO 1976) Surveillance should be undertaken by an independent agency that is provided with legislative powers to support its activities and enforcement of any corrective actions required to protect public health.

There are two approaches to surveillance: approaches based on direct assessment and auditing. In the audit based approach, testing of drinking water quality, as supplied to consumers, is undertaken by the water supplier with assessment of monitoring programmes and results included in the auditing process. In the direct assessment approach, independent testing of water quality is undertaken by the surveillance agency. This type of testing complements the verification programme undertaken by the supplier. Surveillance will normally also include processes for approval and review of WSPs as well as a review of the implementation of plans.

5.2 Operational monitoring for desalination

Hazards can occur at any step from the source of seawater or brackish water to the final supply of drinking water. Control measures are used to prevent, eliminate or reduce these hazards and can include actions such as the protection of source waters from contamination by sewage or industrial wastes, treatment and protection of distribution systems. Chapter 2 provides a

discussion of typical technologies and control measures that can be applied to produce safe drinking water through desalination. The combination of control measures used in particular schemes will vary depending on a range of factors including the type of source water and size of the scheme. Irrespective of the combination of control measures used in a scheme effectiveness of performance of each measure needs to be assessed. This achieved by operational monitoring.

Operational monitoring can be applied to each of the components described in Figure 2.1:

- source water taking into account potential impacts of contamination sources and fluctuations caused by natural events;
- pretreatment including the use of additives and chemicals;
- desalination (membrane-based and thermal processes);
- blending (including treatment of blending water), remineralisation and disinfection; and
- storage and distribution including assessment of corrosion and stability of product/blended water.

Ensuring consistent drinking water quality requires care and attention to details in the day to day operation of all process within a desalination system from source to consumer. Such details should be reflected in the operational management of the desalination facility. This should be manifested in an accurate and up to date operations plan and should be documented and supported by appropriate training for plant operators.

Table 5.1 provides a summary of operational monitoring parameters with suggested monitoring frequencies for large (>10 MGD, ~37850 m³/day) and small plants (<1MGD ~ 3785 m³/ per day). Where resources are limited the selection of operational parameters and frequencies should be guided by a risk assessment. Using this approach monitoring of hazards and control measures can be prioritized on the basis of the level of risk associated with the hazard or with the loss of effective performance of the control measure(s) designed to reduce or remove the hazard. The frequency of testing should also be based on the level of risk in conjunction with a consideration of variability in the presence of the hazard or in the performance of the control measure.

5.3 Source water

Desalination plants can treat seawater (from offshore intakes and pipelines or from wells located on the seabed, beach or inland in coastal areas and on islands) and brackish surface water or groundwater. As indicated in Chapter 2 desalination facilities require reliable sources of water with a reasonably consistent quality. The quality and consistent nature of intake water will influence the nature and effectiveness of pre-treatment processes, the performance of treatment processes and the safety of drinking water produced by desalination. Quality is affected by naturally occurring elements, by events such as storms and spills and ongoing sources of contamination. Wherever possible a preventive approach should be applied to ensure quality of source water and a priority should be given to control measures designed to protect source waters and intake pipes. The less desirable alternative is to design treatment processes to remove preventable contaminants. In this case poor performance or short-term failure of downstream treatment processes can have greater consequences. In addition the presence of contaminants may be hazardous if source water is used in blending processes.

5.3.1 Marine waters

Potential impacts on water quality and desalination plant intakes can include:

- domestic wastewater discharged raw or partially treated
 - predominantly microbial pathogens and some persistent chemicals;
- onshore and offshore dumping of hazardous wastes
 - chemicals, pathogens and radioactive materials;
- offshore and near shore oil and gas exploration, excavation, production and refining processes
 - drilling mud turbidity, chemicals including hydrocarbons, small doses of radioactive nuclides;
- brine and other waste streams from desalination plants
 - chemicals including antiscalants, antifoaming agents;
- transport cargo including oil tankers and tourist vessels
 - ballast water, hydrocarbon spills, wastewater containing microbial pathogens;
- discharges from industrial complexes
 - chemicals including hydrocarbons and heavy metal-organic compound complexes;
- effluents from power generation plants including cooling waters
 - antifouling agents, biocides and thermal pollution;
- military actions where oil spills, chemical, biological and possible radioactive pollutants are produced accidentally or intentionally
- eutrophication associated with discharge of nutrient rich storm waters;
- increased organic loadings associated with fish kills or decomposing marine life and
- trapping and blockage of intake screens by aquatic organisms or passage of organisms through screens and into process equipment. Organisms such as mussels, clams and molluscs can grow in intake structures while microorganisms can attach and grow, producing biofilms.

5.3.2 Brackish surface or groundwaters

Brackish water can be withdrawn from surface sources such as lakes, estuaries, or from aquifers. Open lakes and estuaries can be subject to similar sources of pollution to seawater. Groundwater particularly when taken from deep or confined aquifers is generally more consistent in quality and contains lower levels of contamination than surface water due to the filtering effects of soil barriers. However, contamination of groundwater can occur and is of growing concern. Sources can include:

- domestic wastewater discharged raw or partially treated
 - predominantly microbial pathogens as well as detergents, household cleaning and disinfecting chemicals;
- industrial discharges
 - chemicals including hydrocarbons
- hazardous waste dumps
 - chemicals
- soluble fertilizers and pesticides from agriculture

- oil exploration activities, oil industry products, wastes and heavy petroleum oil derivatives

5.3.3 Operational monitoring parameters

Operational monitoring will be influenced by investigations and knowledge of source water characteristics, potential sources of contamination and the location of feed water intakes in relation to these sources. Investigations undertaken as part of intensive precommissioning surveys or following commissioning will determine the range of parameters and sampling frequencies included in operational monitoring programs. All monitoring needs to have a purpose and to incorporate mechanisms for interpretation and action. Operational limits should be established for parameters selected for monitoring. If these limits are exceeded causes should be investigated and remedial action initiated. Wherever possible remedial measures should be identified and documented prior to limits being exceeded.

Enterococci and/or *E.coli* can be used as indicators of bacteria from sewage contamination while chemical parameters can include ammonia (sewage contamination), oil hydrocarbons including volatile compounds and greases, industrial chemicals (parameters industry dependent) and radioactivity. Total organic carbon (TOC) could be used as a general indicator of contamination by organics or sewage with changes in concentration leading to investigations of potential causes.

Storm events can lead to deterioration in water quality. Impacts of storm events can be assessed by monitoring turbidity and if operational limits are exceeded one option can be to shut down intakes until turbidities fall to normal levels.

Microalgal blooms may also be a cause of increased turbidity or a source of algal toxins. In surface waters prone to blooms; algal species, including dinoflagellates and cyanobacteria, or chlorophyll should be monitored. Other organisms including seaweeds could cause blockages of intake structures and may also need to be monitored. The occurrence or abundance of organisms may be seasonal and monitoring programs should reflect this possibility. Impacts of organisms on intake structures including blockage of screens and growth within intake pipes should be monitored. Biofilms and biofouling of intake structures may be controlled using disinfectants as part of pre-treatment processes.

Depending on source water characteristics there are a range of parameters that can have potential downstream impacts on treatment processes and hence influence pre-treatment requirements. These parameters should be assessed and considered for inclusion in monitoring programs. Parameters could include:

- heavy metals
- low solubility chemicals such as CaCO_3 , CaSO_4 , CaF_2 , BaSO_4 , SrSO_4 , $\text{Mg}(\text{OH})_2$
- turbidity, alkalinity and pH
- silica
- hydrogen sulphide and metal sulphides (particularly in groundwater)
- boron and bromide (particularly in seawater)
- iron, manganese and alumina (in groundwater)
- total dissolved solids (TDS)

- disinfectants and other treatment chemicals in cooling water discharges from power plants

Temperature and pH should be monitored due to impacts on pre-treatment and treatment processes. Temperature of groundwater remains relatively constant but surface water temperatures can vary widely even within the same day and should be monitored more frequently. Measurement of pH and alkalinity is important in relation to control of corrosion and efficiency of coagulation process used as pre-treatment for membrane-based processes.

5.4 Pretreatment

Pretreatment can incorporate the addition of chemicals. Tables 2.1 and 2.2 present typical chemicals used in pre-treatment before thermal and membrane processes. Chemicals can be used to facilitate performance of pre-treatment processes or as cleaning agents. In addition to ensuring that additives and chemicals produce the required result, care also needs to be taken to ensure that they are of sufficient quality, do not contain undesirable contaminants and are not toxic. Quality control of chemicals is discussed in Section 5.11.

5.4.1 Membrane processes

Scaling, precipitation and fouling

Pre-treatment is a requirement for membrane based processes to reduce scaling, precipitation and fouling. The main causes are:

- particulates and suspended solids
- the presence of low solubility salts such as CaCO_3 , CaSO_4 , CaF_2 , BaSO_4 , SrSO_4 , $\text{Mg}(\text{OH})_2$
- organic foulants (oil and grease, hydrocarbons)
- colloidal silica and sulfur,
- metal oxides (iron, manganese and alumina),
- overfeed of antiscalants
- biofouling caused by biological growths

One aim of pretreatment is to remove suspended solids and turbidity in order to achieve a required silt density index (SDI) value. Coagulation (with pH adjustment) and filtration is the most common form of pre-treatment used for seawater while for brackish water, pre-treatment may also include settling and softening. Desalination feed water should have a turbidity below 1 NTU and an SDI below 5 to ensure reliable performance. Turbidity (or alternatively particle counts) can be monitored on-line. SDI can be determined on-site with the frequency of monitoring depending on variability and system characteristics. A second aim is to reduce downstream impacts on treatment processes such as scaling precipitation and fouling. Scale inhibitors (antiscalants) are used to reduce the impacts of low solubility salts or specific chemicals such as silica while disinfectants are used to reduce the likelihood of biofouling.

Membranes can be damaged by oxidizing agents like free chlorine and this needs to be removed from feed water flows. De-chlorination is generally achieved using sodium bi-sulphite. The performance of chlorination and dechlorination processes can be measured on-line using residual analysers or alternatively ORP (oxidation-reduction potential or redox potential) monitors. In addition dosing should be controlled by monitoring injection rates and levels in

chemical tanks. Quantities of chemicals used and average dose rates should be checked and recorded on a routine basis by plant operators.

5.4.2 Thermal processes - multiple stage flash distillation (MSF) and multiple effect distillation (MED).

Thermal processes generally require less pretreatment than membrane based processes. The primary issues are biofouling of intake pipes, corrosion and scaling. Corrosion and scaling can be minimized by a combination of pre-treatment and design features of the downstream process. Corrosion is primarily caused by dissolved gases and physical de-aeration is needed for MSF plants to remove oxygen. In MED plants, de-aeration takes place in the spraying nozzles. Scaling can be caused by the precipitation of calcium sulphate, calcium carbonate or magnesium hydroxide. Scale inhibitors can be added during pre-treatment or alternatively acid can be used to lower pH and prevent the production of scale. Due to the improvement of antiscalant products, acid treatment is generally not required for sea water desalination and is only used in special cases (brackish waters or waste waters with high concentrations of carbonic species).

Biological growth can occur in feed water intakes and supply lines. Chlorination can control this growth. Free chlorine concentrations should be maintained at about 0.1 mg/L. Periodic shock injections at higher doses may also be required depending on source water characteristics.

In addition to antiscalants and disinfectants, antifoaming agents are used in thermal processes to disperse foam-causing organics and to reduce surface tension at the steam/water interface. If scale inhibitors, disinfectants or antifoaming agents are used the quality of chemicals need to be carefully checked before use. In addition dosing should be controlled by monitoring injection rates and levels in chemical feed tanks. Quantities of chemicals used and average dose rates should be measured and recorded on a routine basis by plant operators.

5.5 Treatment

5.5.1 Membrane processes

The effectiveness of membrane processes can be assessed by on-line monitoring of trans-membrane pressures and longitudinal pressure drops and differential pressures (dP). In addition, conductivities and flow rates of permeate and concentrate streams should be monitored and used to determine recovery ratios and chemical balances. Scaling, precipitation and fouling due to inadequate pre-treatment can cause a gradual decline of longitudinal dP (differential pressures), trans-membrane pressure or permeate flux and an increase in salt permeation with time. These consequences can be detected by operational monitoring of membrane treatment processes. Changes in conductivity/TDS ratios in membrane product water can also be an indicator of scaling, precipitation and fouling.

Monitoring membrane pressures and permeate conductivities should give an indication of membrane integrity but minor damage allowing for passage of microbial contaminants may not be detected. The sensitivity of conductivity measurement is limited. TOC monitoring has been suggested as an alternative particularly where source water contains elevated levels of microbial

contamination. However, there are also questions about the sensitivity of this parameter and further research is required to identify sensitive integrity testing procedures.

Temperatures should also be included in operational monitoring plans. A temperature probe could be installed prior to the membranes. High temperatures may decrease the energy requirement of the RO unit, and improve water fluxes but accelerate increase of the salt passage index over time.

5.5.2 Thermal processes

The choice of the top brine temperature (TBT) is a key design feature of thermal processes and it should be continuously monitored. Corrective action and possibly shut-down of the plant should occur if the TBT exceeds a predetermined target value. Calcium sulphate and calcium carbonate scaling can be controlled through operating thermal processes at controlled temperatures. This is achieved at the design stage by the choice of the top brine temperature and of other parameters such as concentration of brine. For example, the maximum TBT of a MSF plant should not be above 112°C, while the maximum for a MED plant should be limited to 65°C.

- Corrosion is also influenced by operating temperatures (formation of carbon dioxide).
- TDS can be continuously monitored using conductivity meters. When concentrations exceed target criteria distillate should be rejected. Should the distillate conductivity become high the cause should be investigated e.g. leakage of a tube or displacement of a demister.
- Distillate and make-up flow rates should also be monitored on-line. If the make-up flow rate falls below a given value, corrective action should be taken and possibly the plant should be shut down.
- Systems are manufactured from a range of materials including steel and alloys of copper and nickel. Copper, iron and nickel can be measured in distillate to assess corrosion and equipment longevity.

In some MED processes incorporating a thermocompressor device (MED-TC) steam condensate may mix with distillate. In this case boiler treatment chemicals including hydrazine, carbohydrazide and other oxygen scavengers (used for treatment of high pressure boilers in power plants) could be carried over into distillate. Ideally this issue should be dealt with in the design stage. However, monitoring may need to be considered.

5.6 Blending and remineralisation

Blending is undertaken to stabilise desalinated water, reduce corrosiveness and improve the taste and acceptability of water supplied to consumers. There are two types of approaches that are taken to achieve these aims, blending with higher salinity water or remineralisation through the addition of chemicals. Blending requires the proper design of mixing facilities to overcome differences in the physical properties of the fluids being blended. Adequate energy must be supplied to overcome density differences in the two fluids and provide dispersion of the fluid

elements from the different streams to produce a homogenous mixture. The blended product should be reliably produced and especially be of a consistent and safe microbiological quality.

The choice of blending water is important from both a chemical and microbiological perspective. From a chemical standpoint, the blending water should produce a product that is stable and will not act aggressively towards the distribution system. Well operated membrane-based and thermal distillation processes should provide desalinated water that is free from pathogens. Blending waters should be of a similar quality. For this reason blending should generally be achieved using pre-treated source water. Alternatives are protected groundwater or treated surface water. As discussed in Chapter 4 treatment of blending waters will generally be required unless it is microbiologically safe (e.g. protected groundwater).

When blending waters of disparate quality, potential chemical reactions and chemical solubility issues should be considered. For example, if blending leads to calcium carbonate scaling there could be adverse impacts on blending performance, leading to fluctuations in product water quality. Scaling can foul static mixing blades causing short-circuiting in the blending unit leading to pockets of highly saline water in the product. The potential for such problems occurring can be assessed by operational monitoring for indices such as the langelier saturation index (LSI), the calcium carbonate precipitation potential (CCPP) or the Larson Ratio as discussed in Chapter 2 and through periodic inspections of blending systems.

Post-treatment may be achieved by the addition of chemicals as described in Chapters 2, 3 and 4. If this is undertaken there are three primary concerns that need to be addressed:

- a) The quality of the additives and the introduction of chemical contaminants produced during manufacturing, storage, distribution and transport (see Section 5.11). Unlike pre-treatment chemicals, there are no downstream processes that will remove undesirable contaminants.
- b) Controlling dose rates to ensure that required concentrations are provided.
- c) Preventing or minimizing unwanted chemical reactions following chemical addition. This issue is similar to blending. Localised changes can occur at dosing points leading to fouling problems on a microscale.

5.6.1 Operational Parameters

Operational parameters for post-treatment will vary depending on the process, the potential impacts on desalinated water quality and the nature of the distribution network. On-line measurement of pH and conductivity can be used to monitor post-treatment processes involving either blending or chemical addition. Calcium, magnesium and alkalinity should also be monitored to ensure that minimum concentrations are achieved. Dosing should be controlled by monitoring injection rates and levels in chemical tanks. Quantities of chemicals used and average dose rates should be checked on a routine basis by plant operators.

In terms of corrosivity, indices such as the LSI or CCPP can be used to ensure the desalinated water will have minimal corrosion impact on mortar lined materials while if steel or carbon/steel materials are present in the distribution system, the Larson Ratio should be used in addition to the LSI or CCPP.

As discussed in Chapter 4 depending on the source of blending waters, *E.coli* (or alternatively thermotolerant coliforms) enterococci, or coliphage can be used to assess potential impacts of faecal pollution. Processes used to treat blending waters should be monitored to ensure that they are effective.

5.7 Post treatment disinfection

General principles of post-treatment disinfection of desalinated water are similar to those of disinfection of freshwater sources of drinking water. However, the presence of higher concentrations of bromides from seawater and other brackish water sources may lead to the formation of brominated disinfection by-products. The presence of bromide can give rise to bromates if ozone is used and bromide concentrations above 0.4 mg/litre can reduce the stability of chloramines if chloramination is used to disinfect desalinated water.

5.7.1 Operational Parameters

As for other post treatment chemicals, dosing needs to be monitored. Dosing should be controlled by monitoring injection rates and residuals levels in chemical tanks. Quantities of chemicals used and average dose rates should be checked on a routine basis by plant operators. Disinfection concentrations or doses can be monitored using on-line devices or manually using field kits. Where disinfection is applied using chlorine or chloramines, residual concentrations can be measured. In combination with flow rates and detention times prior to supply to consumers the residuals can be used to calculate disinfectant CTs. Where UV light irradiation is used minimum doses can be monitored using on-line devices.

Concentrations of disinfection byproducts should be monitored. The composition of by-products will depend on the nature of disinfection e.g. trihalomethanes for chlorination, trihalomethanes and cyanogen chloride for chloramination, bromate and brominated trihalomethanes for ozonation and chlorite and chlorate for chlorine dioxide.

5.8 Storage and distribution

A point of differentiation between desalinated water supplies and other types of drinking water supply is the potential for increased corrosion unless the water is appropriately stabilised by post-treatment blending or addition of chemicals. Post-treatment monitoring should be extended into the distribution system to assess impacts of desalinated water on storage and distribution systems. Monitoring should include testing for corrosion products based on the types of materials used in distribution networks as well as in domestic plumbing. This could include testing for copper, nickel, iron, zinc and lead. If monitoring detects evidence of elevated levels of corrosion, post-treatment blending processes should be reviewed. In some circumstances the choice of materials used should also be reviewed.

Desalination systems are more prevalent in warmer climates and elevated temperatures of water in storages and distribution systems may increase the potential for growth of free-living pathogens such as *Legionella* and *Naegleria fowleri* (Chapter 4). In these climates below-ground installation of pipelines will help control water temperatures and reduce risks from these organisms. Maintaining free chlorine residuals in distribution systems can also provide protection. If this approach is adopted operational monitoring should include testing for free

chlorine residuals throughout the distribution system. An alternative strategy to provide protection from microbial growth in distribution systems is to achieve disinfection using chloramination rather than chlorination. In this case operational monitoring should include testing for total chlorine residuals throughout the distribution system.

At the end of the distribution pipeline, there is a problem when homeowners, particularly in areas where water supply has historically been unreliable, tend to install storage reservoirs, usually on the roof, which can have a negative effect on the quality of water that comes out of the user's tap.

Other types of operational monitoring could be required for control measures that are common to desalinated and non-desalinated supplies. As shown in Table 6.1 these could include measures applied to minimise intrusion of microbial or chemical contamination in distribution systems through cross-connections or backflow. Further information is provided in the *Guidelines for Drinking-water Quality* (WHO, 2004) and the supporting text *Safe Piped Water: Managing Microbial Water Quality in Piped Distribution Systems* (Ainsworth, 2004).

5.9 Discharges including concentrates, cooling water, pretreatment residuals and membrane cleaning solutions

As described in Chapter 2 desalination can produce a number of discharges including:

- residuals from pre-treatment processes used prior to membrane-based desalination. The residuals can contain solids and sludge together with coagulants and residual disinfectants. These residuals can be treated or in some cases discharged without treatment.
- membrane cleaning solutions and subsequent flushing waters
- concentrates from membrane and thermal processes including chemicals removed by the desalination process together with additives such as coagulants, scale inhibitors and anti-foaming agents. Thermal discharges may be at elevated temperatures and can contain low levels of dissolved oxygen.
- cooling water discharges from thermal processes. These can be discharged separately or blended with brine concentrates. The temperature of cooling water discharges will typically be around 10⁰ C above the temperature of source waters and dissolved oxygen concentrations may be reduced. Discharges may contain small amounts of corrosion products, disinfectants and disinfection by-products.

Concentrates and other discharges may be discharged through purpose built outfalls, existing outfalls associated with wastewater treatment plants or other industrial plants. In some cases, particularly for smaller plants, concentrates, residuals and cleaning solutions may be discharged into wastewater systems.

5.9.1 Operational parameters

The composition and volumes of discharges should be monitored to determine the chemical composition of the waste stream and to enable assessment of potential environmental impacts on receiving waters. Temperature and dissolved oxygen in discharges from thermal processes should be monitored. Where combined discharges are produced the quality of the mixed effluents should be monitored. Discharges need to meet local regional or national requirements

established by environment protection agencies and monitoring programs will need to be consistent with these requirements.

Development of bioassays could provide a useful tool to assess environmental impacts from the mixture of chemicals and physical properties in the various discharges produced during desalination. Where concentrates and residuals are discharged to wastewater treatment plants monitoring should be undertaken to determine compatibility with the wastewater quality and with any associated wastewater recycling schemes. Relative flows of wastewater and desalination discharges need to be measured as an indicator of potential variations in water quality.

A comprehensive monitoring program should include:

- *pre-treatment residuals* should be monitored for turbidity/suspended solids, coagulant chemicals, residual disinfectants and pH
- *membrane cleaning solutions* should be monitored for cleaning chemicals
- *brine discharges* should be monitored for TDS, salts, heavy metals, nutrients, temperature and dissolved oxygen (thermal processes) and additives such as antiscalants and antifoaming agents
- the temperature and dissolved oxygen of *cooling water discharges* should be monitored together with copper, nickel and iron as indicators of corrosion products.

5.10 Verification

Verification of desalinated water quality follows the same principles as those applied to other types of drinking water supply as in WSPs (WHO, 2004). The aim of verification is to ensure that desalinated water systems produce safe and acceptable drinking water that meets health-based targets. The range of parameters included in verification monitoring will be directed by established drinking water standards and guidelines. Some verification could be performed by the desalinated water producer, and some by the water supplier in the distribution system.

Verification of microbial quality will typically include testing for faecal indicator organisms and could include testing for heterotrophic plate counts (HPC) (Chapter 4). Testing for specific pathogens is generally not justified although there could be some exceptions. For example, in hot climates testing could be included for organisms such as *Legionella* or *Naegleria fowleri* that can grow within distribution systems. Verification of microbial quality needs to take into account all possible sources of contamination including desalination product water and blending waters as well as ingress during storage and distribution. Information on microbial quality in distribution systems is provided in the document *Safe Piped Water: Managing Microbial Water Quality in Piped Distribution Systems* (Ainsworth, 2004). Verification programmes for microbial quality will generally include a number of locations starting at completion of treatment and including points within distribution systems. Numbers of samples will be a function of system complexity and size and guidance is provided in the *Guidelines for Drinking-water Quality* (WHO, 2004).

The location and frequency of testing for chemical parameters will depend on potential variability and principle sources. Sampling at the end of treatment is generally sufficient for parameters that are not impacted by distribution but for parameters such as disinfection byproducts where concentrations can change, sampling should include locations at the extremities of distribution systems. Due to the presence of bromide in seawater, disinfection byproducts are likely to be dominated by brominated compounds. This could also be an issue for brackish surface water and some groundwaters. Monitoring programs should include testing for the presence of chemicals used in treatment processes as well as testing for calcium, magnesium and other mineral salts. Unless specific treatment (polishing) is applied, boron concentrations in seawater desalinated by reverse osmosis are likely to exceed the current guideline value due to limited removal efficiency of naturally occurring concentrations.

Due to the potentially aggressive nature of desalinated water verification testing by the water supplier could include testing for corrosion products from distribution systems. This testing should include corrosion products arising from household plumbing including nickel, lead, chromium (from plated parts and fixtures) and copper.

Further guidance on identifying priorities for chemical testing is provided in the supporting text *Chemical Safety of Drinking-water: Assessing Priorities for Risk Management* (Thompson, 2004).

Acceptability is an important aspect of desalinated water supplies with specific post desalination measures undertaken to improve taste. Verification should include an assessment of acceptability to consumers. In addition to testing for calcium and magnesium this can include regular testing for parameters such as TDS and pH as well as monitoring of consumer complaints and comments. Changes from the norm are particularly noticeable to consumers, who may interpret aesthetic problems as indicating health risks. While acceptability is largely a subjective judgement complaints can sometimes provide valuable information leading to detection of problems that may not have been identified by routine monitoring.

5.11 Quality control

Quality control of chemicals, maintenance of monitoring equipment, review of laboratory performance and selection of test methods are important components of monitoring programs. Chemicals and additives used in desalination processes need to be of sufficient quality, to not contain undesirable concentrations of contaminants or be toxic. Quality control of activities associated with producing data is required to ensure that results are accurate and meaningful.

5.11.1 Additives and chemicals

Side or breakdown reactions during chemical manufacturing, production, or storage can create unwanted by-products in chemical feedstocks. In some cases these may represent risks to public health. For example, chlorate and bromate contained in some sodium hypochlorite solutions can be a health concern. Chlorate concentrations should be monitored regularly as concentrations increase in storage. The rate of increase is much higher at elevated temperatures prevalent in tropical countries and sodium hypochlorite solutions should preferably be stored at low temperature and not be stored for long periods. Bromate is also commonly introduced in the production of sodium hypochlorite from sodium chloride solutions or seawater. The

concentration will vary according to bromide concentrations in the source materials and relative concentrations can increase as chlorine solutions decay in strength during storage. Hence, like conventional water treatment plants, desalination plants must have appropriate facilities to store chemicals in a manner that minimises formation of breakdown products. Adequate tankage and temperature control are features that need to be addressed during planning and design. The correct use of these facilities, maintenance of chemical stocks and control of temperature should be monitored regularly by operators of desalination facilities.

One way of ensuring the purity of delivered chemical feedstocks is to use only chemicals certified for use in the production of drinking water. Certification programs provide confidence in the quality of products. Certification programs provide formulation details, analytical data including contaminant concentrations and information on maximum use limits to avoid the introduction of deleterious levels of contaminants into treated water. Programs can also include annual inspection of production facilities as well as inspection and certification of storage and transport systems used to deliver chemicals. This means that storage facilities at production facilities, depots, and transfer stations are checked to make sure the chemicals can be properly stored and transferred. Depots and transfer stations should be protected from insects and small animals including birds.

Formal certification of chemical manufacturers to international standards will also provide confidence in the purity of products. Chemical suppliers should be evaluated and selected on their ability to supply products in accordance with required specifications. Documented procedures for the control of chemicals, including purchasing, certification, delivery, handling, storage and maintenance should be established and adherence to these procedures should be monitored. Technical specifications should be included in purchase contracts. Contract terms should specify minimum quality requirements as well as specifying certification requirements for each load of chemicals as delivered. Responsibilities for testing and quality assurance of chemicals (supplier, purchaser or both) should be clearly defined in purchase contracts. If operators are to undertake quality assurance by periodically checking the purity of the chemicals being delivered, access to analytical services will be required either in their own or a qualified external laboratory.

5.11.2 Monitoring equipment, sampling, laboratories and methods of analysis

Monitoring can be undertaken using on-line instruments, field kits and laboratory-based analyses depending upon the application of the data and the precision and accuracy requirements. In all cases the effectiveness and value of monitoring programs is dependent on accuracy. This requires the application of quality control and assurance procedures. These should include:

- maintenance and regular calibration of on-line instruments and field kits. Chemicals used in these instruments and kits should be stored under appropriate conditions and results obtained should be periodically checked by comparison with laboratory based analyses.
- assurance of the accuracy and representative nature of water samples. Guidance on sample collection is provided in International Organization for Standardization (ISO) Standard 5667.
- regular assessment of the competence and accuracy of testing laboratories. General guidance on quality assurance for analytical laboratories is provided in *Water Quality Monitoring* (Bartram, 1996).

An important issue for desalination facilities is the selection of appropriate testing equipment and testing methods. Equipment and methods used to monitor freshwater sources of drinking water may not be suitable or provide accurate results when used with high salinity water.

5.12 Monitoring plans and results

Documentation is an essential component of WSPs and operational monitoring and verification programmes should be documented in a consolidated plan. The plan should include:

- parameters to be monitored
- sampling locations and frequencies;
- sampling methods and equipment;
- schedules for sampling;
- methods for quality assurance and validation of sampling results;
- requirements for checking and interpreting results;
- responsibilities and necessary qualifications of staff;
- requirements for documentation and management of records, including how monitoring results will be recorded and stored;
- requirements for reporting and communication of results.

5.13 Surveillance

Surveillance of desalinated water supplies should follow the same principles applied to all drinking water supplies. The purpose of surveillance is to assess the safety and acceptability of water supplies and preferably should be undertaken by an agency or authority that is independent of the water supplier. In most countries the agency responsible for surveillance is the ministry responsible for public health or environment. In some cases the responsibilities could be shared or delegated to provincial, or state agencies or environmental health departments within local government. In other countries the environmental protection agency may be assigned responsibility. For desalination systems, environmental protection agencies are also likely to regulate performance and undertake surveillance relating to discharges and prevention of environmental impacts.

Surveillance should involve audit based activities and may also include direct testing. Direct testing requires the surveillance agency to have access to analytical facilities as well as having the capacity to collect samples and interpret results. Where direct testing is performed it should complement other verification testing and follow the same approach in terms of location and parameters. However, sampling frequencies may be lower than those used in verification undertaken by water suppliers.

Auditing should include examination and assessment of:

- the design and implementation of WSPs;
- records to ensure that system management including operational monitoring and verification is being carried out as described in the WSP;

- results of operational monitoring including compliance with target criteria and operational limits;
- results of verification monitoring including compliance with water quality standards and guideline values;
- incident responses including implementation of reporting requirements and corrective actions;
- supporting programmes; and
- strategies for improvement and updating of WSPs.

Auditing can also include sanitary inspections.

5.14 Regulation

Appropriate legislation, regulations and standards support the provision of safe and acceptable drinking water. They provide a framework to assist and guide water suppliers in identifying requirements and responsibilities that need to be met in designing, installing and operating drinking water supplies. They also provide benchmarks by which the activities of water suppliers and the quality of water supplied to consumers can be assessed. While legislation and regulations should include penalties for non-compliance these should be regarded as mechanisms of last resort.

Legislation should include provisions dealing with

- management of drinking water supplies;
- drinking water standards and guidelines;
- the responsibilities of water suppliers including notification requirements in the event of incidents and events that may threaten public health;
- surveillance of drinking water supplies including:
 - the identity, functions and responsibilities of the surveillance agency,
 - the authority to undertake surveillance
 - powers to enforce regulations and standards and to require remedial action in the event of non-compliance
 - the responsibility and authority to issue public advice when drinking water supplies are considered to represent an unacceptable risk to public health;
- protection of sources of drinking water including protection zones around marine or brackish water intakes to desalination plants or around groundwater bores used as sources for desalination plants.

Other issues that should be included either in legislation or associated codes of practice and technical regulations include the quality and type of materials and chemicals used in the production and supply of drinking water as well as construction and plumbing standards including provision of backflow prevention and cross-connection control. Below is a sample case study including a number of these regulatory features.

Annex: Case study-Regulation

Regulations

The enabling law requires system operators, including water producers to comply with regulations dealing with supply of safe drinking water together with consideration of plant performance and water conservation. The regulations require:

- licensees to ensure compliance with water quality standards
- that water in major pipelines and trunk mains is not contaminated and is of drinking water quality.
- that water supplied to premises is safe and acceptable
- conservation and efficient use of water
- reduction of waste and over-consumption
- publication of water quality information
- that products and processes used are approved for the production of drinking water
- water to be monitored
- notification of accidents or abnormal incidents.

Three regulations have been established to deliver these outcomes.

1. Water quality regulations

The water quality regulations deal with safety and acceptability, use of products, quality control, provision of information, standards and sampling frequency. Sampling and testing requirements are based on characteristics of the water system including source of water, treatment processes, volumes of water produced, storage facilities and distribution networks.

Sampling requirements are illustrated diagrammatically with parameters divided into six groups (A-F). The parameters included in these groups are shown in the Table below.

MSF is the predominant thermal process employed in the region with less than 15 percent utilising MED. Little groundwater is treated using membrane-based processes and this technology is more likely to be applied to desalination of seawater. In this case testing for Group D parameters may not be required.

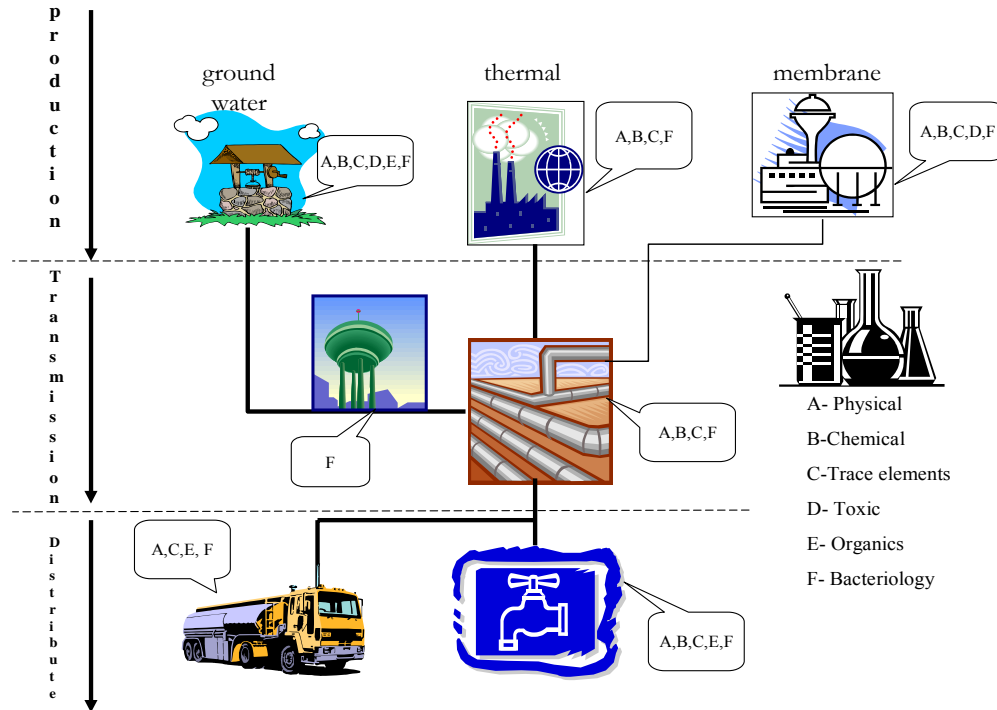
Guidelines are provided on the selection of sampling locations and the collection of samples. For example, it is recommended that treatment facilities should incorporate a storage tank with a 24 hour detention time to ensure that mixing and blending is achieved before supply. It is also recommended that water quality samples should be collected from this tank.

Example of sampling frequencies for an MSF plant producing about 45 MGD (~1.8 million cubic meters per day):

Group A (physical)	360 samples per year
Group B (chemical)	12 samples per year
Group C (trace elements)	12 samples per year
Group F (microbiology)	48 samples per year

In addition to the parameters and standards established to define water quality there are also requirements relating to minimizing corrosiveness.

Water Quality Sampling Structure



Generally the quality of distillate from MSF processes is:-

TDS	≤ 25 mg/litre
pH	5.5 to 6.5

The product water must meet the following requirements to ensure that it is non-corrosive in nature:

TDS	100 – 1000 mg/litre
Chlorine	0.2 – 0.5 mg/l at delivery to consumers
Langlier Index (LSI)	0 – 0.3 (positive)
pH value	7.0 – 8.5
CaCO ₃	max 200 mg/litre

In practice this means that thermal treatment plant operators need to provide post-treatment blending or remineralisation. This can include blending with filtered seawater or the addition of approved chemicals. Distillate is slightly acidic and the pH needs to be raised by adding lime or sodium hydroxide. Corrosion inhibitors may also be added. Finally the distillate requires disinfection to maintain microbiological quality.

With membrane desalination the required post-treatment may be limited to the adjustment of pH and disinfection. However, if the LSI indicates that the water is corrosive, calcium hardness and alkalinity may need to be adjusted.

The regulations incorporate a number of criteria relating to quality control including:

- maintenance of plants and prevention of contamination during and after completing repairs;
- use of process chemicals and inspection procedures;
- certification of laboratory equipment and testing methodology; and
- additional water quality testing before supply following restarting of thermal desalination units after long stoppages or major overhauls for corrosion products iron, copper, nickel and cadmium and other trace elements

2. Drinking water supply regulations

The water supply regulations address issues associated with customer storages and plumbing. The regulations include criteria relating to construction materials, tank fittings, tank cleaning, disinfection and inspection provisions. The regulations also require fitting of water meters and automatic control devices to prevent tank flooding and back contamination.

3. Incident reporting and investigation regulations

System operators are required to maintain contingency plans for bacteriological contamination and hydrocarbon pollution and report any such incidents to the Bureau.

Group	Classification	Parameters
A	Physical	Colour, turbidity, odour, taste, TDS, calcium hardness, total hardness, chlorine, conductivity, pH
B	Chemical	sulphate, magnesium, sodium, potassium, chlorides, nitrate, nitrite, ammonium, total organic carbon, dissolved or emulsified hydrocarbons; mineral oil, aluminium, iron, manganese, copper, zinc, phosphorus, fluoride
C	Trace elements	arsenic, cadmium, cyanides, chromium, mercury, nickel, lead, antimony, selenium, barium, boron
D	Toxicants	Endrine, lindane, methoxychlor, 2,4 dichlorophenoxyacetic acid, 2,4,5 trichlorophenoxypropionic acid, phenols, heptachlor, aldrin, DDT, chlordane, dieldrin, heptachlor epoxide
E	Organics	Trichloroethene, tetrachloromethane, tetrachloroethene, chloroform, polycyclic aromatic hydrocarbons, trihalomethanes, 1,2 dichloroethane, benzene, benzo(a)pyrene, bromoform, dichloromethane, bromodichloromethane, chlorobenzene
F	Microbial	Total coliforms, <i>E.coli</i> or thermotolerant coliforms, enterococci, HPC

End of Annex-----

5.15 Monitoring recommendations

Monitoring should be conducted in accord with the principles of Water Safety Plans and include operational monitoring, verification and surveillance.

- Operational monitoring should be the focus of testing programmes and is required to assess the effectiveness of the control measures that are used ensure that safe drinking water is produced from saline and brackish waters.
- A summary of recommended monitoring requirements for the control measures identified in Chapter 2 is provided in Table 5.1. Indicative frequencies are presented for large (≥ 10 MGD) and small plants (< 1 MGD).
- The range of parameters and extent of operational monitoring will depend on risk assessment including:
 - the type of desalination process being used
 - the nature, stability and quality of the source water
 - the size of the desalination system
- Where necessary operational monitoring requirements should be prioritized on the basis of risk.
- The quality of operational monitoring will depend on the capacity of testing facilities and equipment and application of quality assurance/quality control procedures.

- Verification should follow the same principles as those applied to other types of drinking water systems. However, increased attention may need to be paid to the presence of brominated disinfection byproducts particularly where seawater is the source. In addition, due to the potentially aggressive nature of desalinated water verification testing should include corrosion products arising from distribution systems and household plumbing.
- Verification should ensure that safe and acceptable water is delivered to consumers. In addition to testing of water from distribution systems for health-related parameters verification should include assessment of acceptability. This could include testing for TDS and pH as well as monitoring consumer complaints.
- Surveillance should follow the same principles as those applied to other types of drinking water systems. It can involve audit based activities and direct testing. Surveillance should preferably be undertaken by an agency or authority that is independent of the water supplier.
- Appropriate legislation, regulations, codes of practice and technical documents support the provision of safe drinking water and provide a framework to guide water suppliers in identifying requirements and responsibilities.

Research needs

- Equipment and methods used for freshwater sources may not be suitable or accurate when used with high salinity water. Analytical methods tailored for use with seawater and brackish water sources of desalinated supplies need to be developed.
- Improved methods for on-line operational monitoring of membrane integrity are required.

Table 5.1 Suggested monitoring parameters and frequencies for desalination plants

These suggestions are intended to provide perspective for decision makers to determine the most appropriate monitoring type, frequency and locations to suit their particular circumstances and needs.

Component	Control measures	Operational Parameters	Monitoring frequency	
			Large plant	Small plant
Source Water	Detect and prevent contamination by sewage (Pathogenic protozoa, viruses, bacteria) (Likelihood of presence based on sanitary inspection)	Enterococci and/or <i>E.coli</i>	D or W	W
	Detect and prevent impacts of storm events	Turbidity (used as on-line measurement for process control)	Preferably on-line	Preferably on-li
	Detect and prevent impacts of microalgae/cyanobacteria	Algal species, including cyanobacteria, dinoflagellates, or chlorophyll as a surrogate	W or M	M
	Detect and prevent impacts by industrial discharges (based on an assessment of local conditions)	TOC (if concentrations change investigate sources)	W	M
		Petroleum oil hydrocarbons/grease including volatile compounds	W	Y
		Industrial chemicals	W	M
	Radioactivity	Y	Y	

	Monitoring associated with downstream control measures (pre-treatment and treatment)	Salinity Chloride Sodium Boron Bromide Silica Iron Manganese Turbidity Alkalinity pH Temperature Heavy metals Low solubility chemicals e.g. Ca, F, Ba, Sr, Mg, fluoride, sulfate Hydrogen sulphide and metal sulphides Ammonia Total dissolved solids (TDS)	D D W M M D D D M On-line D On-line On-line W W W W W D	D D W Y Y D D W Y On-line D On-line On-line M M M M D
Pre-treatment	Membranes Detection and prevention of biofouling/scaling/precipitation Use of additives e.g. antiscalant Quality control on additives and materials Prevention of microbial fouling	SDI Flow rates Conductivity Conductivity/TDS ratios Turbidity after pre-treatment, particle counts pH (if acidification or alkalinisation) Flow and dose rate monitoring Test additives and materials; check records Disinfectant residual or ORP	On-line On-line On-line D On-line On-line On-line D On-line	On-line On-line On-line D D On-line On-line D On-line
Pre-treatment	Thermal Processes Use of additives e.g. antiscalant, antifoaming Quality control on additives and materials Prevention of microbial fouling	Flow and dose rate monitoring pH (if acidification used) Test additives and materials; check records Disinfectant residuals	On-line On-line D On-line	On-line On-line D On-line
Process Management	Membranes	Recovery ratio (calculated from flow rates) Chemical balance from conductivities and flow rates (calculated) Trans-membrane pressure Flow meters on permeate and brine Conductivity in permeate and brine TOC (particularly where source water contains	D W On-line On-line On-line On-line	D M On-line On-line On-line On-line

		elevated microbial contamination)		
	Thermal Processes	In-coming steam pressure and temperature Make-up and distillate flow rate Distillate and condensate conductivity Top brine temperature (MSF/MED) Copper, iron and nickel (corrosion) Hydrazine and other boiler treatment chemicals (MED-TC) (depending on design)	On-line On-line On-line On-line W W	On-line On-line On-line On-line Q M
Blending	Preventing microbial contamination (only use pretreated water or protected groundwater. Untreated surface water not to be used)	<i>E.coli</i> /enterococci in blending water Appropriate parameters for processes used to treat blending water e.g. turbidity for filtration, disinfectant dose/concentration	D On-line	W On-line
	Providing chemical stability, maintaining minimum calcium and magnesium concentrations	LSI/CCPP where mortar linings used Larson Ratio Index where steel or carbon/steel used Calcium and magnesium pH Conductivity	D D D On-line On-line	D D D On-line On-line
Remineralisation	Providing chemical stability, maintaining minimum calcium and magnesium concentrations Quality control on additives and materials	LSI/CCPP where mortar linings used Larson Index where steel or carbon/steel used Calcium and magnesium (or total hardness) Alkalinity pH Conductivity Test additives and materials; check records	D D D D On-line On-line D	D D D D On-line On-line D
Disinfection	Removal of microbial contaminants	Disinfectant dose monitoring Calculate Ct HPC Disinfection byproducts (including brominated compounds) relevant to the method of disinfection	On-line D M W	On-line W Y M
Corrosion inhibition	Reduction of corrosion in distribution systems using inhibitors such as phosphates and silicates Quality control on additives and materials	Flow and dose rate monitoring Test additives and materials; check records	On-line D	On-line D

Storage Distribution	Preventing microbial and chemical contamination by controlling intrusion through cross connections/backflow or faults in mains or other infrastructure	<i>E.coli</i> HPC Turbidity Inspect for system integrity, monitor burst main frequency and repairs Monitor system leakage	D D D W M	W M D M Y
	Control of free living microorganisms	HPC Disinfectant residual (consider persistent disinfectant where <i>Legionella/Naegleria</i> potential considered unacceptable)	D D	W D
	Prevention of corrosion in storage tanks, long pipes, domestic plumbing	pH Iron Zinc Nickel Copper Lead (if problem) Zinc and phosphate (if corrosion inhibitors are used)	D M M M M M W	D M Y Y Y M W
	Maintain chemical stability after mixing different sources (desalinated/non-desalinated water) or after disinfection	Post mixing or post disinfection monitoring for LSI/CCPP where mortar linings used or Larson Index where steel or carbon/steel used	D	D
	Disinfection	Disinfection by-products (including brominated compounds)	W	M
Concentrate discharges	In marine or brackish lake environments select discharge points to minimise impacts. Discharge into areas with high levels of mixing or use diffusers to promote mixing	Temperature and DO (thermal processes) pH Salinity Heavy metals/salts Additives Phosphates and nitrates	On-line On-line On-line M M M	On-line On-line On-line Q Q Q
	For brackish aquifer apply discharge requirements set by environment protection agencies	Temperature (thermal processes) pH Salinity Heavy metals/salts Additives Phosphates and nitrates	On-line On-line On-line M M M	On-line On-line On-line Q Q Q

Cooling water discharges	In marine or brackish lake environments select discharge points to minimise impacts. Discharge into areas with high levels of mixing or use diffusers to promote mixing For brackish aquifer apply discharge requirements set by environment protection authorities	Temperature Dissolved oxygen Corrosion products (Cu, Iron, Ni) Disinfectant residuals	On-line On-line W D	On-line On-line Q W
		Temperature Dissolved oxygen Corrosion products (Cu, Iron, Ni) Disinfectant residuals	On-line On-line W D	On-line On-line Q W
Wastewater effluents from pre-treatment facilities or from membrane cleaning	Collect discharges and treat or discharge in accord with requirements set by environment protection agencies	pH Turbidity Suspended solids(SS) Residual disinfectants Iron or aluminium – based on the type of coagulant used Membrane cleaning agents	On-line On-line D D W on discharge	On-line On-line D D M on discharge

Note 1) Monitoring frequency; D: daily, W: weekly, M: monthly; Q: quarterly and Y: yearly. In some cases monitoring requirements will be based on the source of water (seawater, estuarine or groundwater) and sanitary surveys. For example the frequency of petroleum hydrocarbon monitoring will be influenced by the likelihood of potential sources of contamination.

2) The capacity of a “large” or “small” plant is assumed to be more than 10 MGD or 1 MGD, respectively.

References

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Environmental Impact Assessment (EIA) of Desalination Projects

An Environmental Impact Assessment (EIA) is a procedure that identifies, describes, evaluates and develops means of mitigating potential impacts of proposed activities on the environment. The main objective of an EIA is to promote environmentally sound and sustainable development through the identification of appropriate mitigation measures and alternatives. In an EIA, information on the environmental consequences of a project is provided to the public and to decision makers. Based on the EIA, a decision can be reached which balances the societal and environmental impacts and benefits. A detailed EIA is often required for large infrastructure projects, such as a water treatment plant or a dam serving one or more large urban centers. For smaller projects, a simplified EIA may be warranted due to the limited potential of the project to cause significant environmental impacts. In principle, EIAs for desalination projects should not differ in terms of complexity and level of detail from these for other infrastructure projects and water supply systems. Depending on the proposed project, it is incumbent on national authorities to individually define the need, scope and complexity requirements for each Environmental Impact Assessment Study.

Project EIAs are to be distinguished from Strategic Environmental Assessments {SEAs or strategic (program) EIAs} that are undertaken for strategic plans, policies or management programmes. The main objective of a strategic EIA is to ensure that potential impacts are addressed during preparation and before adoption of a new plan, policy or programme. Strategic EIAs will not make EIAs at the project level dispensable – both are rather complementing instruments. Although this document will not further address strategic EIAs, it is emphasized that these could be adequate instruments to manage water supply planning on a regional or national scale. The most relevant plans to address desalination projects along with other water supply alternatives are integrated water resources management (IWRM) and integrated coastal zone management (ICZM) plans.

EIAs are not limited to environmental aspects, but typically address all potential key impacts of new projects, plans or activities on “man and environment”. They consequently relate to many facets of science. In general, an EIA for a water supply project, including that for a desalination project, should predict the impacts related directly or indirectly to the implementation of the project. This may require an interdisciplinary approach covering relevant issues of marine and terrestrial ecology, hydrology and geology, or other disciplines. Taken a step further in relating potential impacts to people and communities, it may also be necessary to consider human health and socio-economics. Where appropriate, these should take into account gender- and age-specific effects and variations among the potentially affected population or community, such as social or ethnic affiliations of sub-groups. Public participation is also considered a fundamental element of EIAs in order to involve the public in the evaluation of potential impacts and in decision-making.

The environmental impact of desalination and its discharges should be also assessed in the context of the environmental impacts of water supply alternatives that may be used instead of

desalination. Desalination projects are typically driven by the limited availability of alternative lower-cost water supply resources such as ground water or fresh surface water (rivers, lakes, etc.). However, environmental impacts may also result from continuation of those water supply practices. For example over-pumping of coastal aquifers over the years has resulted in a significant increase in the salinity of the groundwater and damaged fresh water aquifers. In some arid areas transfers of fresh water from a traditional water supply source, such as river, river delta or a lake, have impacted the eco-balance in this fresh water source to an extent that the long-term continuation of such water supply practice may result in significant and irreversible damage of the ecosystem of the traditional fresh water supply source. In such cases, the environmental impacts of the construction and operation of a new seawater or brackish water desalination project should be weighed against the environmentally damaging consequences from the continuation/expansion of the existing fresh-water supply practices. Waste streams generated from desalination plants, with the exception of the high-salinity reject water, are similar to the waste streams generated by conventional water treatment plants and water reuse facilities. Water reclamation plants, also generate waste streams that usually contain the same chemicals used for desalination and may have elevated content of man-made waste substances which may have impacts on the marine environment. Wastewater reuse for beneficial purposes is another factor to be considered among the options and combinations of options that exist.

With the context so broad, the present document cannot fully encapsulate the whole spectrum and depth of implications of all desalination projects on a worldwide scale. Rather it provides a general overview of the potential impacts of a desalination project on the environment. (Emphasis is placed on the impacts that are specific to desalination projects, such as the impacts of reject streams and chemical additives on the marine environment, whereas impacts common to other infrastructure projects are not discussed in detail.

This document further seeks to provide guidance on how to carry out an EIA (see 6.3). The proposed methodology is not limited to desalination plants, but can be applied to other water infrastructure projects in a similar manner. Based on the information provided, it should be decided on a case by case basis which issues are relevant for an individual desalination project, and an individual approach should be developed to carry out the EIA.

In addition to the obvious benefits of a supply of high quality water, desalination, similar to other water supply alternatives, will consume considerable community resources. This includes economic and social capital, access to coastal land, energy, and on-going revenue to operate and maintain the facility. Desalinated water should thus be regarded as a community asset and a valuable resource. In addition to considering the measures outlined in this document to assess and mitigate potential impacts of the production process, it is also incumbent upon communities to value the water produced by desalination by non-wasteful use and by looking for opportunities of multiple use before the water is discharged.

Finally, although there is at least a 50 year history of large scale desalination projects, the present knowledge of the environmental, socio-economic and human health implications of desalination and its alternatives (water reuse, extended use of limited traditional water supply sources and conservation) could be expanded. This and the fact that EIAs are undertaken before projects are implemented, means that although they are based upon detailed analyses, EIAs can only give a prognosis of the expected impacts based on the information available. It is therefore important to clearly identify any gaps of knowledge in the EIA and to apply the precautionary principle as defined by the UN in the evaluation of potential impacts. Further research should be

initiated and monitoring data from existing facilities and EIA results should be made available to a wider public to improve the understanding of the actual impacts of all water supply alternatives including desalination, reuse, conservation, and the use of traditional water supply sources.

6.1 Potential environmental impacts of desalination projects

Chapter 2 of this document provides an overview of the potential impacts of desalination projects on the environment and references for further reading. It describes impacts on the marine environment that are specific to desalination projects, and in particular, on the impacts of reject streams and chemical additives. Impacts common to many development projects, such as surface sealing or air emissions, are not covered. It is assumed that common effects are sufficiently known and information is readily available from other sources such as relevant literature or other development projects. There are still many gaps of knowledge and uncertainties regarding the actual impacts of desalination projects, as monitoring results of operating plants are only available to a limited extent. Also, a wide variety of project- and site-specific impacts may occur. The following list can thus not be complete or final, and not every described effect will apply to each individual project. Further research is required and the provision of monitoring results to a wider audience highly recommended.

Also see the following literature if not cited otherwise:

- UNEP/MAP/MEDPOL (2003) Sea Water Desalination in the Mediterranean: Assessment and Guidelines. MAP Technical Reports Series No. 139, United Nations Environment Programme (UNEP), Mediterranean Action Plan (MAP), Programme for the Assessment and Control of Pollution in the Mediterranean region (MEDPOL), Athens.
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6.2 Concept and methodology of EIA in general and in desalination projects

6.2.1 Introduction to development of an EIA

EIA is a systematic process used to identify, evaluate and develop means of mitigating potential effects of a proposed project prior to major decisions and commitments being made. This process applies for all wastewater, water reuse and water treatment projects, including desalination plants. It usually adopts a broad definition of “environment” considering socio-economic as well as environmental health effects as an integral part of the process. The main objectives of EIAs are to provide information on the environmental consequences for decision-making, and to promote environmentally sound and sustainable development through the identification of appropriate alternatives and mitigation measures (UNEP 2002).

The three central pillars of an EIA are:

- The establishment of environmental, socio-economic, and public health baseline data for the project site before construction. A prognosis of the “zero alternative” is given, which is the expected development of the project site without project realisation.

- The prediction and evaluation of potential – direct and indirect – environmental, socio-economic, and public health impacts of the proposed project.
- The identification of appropriate alternatives and mitigation measures to avoid, minimise, remediate or compensate for any environmental, socio-economic, and public health impacts resulting directly or indirectly from the project.

In essence, EIA of desalination projects is a systematic process that examines the environmental, socio-economic, and health effects during all life-cycle stages of the project, i.e. during construction, commissioning, operation, maintenance and decommissioning of the plant. The impacts of a proposed desalination project are those alterations in environmental conditions compared with what would have happened had the project not been undertaken (zero alternative).

6.2.2 Systematic EIA process for desalination projects

The EIA process is generally marked by three main phases (Figures 6.1-6.3):

- The pre- or initial EIA phase includes screening and scoping of the project.
- The main EIA phase refers to the actual environmental impact assessment, including the establishment of baseline data, the prediction and evaluation of potential impacts, and the identification of appropriate alternatives and mitigation measures (see “three pillars” above).
- The final EIA phase involves decision-making and a review of the EIA process.

In the following, a 10 step process is proposed for conducting EIAs for desalination projects. It should be noted that in practice, deviations from the outlined process may occur. Single steps may not always be clearly limitable, some steps may overlap or may be interchanged. The EIA procedure should thus be understood as a continuous and flexible process.

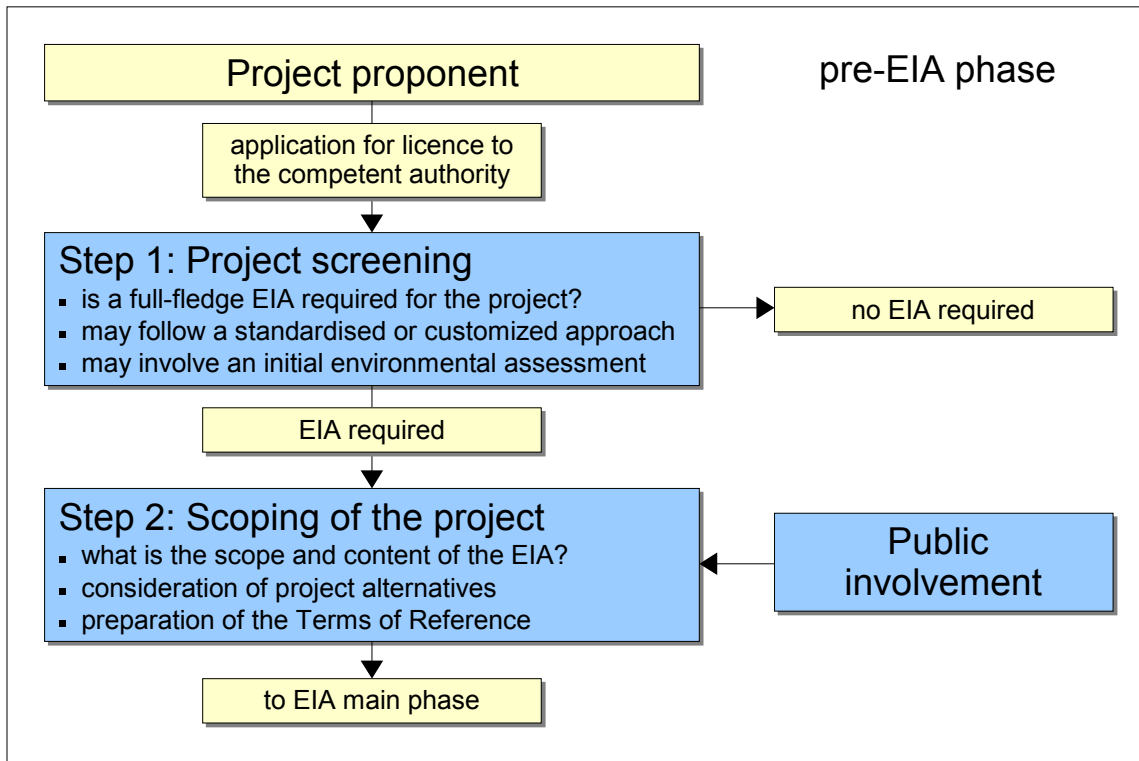


Figure 6.1: Pre- or initial EIA phase (scoping and screening)

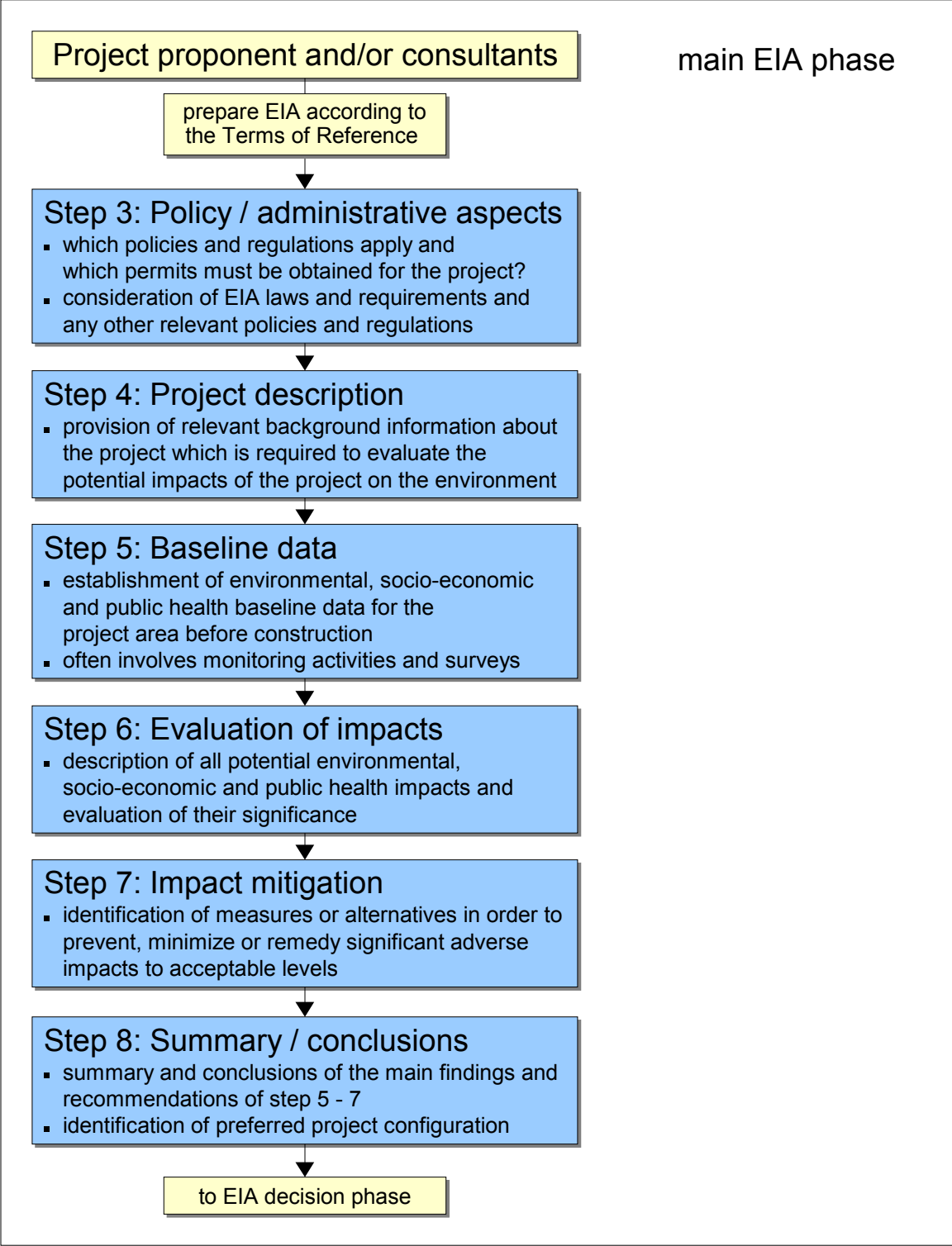


Figure 6.2: Main EIA phase

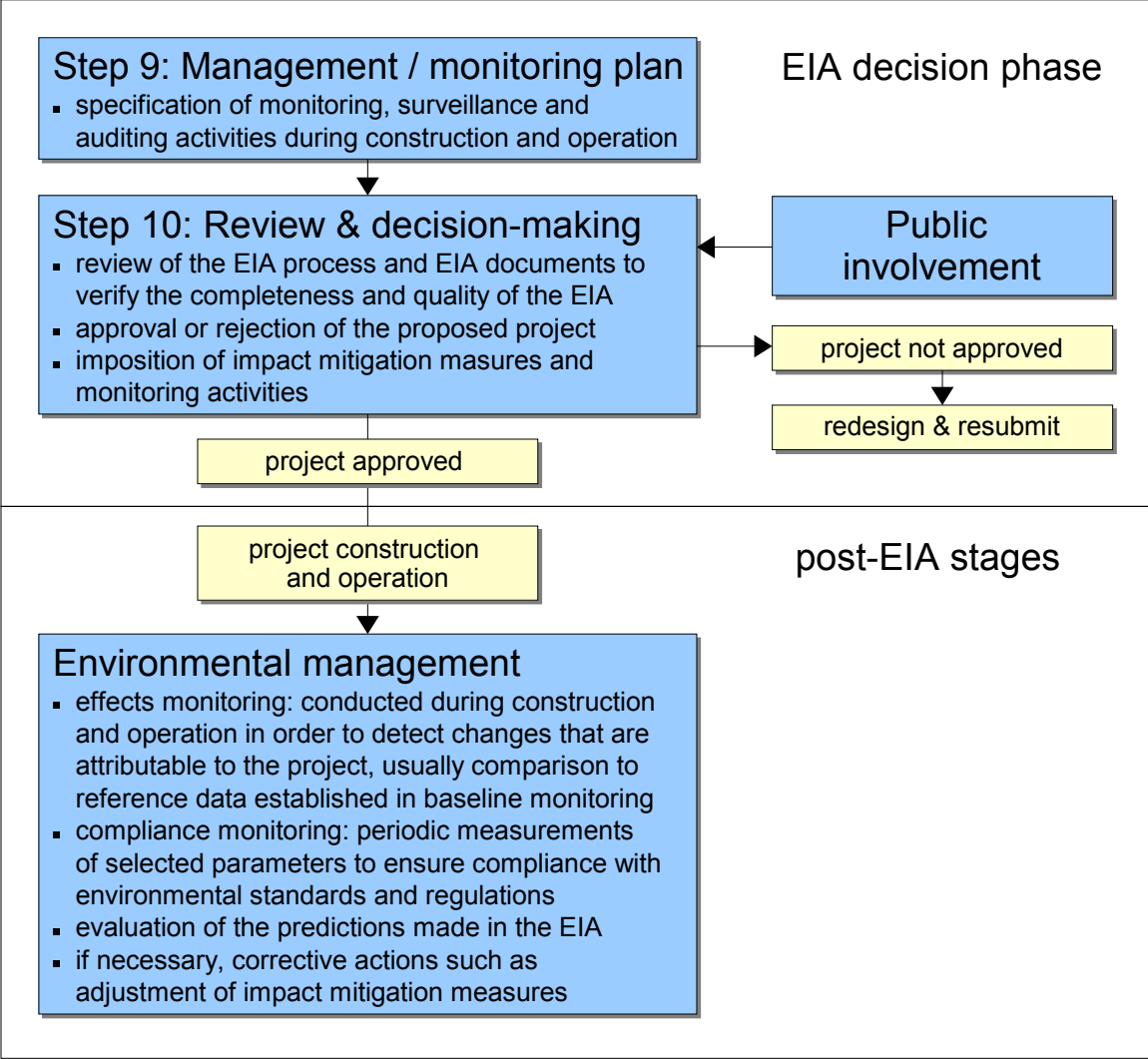


Figure 6.3: Final EIA phase (SEE MEASURES in Box 10)

Step 1 – Screening of the project

Screening is the process by which a decision is taken on whether or not an EIA is required for a particular project. It shall ensure that a full EIA is only performed for projects with potentially significant adverse impacts or where impacts are not sufficiently known. Screening thus involves making a preliminary determination of the expected impact of a proposed project on the environment and of its relative significance. A certain level of basic information about the proposal and its location is required for this purpose. The screening procedures can be broadly classified into two approaches: a *standardised* approach, in which projects are subject to or exempt from EIA defined by legislation and regulations; and a *customised* approach, in which projects are screened on a case-by-case base, using indicative guidance (UNEP 2002).

Standardised approach

Many states have implemented EIA laws and procedures, which facilitate the screening process by defining for which project categories an EIA is required, such as:

- ‘mandatory’ or ‘positive’ lists which include projects always requiring EIA (e.g. major projects, possibly large co-generation plants for electricity and water);
- project lists which define thresholds and criteria above which EIA is required (e.g. a desalination plant with more than 20,000 m³/day of production capacity);
- ‘exclusion’ or ‘negative’ lists which specify thresholds and criteria below which EIA is never required or below which a simplified EIA procedure applies (e.g. a desalination unit with less than 4,000 m³/day of production capacity).

A class screening may be undertaken for small-scale projects that are routine and replicable, if there is a reasonably sound knowledge of the environmental effects and mitigation measures are well established. For example, class screening could be applicable to small-scale, stand-alone desalination systems such as these for hotels, small residential and recreational communities, industrial facilities, military installations, etc. The regulations for water treatment facilities in general and for desalination plants in particular may vary considerably in different states. If the categorisation of projects in general or of desalination plants in particular has not been undertaken, or if a proposed desalination project is on the borderline of a threshold, the project would need to be screened on an a case-by-case basis (customised approach).

Customised approach

Individual screening does not necessarily require additional studies, but can be conducted on the basis of indicative guidance, for example indicators and checklists. These are intended to be used quickly by people with the qualifications and experience typically found in competent authorities or environmental consultant companies, using the information which is readily available about the project and its environment.

The World Bank (1991) categorisation of projects may allow a first, broad screening of desalination plants based on a few common indicators, such as the type, size and location of the project, environmental sensitivity, and likely health and social effects on the local population:

- ***Category A: full EIA required***

Projects likely to have significant adverse environmental impacts that are significant (i.e. probably irreversible, affect vulnerable ethnic minorities, involve involuntary resettlement, or affect cultural heritage sites), diverse, or unprecedented, or that affect an area broader than the sites of facilities subject to physical works (e.g. dams and reservoirs, large-scale industrial plants, port development, thermal- and hydropower development, etc.).

- ***Category B: limited EIA to identify and incorporate suitable mitigation measures***

Projects likely to have adverse environmental impacts that are less significant than those of category A, meaning that few if any of the impacts are likely to be irreversible, that they are site-specific, and that mitigation measures can be designed more readily than for category A projects (e.g. small scale aquaculture, renewable energy, rural electrification, rural water supply and sanitation, etc.).

- **Category C: no EIA**

Projects that are likely to have minimal or no adverse environmental impacts.

Comprehensive indicator lists or checklists can be used for screening, such as the checklists prepared by the European Union as part of the EIA directive framework¹ (EU 2001a). They include a list of questions referring to the project and its environment, which shall help to answer the question if the project is *likely* to have a *significant effect* on the environment. There is no specific rule that can be used to decide whether the results of screening should lead to a positive or negative screening decision (i.e. that EIA is or is not required). As a general principle, the greater the number of positive answers and the greater the significance of the effects identified, the more likely it is that an EIA is required. Uncertainty about the occurrence or significance of effects should also point towards an EIA, as the EIA process will help to clarify the uncertainty. If the need for EIA has been affirmed, scoping follows as the consecutive step.

Preliminary EIA study

In some EIA systems, screening is considered as a flexible process which can be extended into a preliminary form of an EIA study (often termed preliminary or initial environmental assessment). This is typically carried out in cases where the environmental impacts of a proposal are uncertain or unknown, e.g. new technologies or undeveloped areas (UNEP 2002). If a preliminary assessment is undertaken to assist in the screening decision, the information from the preliminary assessment can also be used for scoping and later in the actual EIA process.

Documentation of screening results

After a formal decision has been made by the competent authority, an official screening document is typically prepared which records the screening decision and provides an explanatory statement for this decision. It may be extended into a short screening report which also gives the results of the preliminary assessment, and can be used to prepare the scoping document for public dissemination in the following stage.

Step 2 – Scoping of the proposed desalination project

Scoping is the process of determining the content and extent of the EIA. The Terms of Reference (ToR), which are elaborated in the process, provide clear instructions to the project proponent on the information that needs to be submitted to the competent authority for EIA, and the studies to be undertaken to compile that information.

Scoping is a crucial step in EIA because it identifies the issues of importance and eliminates those of little concern. In this way, it ensures that EIAs are focused on the significant effects and do not involve unnecessary investigations that waste time and resources. The process is completed with preparation of the ToR. However, experience shows that the ToR should be flexible to some degree, as they may need alteration as further information becomes available, and new issues emerge or others are reduced in importance (UNEP 2002). The following range of issues should be considered when planning the scoping phase and preparing the ToR.

¹ EIA Directive 85/337/EEC from 1985, amended by Directive 97/11/EC in 1997.

Consideration of alternatives

The consideration of alternatives to a proposal, such as alternative technologies or sites, is a requirement of many EIA systems. It should be understood as a dynamic process that starts early in project planning and continues throughout the EIA process and decision-making.

Alternatives to a proposal can be generated or refined most effectively in the early stages of project development. At the stage of scoping, a number of alternatives is typically identified, which are subsequently evaluated in the EIA. Alternatives may also be identified later on in the process, especially at the stage when impact mitigation measures are elaborated. The EIA should be open to new, emerging alternatives at all times, while previously considered options are possibly abandoned in the light of new information. The aim is to identify the best practicable option under environmental, socio-economic and human health criteria that is also technically and economically feasible. It is important that the consideration of alternatives during an EIA is not reduced to a superficial and meaningless exercise.

Selection of the project site

Environmental, socio-economic and public health impacts resulting from the construction and operation of a desalination plant are in large part dictated by the location of the facility and its associated infrastructure. Therefore, proper site selection for a desalination plant during the planning process is essential for impact minimisation.

Site selection typically takes place in the early stages of a desalination project and leads to the identification of a preferred site and possibly one or two alternatives. An EIA, usually accompanied by a site-specific monitoring programme, will then be carried out for the identified location(s). In many cases, the competent authority will attach conditions to project approval, such as to implement certain mitigation measures in order to minimise impacts on the project site. In some cases, however, the EIA may also come to the final conclusion that the chosen site(s) are not suitable, even if impact mitigation measures are implemented.

To reduce the likelihood of this outcome, site-selection should play an important role in project planning. Site selection can take place during a 'preliminary' EIA study as part of the screening process (cf. Step 1 above), or during scoping when the EIA requirements are determined. To facilitate the site selection process for desalination plants, public authorities may designate suitable areas in regional development plans or may provide criteria that can be used by project developers. Site selection must be carried out on a case-by-case basis, since there are a large number of site-specific considerations that vary according to the specific operational aspects of each plant. Generally, it is important to consider the following site features.

- ***Geologic conditions***

Sites should provide stable geologic conditions and little risk that construction and operation of the plant will affect soil and sediment stability.

- ***Biologic resources***

Ecosystems or habitats should be avoided where possible,

- if they are unique within a region (e.g. reefs on an otherwise sandy shoreline) or worth protecting on a global scale (e.g. coral reefs, mangroves);

- if they are inhabited by protected, endangered or rare species (even if temporarily);
- if they are important in terms of their productivity or biodiversity;
- if they have important biological functions, such as feeding grounds or reproductive areas for a larger number of species or certain key species within a region;
- if they are important for human food production (fishing or marine harvesting).

- ***Oceanographic conditions***

The site should provide sufficient capacity to dilute and disperse the salt concentrate and to dilute, disperse and degrade any residual chemicals. The load and transport capacity of a site will primarily depend on water circulation and exchange rate as a function of currents, tides and/or surf, water depth, bottom and shoreline morphology. In general, exposed rocky or sandy shorelines with strong currents and surf may be preferred over shallow, sheltered sites with little water exchange. Water exchange and sediment mobility will affect the residence time of pollutants within the ecosystem and the time of exposure for marine life to these pollutants.

- ***Raw water quality and proximity***

The intake location should ideally provide a good and reliable water quality, taking seasonal changes into account, with minimum danger of pollution or contamination, in order to avoid performance problems of the plant or impacts on product water quality. The plant site should ideally be close to the source water intake to minimise land use for pipelines and to avoid passage of pipes through agricultural land, settlements, etc. However, this cannot be generalised and in some cases it may be more appropriate to locate the plant further inland, for example when construction on the shore is not possible for certain reasons (e.g. use of beaches, nature reserves, geological instability, etc.).

- ***Proximity to water distribution infrastructure and consumers***

The site should ideally be close to existing distribution networks and consumers to avoid construction and land-use of pipelines and pumping efforts for water distribution. However, impairment of nearby communities (i.e. consumers) by visual effects, noise, air pollution or other environmental health concerns should be avoided.

- ***Vicinity of supporting infrastructure***

The site should allow easy connection with other infrastructure, such as power grid, road and communication network, or may even allow the co-use of existing infrastructure, such as seawater intakes or outfalls.

- ***Conflicts with other uses and activities***

The site should ideally provide no conflict or as little as possible with other existing or planned uses and activities, especially recreational and commercial uses, shipping, or nature conservation.

Public involvement

Public participation is a mandatory requirement in the planning and implementation of development projects, and an inherent component of the EIA process, especially of scoping. As a

general rule, the public should be involved as early as possible and continuously throughout the EIA process. The overall goal is the involvement of the public in decision-making. This is based on fundamental premises of democratic societies, such as transparency of decision-making and equity among the affected populations in terms of ethnic background and socio-economic status.

Public involvement in desalination projects – seeks to:

- inform the public about the desalination project;
- gather a wide range of perceptions of the proposed desalination project, addressing the benefits, potential public health, environmental and socio-economic impacts and their short- and long-term implications;
- present a discussion of project alternatives including water conservation and recycling;
- provide information on the value of the desalinated water and the extent of the likely community investment;
- take advantage of the knowledge of indigenous and local communities about their living environment.

The overall benefits of public involvement are to:

- develop partnership with the community which is critical for project sustainability;
- address and, where applicable, dispel subjective public doubts and concerns about the project;
- develop trust and working relationships among the stakeholders, including the affected communities, particularly vulnerable groups, developers, planners, local and national governments, decision-makers, NGOs, and networks of people and organisations;
- ensure that important issues are not overlooked when the ToR are prepared, thus providing for the comprehensiveness, integrity, quality and effectiveness of EIA.

Human health impact assessment

EIAs, as widely required by national legislations and international agencies, offer integrated analyses of potential impacts of development projects on *all* components of the environment, including human health. There has been recent emphasis on the necessity to delineate the *health effects of environmental impacts* (as stated in the 2003 European Directives² and the ESPOO Convention on EIA³) on directly or indirectly affected populations. When conduction scoping for a desalination project, relevant human health effects should therefore be identified.

The human health component should be broadly addressed in EIAs for desalination projects, relying on readily available information. This includes community health determinants, such as incidences of disease, public information and concerns, and traditional knowledge of the local inhabitants and indigenous population. Baseline information on health and quality of life needs to be established in order to assess the significance of potential effects of environmental impacts. Potential environmental health impacts should be prioritised, with corresponding indicators and risk factors. Both positive and negative health effects should be delineated, for the

² EIA Directive 85/337/EEC from 1985, amended by Directive 97/11/EC in 1997

³ Convention on Environmental Impact Assessment in a Transboundary Context (Espoo 1991)

public at large as well as for vulnerable groups. Where there are specific concerns with exposure to certain toxic emissions or infectious agents, the scientific literature should be searched for relevant published studies and epidemiological investigations. This is usually sufficient to address concerns with the potential health impact. Most EIA assessments rely on existing information. Except for large projects, it is often too expensive, and too time consuming to generate new health information within the timeframe allotted to develop the EIA.

Procedures for environmental health impact assessment within EIAs are described in greater detail in the publication “Environmental Health Impact Assessment of Development Projects: A Practical Guide for the WHO Eastern Mediterranean Region” (WHO 2005).

Gender impact assessment

Gender mainstreaming is a globally accepted strategy for promoting gender equality⁴. The UN Economic and Social Council⁵ defined gender mainstreaming as the process of “assessing the implications for women and men of any planned action, including legislation, policies or programmes, in all areas and at all levels”, so that “women and men benefit equally and inequality is not perpetuated.” Gender Impact Assessment is increasingly recognised as an adequate tool for implementing gender mainstreaming. It is usually applied to policies and programmes, and means to compare and assess, according to gender relevant criteria, the current situation and trend with the expected development (EU 1997). In the same manner as policies and programmes may have differential impacts on women and men, many development projects will not be gender neutral. Gender-specific effects may not be easily recognised, but an effort should be made to identify any significant effects that may perpetuate gender inequality.

Water projects and thus desalination projects have a high potential for gender-specific effects. “Women play a central part in the provision, management and safeguarding of water”, which is one of four recognised principles of the Dublin Statement on Water and Sustainable Development⁶. The consideration and integration of gender-specific effects in EIAs for desalination plants, from scoping to decision-making, is thus highly recommended to evaluate the advantages and disadvantages of desalination activity on both sexes. Where appropriate, a distinction in the EIA process should be made between impacts on men and women.

Scoping procedure

Scoping procedures may vary considerably in different states. For example, scoping may either be carried out under a legal requirement or as good practice in EIA, or it may either be undertaken by the competent authority or by the project proponent (EU 2001b). It is recommended that the competent authority takes responsibility at least for monitoring of the process, for preparing the minutes and official transcripts of the scoping meetings, for keeping the records of the scoping outcome, and for preparing the ToR. As a generalised approach, the scoping procedure may follow the following steps:

- Based on the information collected during screening, a scoping document containing a preliminary environmental analysis will be prepared. This will specify details and proposed

⁴ UN Office of the Special Advisor on Gender Issues and Advancement of Women (OSAGI)

⁵ ECOSOC Agreed Conclusions, 1997/2

⁶ International Conference on Water and the Environment, Dublin 1992, organised by the UN World Meteorological Organization (WMO)

location of the project, review alternatives, briefly and concisely describe the environmental characteristics of the selected site and raise potentially significant project-related issues. The scoping document serves as a background document for hearings and discussions.

- The date and venue for the scoping meeting(s) will be set and a provisional agenda prepared. Invitations for the meeting and the scoping document will be sent to collaborating agencies, stakeholder groups, NGOs, experts and advisers. The scoping meeting will also be announced in public and the scoping document put on display for public inspection. A handout may be circulated, notices posted in communities and media advertisements arranged to enhance public participation. If the number of potentially interested people and organisations is large, questionnaires requesting written comments should be considered.
- During scoping consultations, a complete list of all issues and concerns should be compiled. These items may then be evaluated in terms of their relative importance and significance to prepare a shorter list of key issues, which can be classified into different impact categories to be studied in the EIA.
- The Terms of Reference for EIA will be prepared, including information requirements, study guidelines, methodology and protocols for revising work.

Scoping tools and instruments

When a competent authority or a developer undertakes scoping, three key questions should be answered (EU 2001b):

- What effects could this project have on the environment?
- Which of these effects are likely to be significant and therefore need particular attention in the environmental studies?
- Which alternatives and mitigating measures ought to be considered?

Basic instruments such as checklists and matrices are often used to provide a systematic approach to the analysis of potential interactions between project and environment. For example, checklists for scoping have been elaborated by the European Union as supporting information to the European EIA directive framework⁷. The scoping checklists provide (a) a list of project characteristics which could give rise to significant effects, and (b) a list of environmental characteristics which could be susceptible to significant adverse effects.

Standardised scoping procedure

An effective way of dealing with an increasing number of desalination projects may be to elaborate a standardised scoping procedure and Terms of Reference. The scoping process will often involve the same representatives of government agencies, NGOs, consultants, etc. A guideline, elaborated in a collaborative effort between these groups, may routinise the scoping procedure and may establish standards for the environmental studies to be undertaken and the information to be submitted in EIAs for desalination plants. The guideline could thus serve as a blueprint for scoping, which should still allow for project-specific adjustments.

⁷ EIA Directive 85/337/EEC from 1985, amended by Directive 97/11/EC in 1997.

Step 3 – Identification and description of policy and administrative aspects

EIAs usually take place within the distinctive legislative frameworks established by individual countries and/or international agencies. It is therefore recommendable to gain a deeper insight and understanding of any national policies or international agreements that apply in a country or region and that relate to EIA procedures in general (UNEP 2002).

Moreover, any other policy relevant to the desalination project needs to be identified. Major thematic areas that should be considered when searching the national or international legal system include conservation of nature and biological diversity, control and prevention of pollution, water resources management, and land-use and regional planning.

In many jurisdictions, more than one permit will be required to realise a desalination project. The main approval process, which authorises construction and operation of a plant, will not necessarily replace other existing statutory provisions and permits. For example, the construction and operation of a desalination plant can present a number of safety hazards to plant workers, so that a specific workplace safety permit will probably be required and/or a plan must be developed to ensure occupational safety and health of the workers.

It is important to clarify early in project planning which permits must be obtained and to contact the competent authorities. The permitting process may be facilitated by nominating a “lead“ agency, which coordinates the process by involving other agencies and by informing the project proponent about permitting requirements.

Step 4 – Investigation and description of the proposed desalination project

A technical project description should be prepared and included in the EIA report. It should form the basis of the EIA process by providing background information on the project which is required to investigate and analyse all potential impacts. The project description should cover the different life-cycle stages of construction, commissioning, operation, maintenance and decommissioning of the desalination plant. It should be succinct, containing all the information necessary for impact assessment but omitting irrelevant or distracting details.

Step 5 – Investigation and evaluation of environmental baseline

This step will entail assembling, evaluating and presenting baseline data of the relevant environmental, socio-economic and public health characteristics of the project area before construction and including any other existing levels of degradation or pollution.

A reference area with similar baseline characteristics may be selected and surveyed in parallel, to which the project site can be compared during project monitoring in order to detect any changes caused by construction and operation activities.

The scope of the baseline studies to be undertaken in an EIA for a desalination project should have been determined during scoping (Step 2) and should be briefly outlined in the EIA report. They will often have the following information requirements.

- **Socio-economic and -cultural environment:** population, land-use, planned development activities, status of existing water resource management programmes (conservation and reuse), community structure, employment, distribution of income, goods and services,

recreation, public-health, cultural properties, tribal and indigenous people, customs, attitudes, perception, aspiration etc.

- **Public health environment:** health indices of the populations at risk of being affected by the project, e.g. rates of morbidity, mortality, injuries, accidents, and life expectancy, as well as relevant socio-economic indicators of the quality of life. It should be noted here that WHO Constitution defines health as “state of complete physical, mental, and social well-being and not merely the absence of disease or infirmity”.
- **Abiotic environment:** geology, topography, climate, meteorology, ambient air quality, surface and ground water quality and hydrology, coastal and marine environmental quality, existing sources of emissions to air, soils and water, capacity of environmental systems to take up, degrade, dilute and disperse emissions, noise levels, etc.
- **Biotic environment:** flora and fauna including rare and endangered species, sensitive habitats, species of commercial value, species with potential to become nuisances, etc.

Step 6 – Investigation and evaluation of potential impacts of the project

In this step of the EIA, a prognosis, description and evaluation of the potential environmental, socio-economic and health impacts of the proposed project is elaborated. Potential impacts can be identified and evaluated by comparing the observed changes in the project area with baseline data from pre-construction or with reference data from a reference site. Reference data from a site with similar environmental characteristics may be particularly useful to identify natural variations or detect other anthropogenic changes that are not attributed to the desalination project.

The magnitude, spatial and temporal range of all identified impacts and their relative significance should be evaluated in this step. Where possible, an attempt should be made to further distinguish between direct and indirect impacts, immediate and long-term impacts, reversible and irreversible impacts, avoidable and unavoidable impacts, positive and negative impacts. It is recommended that identified positive and negative effects are also balanced in terms of their societal and environmental costs and benefits. If possible, potential cumulative, transboundary and growth-inducing effects should be identified and investigated. Careful deliberation about the accuracy of all predictions made in the EIA is recommended. These can only be as accurate and valid as the data and information available. It is therefore necessary to identify any information gaps and deficiencies in the EIA, and to assess any uncertainties associated with the prognosis of impacts.

Application of the precautionary principle

The precautionary principle as defined by the UN should be applied in the EIA where uncertainty about impacts exists. The precautionary principle was defined and adopted by the Rio Conference on the Environment in 1992 as Principle No. 15, which states that “in order to protect the environment, the precautionary approach shall be widely applied by States according to their capability. Where there are threats of serious or irreversible damage, lack of full scientific certainty shall not be used as a reason for postponing cost-effective measures to prevent environmental degradation.” The precautionary principle, therefore, requires action to be taken to prevent serious adverse impacts on human health or the environment, even if there is not incontrovertible proof but where there is strongly suggestive evidence. This does not mean action

on the basis of speculation and complete lack of evidence. There is, of course, a balance to be struck between human welfare and environmental protection that will allow sustainable societies.

The Rio definition leaves room for interpretation on when and how to apply the precautionary principle. Recognizing the need for a clear and consistent approach, the European Commission has adopted a Communication⁸ in the year 2000, which provides guidance on the use of the precautionary principle by:

- outlining the Commission's approach to using the precautionary principle;
- establishing guidelines for applying the precautionary principle;
- building a common understanding of how to assess, appraise, manage and communicate risks that science is not yet able to evaluate fully; and
- avoiding unwarranted recourse to the precautionary principle, which in certain cases could serve as a justification for disguised protectionism.

The World Health Organisation is also addressing decision-making in environmental and health matters under scientific uncertainty and complexity. As part of the Health Impact Assessment Methods and Strategies (HMS) Programme, the role and relevance of the Precautionary Principle in protecting human health is to be further clarified.

The 4th Ministerial Conference on Environment and Health (Budapest, 2004)⁹, recognising the Rio Declaration and the European Commission's Communication, reaffirmed the importance of the precautionary principle as a risk management tool. In the Conference Declaration, it is recommended that the precautionary principle should be applied "where the possibility of serious or irreversible damage to health or the environment has been identified and where scientific evaluation, based on available data, proves inconclusive for assessing the existence of risk...". The document "The precautionary principle: protecting public health, the environment and the future of our children" was prepared as background document (WHO, 2004).

Methods for predicting impacts

All predictions in an EIA are based on conceptual models of the environmental systems. Several approaches and instruments can be used for predicting impacts. Each covers the range of impacts only partially and should therefore be used in conjunction with others.

- **Field and laboratory experimental methods:** This might include tests to predict impacts of a certain agent or activity on an indicator (e.g. a sensitive species), e.g. testing of desalination effluents in whole effluent toxicity tests (WET) using sensitive endemic species.
- **Physical or image models:** This involves the design and construction of small scale models to study effects with a high degree of certainty in miniature.
- **Analogue models:** Predictions are based on analogies, i.e. by comparing the potential impacts of the proposed desalination project to a similar, existing project.

⁸ http://europa.eu.int/comm/environment/docum/20001_en.htm

⁹ <http://www.euro.who.int/document/e83335.pdf>

- **Mathematical models:** Models based on cause-effect relationships are used, which vary in complexity from simple input-output relationships to highly sophisticated dynamic models with a wide range of interrelations, variable parameters and coefficient constants that have to be identified and determined.
- **Mass balance models:** These models are based on the difference in the sum of the inputs as compared to the sums of outputs.
- **Matrices:** For predicting the impacts of a project, a two dimensional matrix is often used which cross-references the project activities on one axis with the environmental, socio-economic and human health setting in the project site on the other axis.

Criteria for evaluating the significance of impacts

General criteria can be used to assess the significance of environmental and socio-economic impacts of a desalination project. These criteria are not mutually exclusive but are very much interrelated. The following general criteria should be taken into account when examining potentially significant adverse effects:

- **nature of impacts** (direct / indirect, positive / negative, cumulative, transboundary);
- **time-span** (short / medium / long-term, permanent / temporary, often / seldom);
- **extent** (geographical area, size of affected population / habitat / species);
- **magnitude** (low / severe, reversible / irreversible);
- **probability** (high / medium / low probability, certain);
- **possibility to mitigate, avoid or offset** significant adverse impacts.

Step 7 – Mitigation of negative effects

The consideration of major alternatives such as alternative location, technology etc. should start early in the planning of a new project (cf. Step 2 – Scoping), as the disposition to make major modifications is typically still high at this time. As project planning consolidates, major alternatives will only be seriously considered if the EIA has revealed significant impacts that cannot be mitigated otherwise. The investigation of impact mitigation measures should thus be understood as a process, which starts with the consideration of major alternatives in early project planning and continues after potential impacts have been analysed (Step 6). At this stage, specific recommendations need to be elaborated that mitigate the predicted effects of the project.

The step of impact mitigation should identify the most feasible and cost-effective measures to avoid, minimise or remedy significant negative impacts to levels acceptable to the regulatory agencies and the affected community. The definition of “acceptable” will vary according to different national, regional or local standards, which depend on a society's or community's social, ideological and cultural values, on economic potentials and on politics. For impacts which cannot be mitigated by technically and economically feasible methods, compensation methods should be identified. These may include monetary compensation or remediation activities.

The elements of mitigation are organised into a hierarchy of actions (UNEP 2002):

- **Prevention:** avoid impacts by preventive measures, consider feasible alternatives and identify the best practicable environmental option.
- **Minimisation:** identify customised measures to minimise each of the main impacts predicted and ensure they are appropriate, environmentally sound and cost-effective.
- **Remediation:** remedy or compensate for adverse residual impacts, which are unavoidable and cannot be reduced further, as a last resort.

Mitigation can include *structural measures* (e.g. design or location changes, technical modifications, waste treatment) and *non-structural measures* (e.g. economic incentives, policy instruments, provision of community services, capacity building). Remediation and compensation may involve *rehabilitation* of the affected site (e.g. habitat enhancement, restocking of fish), *restoration* of the affected site to its previous state after project demolition, and *replacement* of resource values at another location.

Step 8 – Summary and conclusions

In this step, the main findings and recommendations of steps 5 – 7 are summarised. The focus should be on the key information that is needed for drawing conclusions from the EIA results.

An overview of the main impacts (possibly in the form of a table) should be provided for this purpose, distinguishing between significant impacts which can be prevented or minimised, and those which cannot. Both direct and indirect impacts, positive and negative impacts, as well as potential cumulative effects, should be considered.

Mitigation or alternative options should be offered for significant impacts where possible. In essence, the original project proposal should be systematically compared with alternative project configurations in terms of adverse and beneficial impacts and effectiveness of mitigation measures. As far as possible, trade-offs and uncertainties should be mentioned.

Finally, the '*best practicable environmental option*' should be identified, which is the preferred project configuration under environmental, social, cultural and public health criteria. It should be ensured that this option is both economically and technologically feasible. The decision should be transparent and backed by arguments.

Step 9 – Establishment of an environmental management plan

An environmental management plan should be elaborated to ensure the ongoing assessment and review of the effects of the proposed desalination project during construction, commissioning, operation, maintenance, and decommissioning. It thus builds continuity into the EIA process and helps to minimise environmental impacts and optimise environmental benefits at each stage of project development. Attention should be given to involve the public in EIA implementation activities, for example by establishing stakeholder monitoring committees.

The key objectives of EIA implementation and follow up are to (UNEP 2002):

- identify the actual environmental, socio-economic and public health impacts of the project and check if the observed impacts are within the levels predicted in the EIA;
- determine that mitigation measures or other conditions attached to project approval (e.g. by legislation) are properly implemented and work effectively;
- adapt the measures and conditions attached to project approval in the light of new information or take action to manage unanticipated impacts if necessary;
- ensure that the expected benefits of the project are being achieved and maximised;
- gain information for improving similar projects and EIA practice in the future.

To achieve these objectives, the management plan should specify any arrangements for planned monitoring, surveillance and/or auditing activities, including methodologies, schedules, protocols for impact management in the event of unforeseen events etc. The main components and tools of EIA implementation and follow up as part of a management plan include (UNEP 2002):

- **Monitoring activities:** measure the environmental changes that can be attributed to project construction and operation, check the effectiveness of mitigation measures, and ensure that applicable regulatory standards and requirements are being met, for example for waste discharges and pollutant emissions.
- **Surveillance activities:** oversee adherence to and implementation of the terms and conditions of project approval.
- **Auditing activities:** evaluate the implementation of terms and conditions, the accuracy of EIA predictions, the effectiveness of mitigation measures, and the compliance with regulatory requirements and standards.

Step 10 – Review of the EIA and decision-making process

The purpose of review is to verify the completeness and quality of the information gathered in an EIA. This final step shall ensure that the information provided in the report complies with the Terms of Reference (ToR) as defined during scoping (Step 2) and is sufficient for decision-making purposes. Review is a formal step in the EIA process and serves as a final check of the EIA report that will then be submitted for project approval.

The review may be undertaken by the responsible authority itself, another governmental institution or an independent body. Participation of collaborating and advisory agencies in the review process is strongly recommended, as is the involvement of the public and major stakeholders in public hearings about the outcomes of the EIA. The review should follow a systematic approach. This will entail (a) an evaluation and validation of the EIA methodology and procedure and (b) a check for consistency, plausibility and completeness of the identified impacts, proposed alternatives and suggested mitigation measures. The review process can be based on explicit guidelines and criteria for review, or may draw on general objectives, such as the following questions (UNEP 2002):

- Does the report address the Terms of Reference?
- Is the requested information provided for each major component of the EIA report?
- Is the information correct and technically sound?
- Have the views and concerns of affected and interested parties been considered?
- Is the statement of the key findings complete and satisfactory, e.g. for significant impacts, proposed mitigation measures, etc.?
- Is the information clearly presented and understandable?
- Is the information sufficient for the purpose of decision-making and condition setting?

The response to the last question is the most significant aspect for review and will largely determine whether or not the EIA can be submitted to the competent authority as it is or with minor revisions for decision-making.

The competent authority will form its own judgement on the proposed project based on the EIA report, the analysis of stakeholder interests, statements from collaborating agencies etc. and decide on approval or rejection of the proposed project. The competent authority will typically impose conditions if the project is approved, such as mitigation measures, limits for emissions or environmental standards which must be observed.

6.3 Summary recommendations for EIA

An Environmental Impact Assessment (EIA) is a procedure that identifies, evaluates and develops means of mitigating potential impacts of proposed activities on the environment. Its main objective is to promote environmentally sound and sustainable development through the identification of appropriate mitigation measures and alternatives. Based on the EIA results, a decision must be reached which balances the positive and negative effects of a project in terms of their societal and environmental costs and benefits.

A formal EIA is often required for major development projects, such as a power plant or motorway, and may also be requested by authorities for projects in the water sector, such as for a dam and reservoir, water pipeline, wastewater treatment plant or desalination facility. An EIA can also be adopted for plans, policies or programmes (e.g. water resources or coastal zone management plans) in the form of a Strategic Environmental Assessment (SEA). The present document is primarily considered as a guidance for impact assessment on project level. Depending on the proposed project, it is incumbent upon the national authorities to define the scope and requirements for each EIA.

In general, an EIA should predict the impacts related directly or indirectly to the implementation of a desalination project. Where appropriate, this should comprise implications including ecosystem, socio-economic, cultural and public health effects, as well as cumulative and transboundary implications. The EIA should identify the positive effects and offer measures for mitigation of negative impacts.

The impact mitigation step should identify the most feasible and cost-effective measures to avoid, minimise or remedy significant negative impacts to levels acceptable to the regulatory agencies and the affected community. The definition of “acceptable” will vary according to

different national, regional or local standards, which depend on a society's or community's social, ideological and cultural values, on economic potentials and on politics.

An EIA for a desalination project should address the following three areas of impact:

▪ Abiotic and biotic environment

Abiotic factors include characteristic landscape and natural scenery, as well soils and sediments, air and water quality. The biotic environment encompasses the terrestrial and marine biological resources, including flora and fauna, in particular sensitive species that inhabit the area impacted by the proposed project.

▪ Socio-economic and cultural environment

Socio-economic and cultural considerations include the project's effects on the day-to-day lives of the individuals and the community, the project's impact on the management of natural resources and the project's impact on local and regional development. Gender- and age-specific effects and variations among the potentially affected population, such as social or ethnic affiliations, should be considered where appropriate.

▪ Public health

Public health addresses the quality of life (well-being), improvement in community health, and potential risks associated directly or indirectly with the desalination project.

Key aspects that should be investigated in EIAs for desalination projects are:

Impacts related to the siting of the desalination facility and supporting infrastructure.

▪ Impacts related to the intake of source water, in particular impacts due to

- the construction of intake structures;
- the entrainment and impingement of organisms.

▪ Impacts related to the discharge of concentrates, cooling water and other waste streams resulting from the process, including

- an investigation of the hydrological mixing process in the discharge area;
- an investigation of impacts related to salinity, temperature, pH or dissolved oxygen levels deviating from ambient conditions in the mixing zone;
- an investigation of environmental fate and potential toxic effects of chemical residuals and by-products from the process, particularly of pretreatment and cleaning chemicals.

The EIA process proposed for desalination projects involves 10 basic steps

1. Decide, on the basis of a screening process, whether or not an EIA is required.

2. Conduct scoping to determine the contents and extent of the EIA.
3. Identify policy and administrative aspects relevant to the project and the EIA.
4. Describe the technical design and process of the proposed desalination project.
5. Describe and assess the environment baseline of the project site.
6. Describe and evaluate the potential impacts of the project on the environment.
7. Identify approaches for mitigation of negative impacts.
8. Provide a summary of the major findings and develop conclusions.
9. Establish a programme to monitor impacts during construction and operation.
10. Review the EIA process for decision-making purposes.

The following aspects should be considered when carrying out an EIA:

▪ Precautionary principle

Gaps of knowledge and uncertainties should be clearly identified and the precautionary principle as defined by the UN applied as appropriate in the EIA.

▪ Public involvement

Public involvement is an integral part of the planning and decision-making process and implementation of desalination projects for community water supply.

Additional recommendations which go beyond the scope of individual EIAs are:

▪ Implementation of management plans

To manage increasing desalination activity on a regional or national scale, and to make it compatible with other human activities and nature conservation in the coastal zone, it is recommended to elaborate plans which go beyond the scope of individual projects, in particular water resources management and integrated coastal zone management plans.

Water resources management plans should cover a suite of supply and demand options including water conservation programmes and education, the use of water saving devices and water recycling for agricultural, industrial and environmental applications.

▪ Future research

The present knowledge of the environmental, socio-economic, cultural and human health implications of desalination activity is limited. It is recommended that further research be initiated, that monitoring of existing facilities be conducted, case studies initiated, and that results from monitoring, case studies and EIAs be made available to a wider public to improve the understanding of the actual impacts of desalination activity on man and environment. To facilitate this process, the establishment of a clearing house for collecting and distributing the information should be considered.

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